



钕铁硼永磁废料中稀土回收循环利用现状及展望

宋 强^{1,2,3}, 童 雄^{1,2}, 谢 贤^{1,2}, 张文杰^{1,2}, 曹 阳^{1,2}, 杜云鹏^{1,2}, 程雅芝^{1,2}

(1. 昆明理工大学 国土资源工程学院, 昆明 650093;

2. 金属矿尾矿资源绿色综合利用国家地方联合工程研究中心, 昆明 650093;

3. 云南缘矿科技开发有限公司, 昆明 650093)

摘 要: 钕铁硼(NdFeB)永磁材料在众多领域得到广泛应用, 在生产NdFeB永磁材料的过程中, 会产生大量废料, 直接丢弃不仅会污染环境, 还是对二次资源的浪费。本文综述了NdFeB永磁废料中稀土循环利用的技术现状, 对比分析了氯化法、合金法、选择氧化法等火法在工业应用中的现状和存在的不足; 并且详细阐述了全溶法、盐酸优溶法、草酸沉淀法、硫酸复盐法、溶剂萃取法等湿法的研究情况, 深入剖析了不同方法存在的局限和优势; 同时, 介绍了电沉积法、生物浸出法、氢化法、机械化学法等新技术方法的研究现状。在此基础上, 展望了未来回收循环利用NdFeB永磁废料中稀土技术方法发展的方向。

关键词: 钕铁硼永磁材料; 废料; 稀土; 循环利用; 火法; 湿法

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稀土元素具有独特的4f层电子结构, 加入稀土制成的稀土材料表现出优异的电、光、催化、磁等性质, 使其在陶瓷、国防、航空、电子信息、新能源等领域有着极其重要的应用^[1-5]。其中, NdFeB永磁材料由于具有高剩磁、高矫顽力、高磁能积等特点而在风力发电、新能源汽车、电机、耳机等现代工业得到广泛应用^[6-8]。具体消耗情况见如图1所示, 且需求量逐年增长^[9]。

NdFeB永磁材料中含有30%左右的稀土元素(Nd、Pr、Dy、Tb等), 在永磁材料需求日益增长的背景下, 其年产量以5%的增幅增长, 2020年全

世界稀土永磁材料产量接近20万t^[10-11]。巨大的产量使不可再生的稀土资源急剧消耗, 虽然我国稀土储量位居世界第一, 但粗犷的开采方式和急剧的消耗使我国稀土资源终将面临枯竭的困境^[12]。随着绿色环保、循环经济理念的不断深入, 人们越来越重视二次资源中稀土的绿色高效循环利用, 以此缓解稀土资源供应的压力。在生产NdFeB永磁材料过程中, 由于产品易氧化、开裂等因素从而会产生大量废料, 直接丢弃不仅污染环境, 而且也造成资源的极大浪费^[13-14]。相较于美国、日本和欧洲等发达国家, 我国对NdFeB永磁废料的利用还远远不够。

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通信作者: 谢 贤, 教授, 博士; 电话: 15987188290; E-mail: kgxianxie@126.com

只有极少数企业具备循环利用永磁废料中稀土的工艺,但也存在处理成本高、技术不成熟等弊端。在国务院颁布《国务院关于促进稀土行业持续健康发展的若干意见》中,明确指出要积极开展稀土资源回收工作^[15-18]。为此,本文综述了当前NdFeB永磁废料中稀土元素循环利用的技术现状及存在的弊端,并探讨其发展趋势,为我国NdFeB永磁废料中稀土元素绿色高效循环利用提供借鉴。

1 NdFeB 永磁材料及废料来源

1.1 NdFeB 永磁材料

进入 20 世纪后,永磁材料得到了飞速发展,其中,稀土永磁体材料经历了以SmCo₅为代表的第一代、以Sm-Co为代表的第二代及以Nd₂Fe₁₄B为代表的永磁合金。由于Co价格过于昂贵,严重制约第一和第二代永磁材料的应用和发展^[19]。NdFeB永磁材料最早通过粉末冶金技术制备,其单晶的饱

和磁化强度 $M_s=1.6\text{ T}$,磁晶各向异性 $H_A=5.81\text{ MA/m}$,居里温度 $T_c=585\text{ K}$ 。在此基础上,实验室制备的NdFeB永磁材料的磁体能级超过 6.91 kJ/m^3 ,因此也被称为“磁王”^[20]。

在后续的研究中,通过加入Cu、Al、Ga、Dy等元素可对NdFeB系永磁材料进行改性研究,以取代主相晶格的原子的方式来改变材料的磁化强度 M_s 、磁晶各向异性 H_A 、居里温度 T_c 等性质^[21-22]。还可利用“掺杂”型金属元素,将其置于主相晶粒间,起到抑制软磁相生成,改善晶间相的作用,增强矫顽力和抗腐蚀性,提高NdFeB性能。

1.2 NdFeB 永磁废料的来源

优良的性质使NdFeB永磁材料拥有广阔的应用前景,目前永磁材料的生产制造流程如图2所示^[23]。在NdFeB永磁材料的生产过程中,由于对产品质量要求高,永磁材料易氧化、开裂等因素往往导致产品报废率较高,原料利用率只有70%左

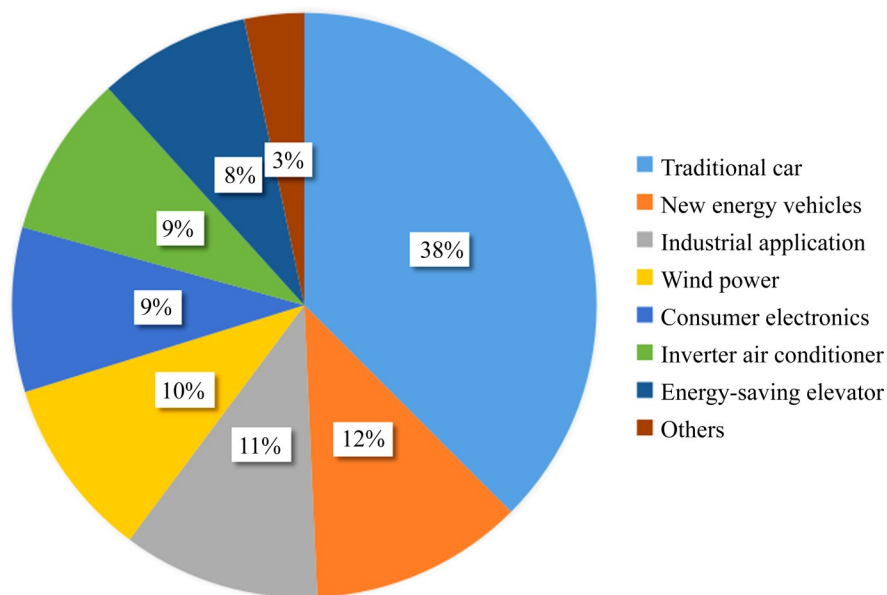


图1 高性能NdFeB永磁材料不同行业消费占比

Fig. 1 Consumption proportions of high-performance NdFeB permanent magnet materials in different industries

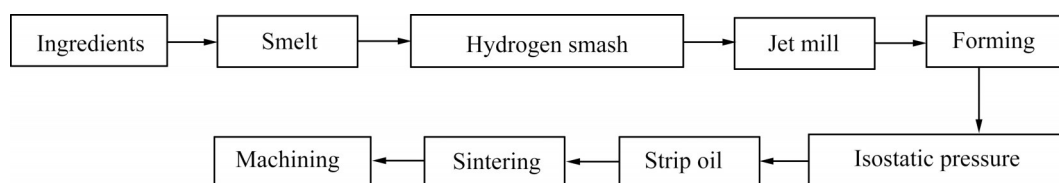


图2 NdFeB永磁材料生产流程图^[23]

Fig. 2 Production flow chart of NdFeB permanent magnet material^[23]

右,会产生大量的废料,中国每年产生的废料约有6万t,其中含有大量稀土资源^[24]。

在生产NdFeB永磁材料的各个阶段,均会伴随废料的产生,一般包括原料预处理过程中的损耗、熔炼过程中被氧化的钕、氢碎和气流磨磨粉阶段中产生的超细粉、制粉阶段被空气氧化的粉末、烧结过程中被氧化的NdFeB块状料及机加工时边角料和表面处理产生的不合格产品等^[25]。由此可以看出,NdFeB永磁废料在生产过程中很难避免且废料量大,对废料中稀土绿色高效循环利用,不仅是提高稀土利用率的需要,更是降低生产成本的迫切需要,具有显著的经济效益。

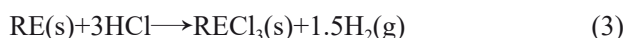
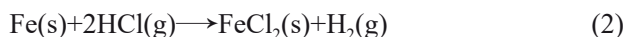
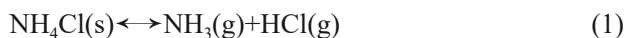
2 火法回收

2.1 氯化法

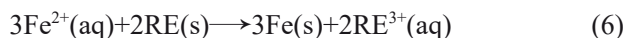
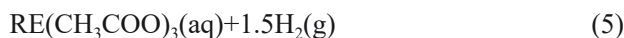
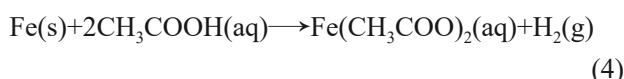
钕铁硼废料中稀土元素相较于其他金属元素更活泼,能对Cl⁻表现出更强的亲和力,生成稀土氯化物而与其他元素如Fe分离。目前,在氯化法中用于分离回收稀土的氯化剂一般为FeCl₂、NH₄Cl、MgCl₂-KCl等^[26-27]。其中,当FeCl₂作氯化剂时由于钕铁硼废料中含有氧,容易氧化Fe²⁺,因此,在反应过程中往往需要添加碳粉,脱除废料中所含的氧,促使稀土元素被完全氯化。UDA等^[28]以永磁废料为研究对象,采用氯化法回收其中稀土;研究表明当FeCl₂为氯化剂时,添加碳粉在800℃条件下能有效促进氯化反应进行;反应过程中加入过量的FeCl₂能促使稀土氧化物完全转化为稀土氯化物,再利用彼此间沸点的差异采用真空蒸馏的方式使其分离,最终永磁废料中稀土回收率接近96%,且所得稀土氯化物纯度超过99%。采用NH₄Cl作氯化剂时,其在较高温度下能发生分解,产生的干燥HCl气体可对稀土元素进行氯化,适用于回收超细粒永磁废料中的稀土元素。ITO等^[29]将NH₄Cl和钕铁硼永磁材料置于反应器中,在300℃的条件下反应3h,将所得固体产物用去离子水浸出溶解,最终稀土回收率可达87%。TOM等^[30]以NH₄Cl为氯化剂回收风力电机废旧永磁材料中的稀土元素;在225~325℃的反应温度下,NH₄Cl发生分解,产生的干燥HCl使稀土转变成稀土氯化物,再将其溶解于醋酸缓冲溶液中,所发生的化学反应如式(1)~(6)所示。该工艺能回收约85%的稀土,相较于最优条

件下的盐酸优溶法,该方法的化学试剂消耗减少了45%,还可得到额外具有经济价值的产品(质量分数为2.9%的氨水溶液),且在德国弗莱堡工厂已经开始应用。

氯化反应:



醋酸缓冲溶剂溶解反应:



采用MgCl₂-KCl作氯化剂时,需在较高温度下使其处于熔融态,与稀土元素反应生成稀土氯化物,从而与其他金属分离。HUA等^[31]以MgCl₂-KCl为氯化剂回收钕铁硼中稀土元素,在800~1200℃反应温度下使氯化剂处于熔融态,再与破碎后的永磁材料进行反应;Nd能将熔融态的MgCl₂还原成Mg,同时转化为NdCl₃,最终得到的产物为RECl₃-MgCl₂-KCl混合物,再经真空蒸馏分离回收稀土,回收率能达到90%。

氯化法回收稀土对一般钕铁硼废料具有较好的回收效果,但对氧化严重的废料进行处理时回收效果较差。该方法最终得到的产物一般为稀土氯化物,由于这类物质易潮解,因此还需转化为稀土氧化物,间接增加了工业流程,提高了生产成本。

2.2 合金法

采用合金法回收钕铁硼废料中的稀土时,由于稀土元素Nd与一些金属元素能形成低熔点合金,因此可达到分离稀土的目的^[32]。常用的金属元素有Mg、Ag等,Mg能在较低温度下形成熔融态,稀土Nd与熔融态Mg结合形成MgNd、Mg₂Nd、Mg₃Nd、Mg₄₁Nd₅等合金^[33-34]。同样,稀土Nd也能与熔融态Ag形成AgNd、Ag₂Nd、Ag₅₁Nd₁₄等合金,从而将稀土元素提取出来^[35-36]。再利用高温蒸气法使此类合金中稀土分离,得到较高纯度的稀土产品。

TAKEDA等^[37]在如图3所示反应装置中回收钕铁硼废料中稀土时,往位于装置底部的Ta坩埚中

装入Mg,在高温条件下Mg变为蒸汽挥发,在装置顶部冷凝后滴入进装有钕铁硼废料的Fe坩埚中;此时处于熔融态的Mg与废料中稀土Nd结合形成Mg-Nd合金,再经Fe坩埚壁上的缝隙滴落进底部坩埚中;经过充分反应直至Nd被提取完成,再经高温蒸馏使Nd从合金中分离;在最佳反应条件下,废料中稀土Nd的回收率和最终产物纯度分别为99%和98%。在此基础上,TAKEDA等^[38]探究了利用熔融Ag直接提取钕铁硼永磁磁铁残渣中的稀土Nd,在1273 K条件下残渣中90%的Nd能被提取回收,最终所得Ag-Nd合金在空气中氧化,以Nd₂O₃形式存在于合金中。虽然银液作为一种有效提取Nd的介质,但从所得产物合金中将Nd₂O₃分离的难度较大。

该方法在回收永磁废料中稀土时能得到稀土金属单质,在一定程度上缩减了后续工艺流程。但该工艺在反应过程中所需温度较高,不仅对操作设备要求比较高,而且能耗高,同时所得合金产物还需高温蒸馏,使工艺较冗长繁琐。

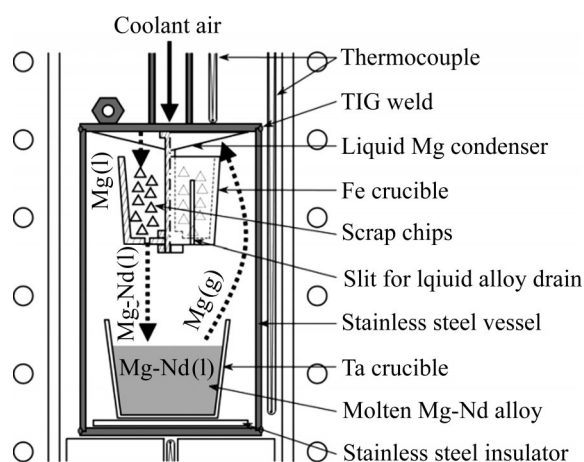


图3 镁合金法实验装置示意图^[37]

Fig. 3 Schematic illustration of apparatus for neodymium extraction from scrap alloys using magnesium circulation^[37]

2.3 选择氧化法

采用选择氧化法回收钕铁硼废料中稀土时,主要利用不同温度下铁和稀土对氧亲和力的差异性,并依据Nd-Fe-O相图控制反应过程中氧分压,最终使稀土优先与氧结合形成稀土氧化物,而Fe以金属态形式存在,从而达到分离回收的目的^[39-40]。其中,Fe-Nd-O (1077 ℃)、Fe-Dy-O (977 ℃)、Fe-Pr-O (1027 ℃)的相图如图4所示,由图4可知,在温度

为1077 ℃、当氧分压 $<10^{-10}$ Pa的条件下,NdFeO₃会分解成Fe(s)和Nd₂O₃(s);在氧分压 $<10^{-12}$ Pa、温度在977 ℃和1027 ℃的条件下,NdFeO₃均会分解^[41]。减小氧分压的本质是脱氧过程,在处理过程中一般通过加氢或加钙来达到脱氧的目的。NAKAMOTO等^[42]在Fe-Nd-O相图基础上,通过石墨坩埚控制系统氧势,加入钙来脱除氧,使系统中氧势控制在 10^{-12} ~ 10^{-13} Pa之间,最终得到Fe单质和稀土氧化物,且稀土回收率超过99%。采用选择氧化法控制氧势分离稀土和Fe时,得到的稀土产品中往往还有较多氧化硼,降低了稀土纯度。为了降低稀土氧化物中硼的含量,SAITO等^[43]以采用玻璃渣法(Glass slag method)回收钕铁硼材料中稀土Nd;利用B₂O₃作氧化剂,使稀土Nd氧化成Nd₂O₃,而氧化硼被还原为硼单质进入Fe中,有效提高了Nd₂O₃的纯度。

该方法一定程度上能有效回收钕铁硼废料中稀土元素,并且基本无需消耗其他化学试剂,对环境友好。但是,所得稀土氧化物产物纯度不高,往往还含有Fe和硼杂质,虽然可以延长反应时间或磁吸引来提高稀土产品纯度,但反应温度整体较高,增加了生产成本。

3 湿法回收

3.1 全溶法

全溶法是通过盐酸将铁钕硼废料中能溶解的稀土和铁等元素全部溶解,也被称为盐酸全溶法。再以H₂O₂为氧化剂使铁以Fe³⁺形式存在溶液中,结合后续沉淀或萃取工艺分离回收溶液中的稀土元素^[44-45]。

PADHAN等^[46]以盐酸为溶剂将NdFeB废料全部溶解,再以萃取剂NaCyanex302分离回收溶液中Dy和Nd;整个过程在pH=1.2的条件下进行,Dy和Nd的分离系数达到53.65%,分离效果明显。LAI等^[47]以4 mol/L盐酸溶解处理NdFeB废料,待全部溶解后再分步沉淀,最终得到的稀土产品纯度高于99.4%,能直接用于新材料的生产。全溶法在溶解NdFeB废料时,溶液中除稀土外还存在大量杂质离子,对后续沉淀法和萃取法都有明显干扰。如沉淀过程中杂质离子与稀土离子出现沉淀的pH范围相近,降低了所得稀土产品纯度;萃取分离过

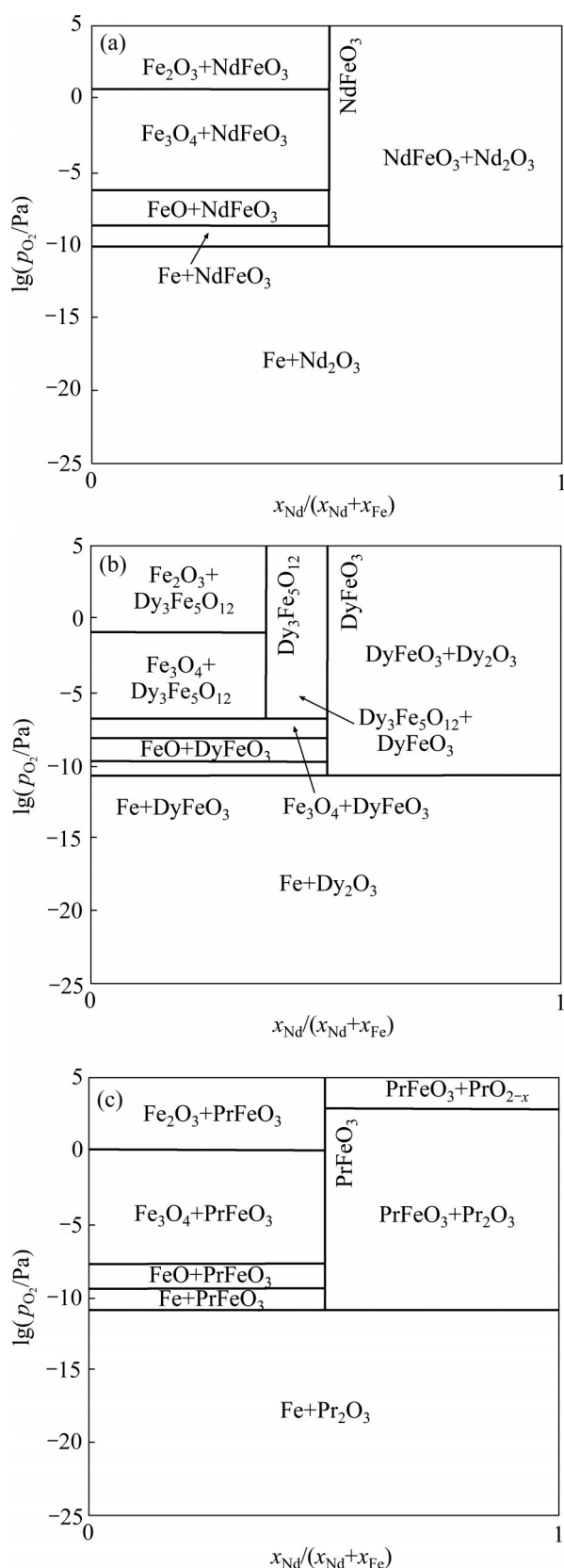


图4 不同温度下Nd-Fe-O系热力学平衡图^[41]

Fig. 4 Thermodynamic equilibrium diagram of Nd-Fe-O system at different temperatures^[41]: (a) 1077 °C ; (b) 1027 °C; (c) 977 °C

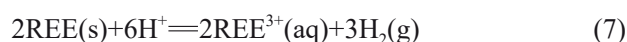
程中常见萃取剂易受到 Fe^{3+} 等杂质离子影响, 出现乳化现象, 降低分离效果, 增加分离成本^[48]。因此, 在工业生产中往往需要增加除杂工序, 提高分离效率。环烷酸、N503等萃取剂与 Fe^{3+} 结合效果明显, 常被用于脱除溶液中的 Fe^{3+} ; Fe^{2+} 和稀土离子在草酸环境中出现沉淀的pH值范围相差明显, 借助草酸调节溶液pH值能有效分离杂质 Fe^{2+} 。陈云锦^[49]在NdFeB废料全部溶解后, 以 H_2O_2 氧化 Fe^{2+} , 以萃取剂N503萃取 Fe^{3+} 净化溶液, 再以膦酸萃取剂P507提取溶液中稀土元素。该处理工艺不仅提高了稀土回收率, 还增加了萃取剂循环利用率。TIAN等^[50]以6 mol/L盐酸溶解NdFeB废料, 并添加酒石酸和六次甲基四胺(HMTA)螯合剂提高盐酸溶解浸出率, 再通过草酸去除杂质 Fe^{2+} , 最终回收的稀土产品纯度达到96%, 且回收率超过90%。MEHMET等^[51]以硫酸为溶剂将NdFeB废料全部溶解后, 加入 MnO_2 将超过99%的 Fe^{2+} 氧化成 Fe^{3+} , 再以 $\text{Ca}(\text{OH})_2$ 为沉淀剂去除杂质 Fe^{3+} , 最终得到合格的稀土产品。

采用全溶法处理NdFeB废料虽然原理和操作简单, 但在溶解废料过程中酸消耗量大, 对环境污染严重, 生产环境差, 且在溶解过程中会伴随大量杂质离子的溶出, 不仅增加了后续分离除杂的难度, 还降低了稀土产品纯度。

3.2 盐酸优溶法

针对全溶法中酸消耗量大的弊端, 人们提出了盐酸优溶法。首先通过氧化焙烧使NdFeB废料中稀土、Fe和其他金属物质均转化为氧化物, 再通过调节溶液pH值控制稀土氧化物优先与盐酸反应溶解, 使稀土元素以离子形式进入溶液中, 而其他元素残留在滤渣中^[52-53]。溶液中的稀土离子再经萃取剂提取纯化, 结合草酸使稀土沉淀, 最终能得到纯度较高的稀土氧化物。

LIU等^[54]经过研究发现, 在800 °C温度下对NdFeB废料进行焙烧, 能有助于后续稀土分离; 经过焙烧后的废料采用HCl对其溶解, 涉及反应如式(7)~(10)所示; 加入2 g/L NaNO_3 能显著促进稀土和硼从Fe中分离, 经过EHD萃取后使用草酸进行沉淀, 最终得到的稀土产品纯度超过99%, 且硼的回收率超过99.5%, 具体流程见图5所示。



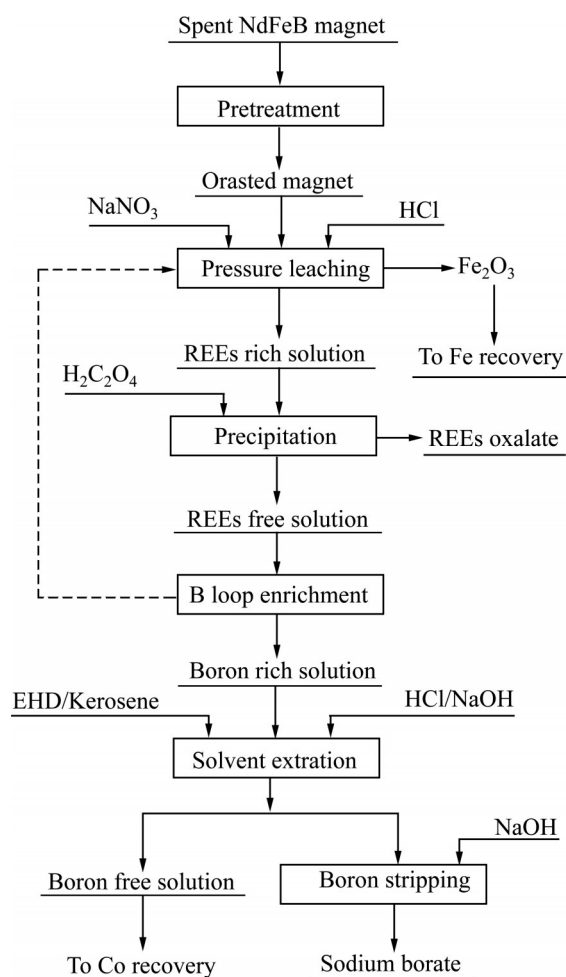
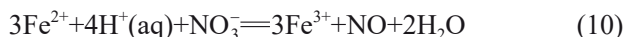
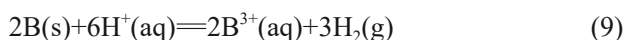
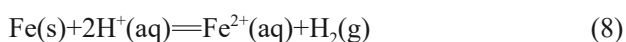
图5 盐酸优溶法回收NdFeB废料中稀土流程图^[54]

Fig. 5 Flow chart of process of recovering rare earth from NdFeB waste by hydrochloric acid excellent solution method^[54]



江泽佐等^[55]采用氧化焙烧-盐酸优溶-氧化除铁-萃取分离的工艺处理NdFeB回收料, 研究表明在90℃条件下以NaClO₃为氧化剂能使Fe²⁺的氧化

率达到99.99%, 在pH=4的溶液中形成Fe(OH)₃, 最终得到质量合格的稀土产品。

采用盐酸优溶法处理NdFeB废料时, 对焙烧温度的控制至关重要, 合适的焙烧温度可使稀土和铁能转化成Re₂O₃和Fe₂O₃, 同时避免稀土铁酸盐形成, 为后续盐酸控制pH, 优先溶解稀土氧化物奠定基础。相较于盐酸全溶法, 该方法对酸的消耗量有了明显降低, 资源利用率有了提高^[56]。但目前对焙烧的理论研究较为欠缺, 在实际工业处理中很难避免稀土铁酸盐(NdFeO₃)的产生, 使Nd和Fe无法有效分离; 并且在调控pH选择沉淀过程中, 在产生Fe(OH)₃沉淀的同时, 部分稀土也会形成沉淀, 造成稀土损失。王毅军等^[57]在盐酸优溶处理NdFeB废料后, 以晶型碳酸沉淀分离Nd, 该工艺有效降低了盐酸的消耗, 稀土损失率接近10%。

综上所述, 采用盐酸优溶法在处理NdFeB废料时, 工艺流程有了明显缩短, 且化学试剂消耗降低, 对环境更加友好, 具有应用前景。但在废料溶解过程中, 该方法效率较低, 同时产生大量废水, 对焙烧过程物相变化的理论研究较欠缺, 缺乏科学指导, 还需进一步深入研究。

3.3 草酸沉淀法

NdFeB废料经过溶解后, 溶液中的Fe²⁺和稀土离子与草酸形成的盐类物质的溶解度有显著差异, 借助其溶解度差异可使Fe和稀土分离。通过控制草酸加入量、溶液pH值和反应温度等因素变量, 可在最佳条件下得到较高纯度的Re₂(C₂O₄)₃, 再经灼烧而转变成稀土氧化物^[58-59]。尹小文等^[60]以草酸沉淀法分离回收NdFeB废料浸出液中稀土, 在溶液pH为1.5~2、草酸用量比为1.5、温度80℃的条件下对稀土沉淀效果最佳, 再将烘干的稀土草酸盐在800℃温度下焙烧, 最终产品中稀土氧化物含量

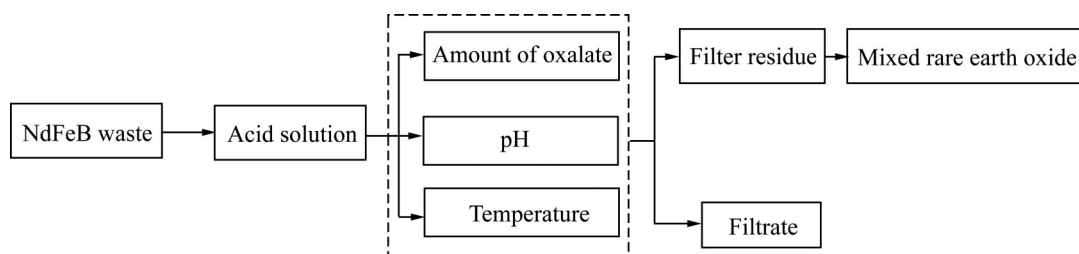


图6 草酸盐沉淀稀土流程图

Fig. 6 Flow chart of oxalate precipitation of rare earth

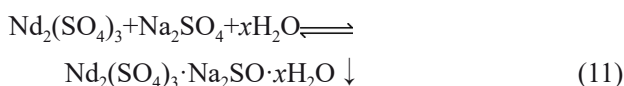
达到99.3%，具体流程如图6所示。

采用草酸沉淀法处理浸出液中稀土和Fe时，还存在大量杂质离子，会严重影响最终产品纯度。为此也有相关研究尽量减少浸出液中杂质离子含量，INNOCENZI等^[61]以柠檬酸为抑制剂，加入至废料浸出液中，有效抑制废料中锰的浸出，不仅减少了溶解过程酸的消耗量，还大幅提高了最终产品中稀土氧化物的纯度。

草酸沉淀法在一定程度上能有效分离稀土与铁，生产工艺简单，生产流程短。但由于NdFeB废料中铁的含量高，直接草酸沉淀会消耗大量草酸，并且草酸价格较高，制约了该方法在工业生产中的应用。

3.4 硫酸复盐法

由于稀土硫酸盐在溶液中能与 Na_2SO_4 反应，生产复盐沉淀，从而与溶液中 Fe^{2+} 分离，具体反应见式(11)所示。



采用该方法处理NdFeB废料时，首先通过 H_2SO_4 溶解浸出，使稀土和铁分别以稀土硫酸盐和 FeSO_4 形式存在溶液中，再控制温度加入 Na_2SO_4 ，使稀土形成复盐沉淀，而Fe则停留在溶液中；经过过滤后，稀土硫酸复盐沉淀与 NaOH 结合形成稀土氢氧化物，再经高温灼烧后得到纯度较高的稀土氧化物产品，具体流程如图7所示^[62-63]。

唐杰等^[64]对比了草酸沉淀法和硫酸复盐法回收NdFeB废料中稀土的效果，研究表明，草酸沉淀法不仅难以使稀土完全沉淀，并且沉淀中非稀土杂质含量较高，而硫酸复盐法得到的 Nd_2O_3 纯度较高，且对Nd的回收率超过82%。

硫酸复盐法在工业回收NdFeB废料过程中，对稀土的回收率能达到80%以上，整体操作流程简短，反应条件温和，成本相对较低，具有明显优势，尤其是对含Nd含量高的稀土废料效果显著，化学试剂消耗较少，更利于环境保护。但在采用硫酸复盐法的生产中，需要严格控制温度和 Na_2SO_4 用量(<理论量50%)，避免副反应发生；整个操作过程忽视了对溶液中硫酸亚铁的回收，不仅使资源被浪费，同时直接排放还会造成环境污染。

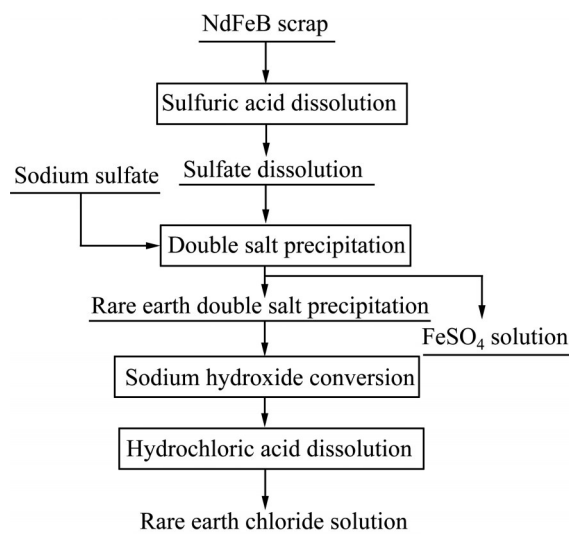


图7 钕铁硼废料回收的硫酸复盐沉淀法流程

Fig. 7 Flow chart of process of sulfuric acid double salt precipitation method for NdFeB waste recovery

3.5 溶剂萃取法

NdFeB废料中稀土等物质被溶解后，大量稀土与非稀土离子共同存在于溶液中，草酸沉淀、硫酸复盐等方法虽然在一定程度上能有效分离出稀土元素，但整体效率较低。溶剂萃取法通过有机萃取剂与溶液中稀土离子结合，而达到分离稀土的目的^[65-67]。该方法具有处理量大、分离系数和效率高、针对性强等优势。溶剂萃取法至关重要是有有机萃取剂的选择，目前对溶液中稀土有较好萃取性能的传统萃取剂有：D2EHPA、PC88A、Cyanex272、Cyanex923、Cyanex272、TBP、CA12等^[68-75]。YOON等^[76]对比分析了萃取剂D2EHPA和PC88A对Dy和Nd的回收效果，发现D2EHPA整体萃取分离Dy的性能优于PC88A；当D2EHPA浓度为0.1 mol/L、相比(O/A)为1:1时，经过2级萃取后，能有效分离Dy，分离系数 $\beta_{\text{Dy/Nd}}=410.68$ 。MOHAMMADI等^[77]采用1L三己基(十烷基四)膦酸酯萃取硝酸浸出液中稀土，以EDTA选择性络合分离Nd、Dy，在最优参数条件下，最终制备的 Nd_2O_3 和 Dy_2O_3 纯度分别为99.6%和99.8%。溶剂萃取剂法虽然能生产单一稀土元素的产品，但在萃取过程中，萃取剂自身具有一定毒性，且易受到杂质离子影响而产生乳化现象，阻碍了连续生产。

针对传统萃取剂的问题，离子液体萃取剂逐渐被开发。离子液体萃取剂一般由有机阳离子与无

机、有机阴离子组合而成,以液态盐类形式存在,依靠离子液体与溶液中金属离子结合能力的差异而达到分离富集稀土元素的目的。相较于传统萃取剂,离子液体萃取剂具有分离系数高、循环利用效果好、不挥发、萃取体系稳定等优势,在回收NdFeB废料中有价金属方面越来越受到关注。ZHOU等^[78]设计并合成了新型离子液体 $[P_{66614}]_2[IOPAA]$ 用于回收NdFeB废料浸出液中的稀土元素,以 $[P_{66614}]Cl$ 萃取剂脱除杂质铁,且稀土回收率达到99.85%,并揭示了离子液体萃取剂与稀土结合的机理,如式(12)所示。



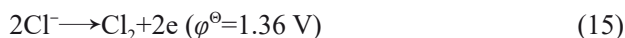
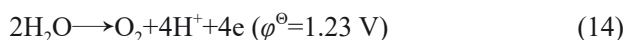
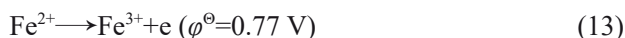
MATSUMIYA等^[79]以 $[P_{2225}][TFSA]$ 离子液体萃取剂分离回收NdFeB废料中的稀土,在最优条件下对Pr、Nd和Dy的萃取率分别为96.7%、97.6%和96.3%。LIN等^[80]采用硝酸溶解铁钕硼废料后,通过调节溶液pH去除杂质铁离子,以合成的离子液体萃取剂 $[A336][NO_3]$ 提取分离溶液中的Nd、Pr和Dy;离子液体与稀土的结合能力由小到大依次为Dy、Pr、Nd,并且加入盐析剂 $NaNO_3$ 能提高离子液体萃取性能。其他学者还合成了 $[C_{12}mim][TFSA]$ 、 $[C_4mim][TFSA]+TBP$ 等离子液体萃取剂,均能有效分离溶液中稀土元素^[81-82]。虽然离子液体萃取剂回收稀土效果显著,但也存在合成成本较高、萃取过程中易损失等弊端。目前,该方法还停留在实验室阶段,离工业生产应用还存在一定距离。

4 其他方法

4.1 电沉积法

在永磁材料NdFeB生产的过程中也会伴随超细钕铁硼废料的产生,相较于传统NdFeB废料,超细NdFeB废料中杂质较少,主要以铁和稀土(>98%,质量分数)为主,同时废料表面污染物少。采用传统火法和湿法处理这类废料时存在较多弊端,其中火法处理消耗能量高,生产成本低;湿法处理需要大量盐酸、草酸等溶解和沉淀剂,生产工艺繁琐且伴随大量废水。在此基础上,借助电化学选择性氧化将Fe(II)转变成Fe(III),再使稀土形成沉淀被回收,即电沉积法^[83-84]。PRAKASH等^[85]采

用如图8所示的装置进行原位电化学氧化反应,研究发现溶液中Fe(II)被氧化的程度与阳极所通的电流关系如图9所示;当电流为1.2 A时,经过4 h氧化后,溶液中99%的Fe(II)被氧化,阳极所涉及反应如式(13)~(15)所示。再经过草酸处理,最终能得到99.2%的稀土氧化物,且稀土回收率超过98%,溶液中残留的Fe(III)也能被循环利用,提高了超细NdFeB废料的利用率。



IRINA等^[86]以硫酸为溶剂处理NdFeB废料,经过电化学氧化处理后,采用 H_2CO_4 使稀土沉淀,从而与Fe分离。对NdFeB废料进行电解前往往需无机酸(HCl、 HNO_3 、 H_2SO_4)将其溶解,经过电解后还需加入草酸沉淀稀土,后续再分离纯化。以氢氟酸做溶剂处理NdFeB废料,生成的稀土氟化物不

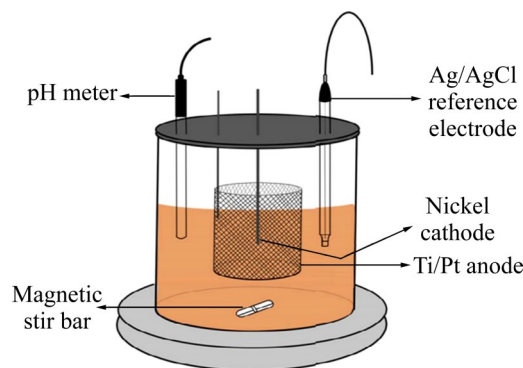


图8 电解装置的示意图^[85]

Fig. 8 Schematic illustration of electrolysis set-up^[85]

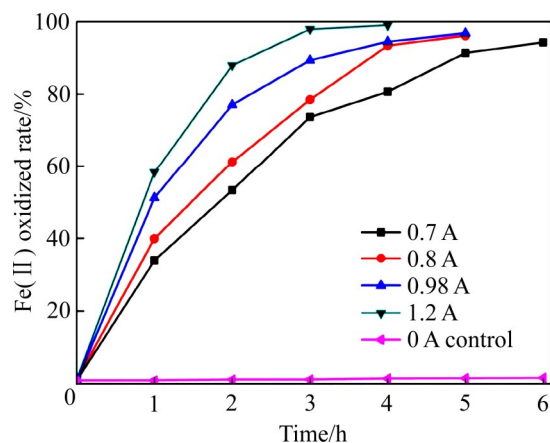


图9 Fe^{2+} 氧化速率与电流的关系

Fig. 9 Relationship between oxidation rate of Fe^{2+} and current

溶于氢氟酸，能直接分离得到稀土沉淀。YANG 等^[87]以 HF 为回收溶剂处理超细 NdFeB 废料，经过一步沉淀最终能得到可以电解的稀土氟化物，极大降低了化学试剂的消耗，是一种更加简便高效的方法。

4.2 生物浸出法

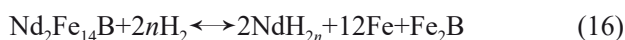
在环保、绿色、高效的生产理念下，传统火法和湿法处理 NdFeB 废料存在能耗过大、化学试剂消耗过多易造成环境污染等问题。生物浸出是在微生物的帮助下以水溶性形式对不溶性金属化合物进行的生物转化，它基于生物氧化和络合作用对金属离子的迁移，所涉及的微生物在此过程中具有多种功能^[88-89]。首先，它们产生 Fe(III) 离子和氢离子，再将它们浓缩在样品材料与细菌细胞之间的界面中，从而提高难溶金属性化合物的溶解度。借助生物浸出处理二次资源已经受到广泛关注，在电子设备、催化剂、荧光粉、电池及金属加工行业的炉渣和煤灰等领域有较好研究和应用^[90-91]。借助生物浸出对 NdFeB 废料进行处理的研究相对较少，但生物浸出法处理二次资源的优势也促使该方法在处理 NdFeB 废料中的研究。ROMY 等^[92]最先开展了生物浸出法处理 NdFeB 废料，对比分析了不同细菌对稀土的浸出效率，研究发现，酸性氧化铁硫杆菌 (*Acidithiobacillus ferrooxidans*) 和氧化亚铁螺旋体 (*Leptospirillum ferrooxidans*) 对 NdFeB 废料中稀土的浸出率最高，其中 Dy、Nd 和 Pr 的浸出率分别为 86%、91% 和 100%。该研究为常规工艺提供了一种可管理、经济高效且环保的替代方法。

生物浸出法处理 NdFeB 废料能极大降低化学试剂消耗，更加绿色环保，更加符合当前社会绿色发展的理念。相较于传统湿法和火法工艺，生物浸出法具有处理量大、成本低、环保等显著优势，是未来发展极具潜力的方法。但是，该技术目前还停留在实验室阶段，离工业应用还有一定差距，还需从菌株筛选、浸出机理等方面开展深入研究。

4.3 氢化法

由于 NdFeB 合金接触 H₂ 后容易发生晶界断裂，以此推演出氢化-歧化-脱氢工艺处理 NdFeB 废料。在处理过程中 NdFeB 废料吸收 H₂，生成氢爆粉，再经歧化脱氢使稀土 Nd 分离，所涉及的反应如式

(16)~(17)所示^[93]。



整个反应处于高温环境中，且温度越高，反应式中 n 越趋于 1。氢化法在处理 NdFeB 废料过程中，Nd 在回收阶段易发生氧化挥发，使其再被用致永磁材料中时，往往会使材料性能下降^[94-95]。因此，在循环利用中还需与新稀土 Nd 搭配使用。该方法当前还处于实验室阶段，但其高效和环保的优势使其成为研究热点。虽然氢化法对废料中 Nd 的回收效果好，但对 Fe 的循环利用较差^[96]。MIURA 等^[97]结合氢化法的优势，提出氢化-碳基铁法回收 NdFeB 废料中稀土和 Fe；废料经过氢化歧化处理，在高温高压条件下以硫作催化剂，最终使 Fe 以 Fe(CO)₅ 的形式被回收，且回收率超过 90%。结合碳基铁法能使废料中 Fe 的循环利用率大幅提高，但也存在反应周期长，生产效率较低。

4.4 机械化学法

传统工艺处理 NdFeB 废料一般需要高温高压条件，存在明显弊端，需要开发回收条件更温和的工艺。机械化学法最早由日本岛根大学提出，在球磨动能的配合下，常温常压下能被硫酸和草酸组成的溶剂高效回收，可得到纯度超过 80% 的 Nd^[98]。该技术的开发使回收工艺条件温和，大大降低回收成本，是稀土循环利用技术的重大突破，具有广泛的应用前景。SASAI 等^[99]将消磁的废烧结 NdFeB 磁体用行星式铣削的方式处理，采用直径为 10 mm 的 ZrO₂ 球在 300 r/min 速度下将其粉碎成粗颗粒，再用盐酸和草酸组成的溶剂回收其中稀土，最终稀土回收率和纯度均超过 95%。经过近几年的发展，机械化学法回收处理 NdFeB 废料的研究取得了一定进展，但离大规模工业生产还存在差距。

5 结论和展望

随着 NdFeB 废料产量的逐年增加，人们对废料中稀土元素进行绿色高效循环利用的意识也在逐渐增强。目前，各国学者对 NdFeB 废料中稀土回收的技术方法进行了大量研究，并取得了丰富的研究成果。不同技术方法的优势和不足如表 1 所示。

虽然对 NdFeB 废料中稀土回收的工艺方法在

表 1 不同技术方法回收 NdFeB 废料中稀土的优势和劣势

Table 1 Advantages and disadvantages of different technical methods for recycling rare earths in NdFeB waste

Method name	Method principle	Disadvantage	Advantage
Chlorination	Rare earth elements can show stronger affinity with chloride ions	Severely oxidized waste has poor recovery	Good recycling effect
Alloy method	Rare earth Nd combines with molten Mg and Al to form an alloy	High requirements for operating equipment and high energy consumption	Get a single rare earth Short process flow
Selective oxidation	Difference of affinity of iron and rare earth for oxygen at different temperatures	High reaction temperature and high energy consumption	Environmentally friendly No chemical reagent consumption
Total solution	Hydrochloric acid dissolves rare earth and other elements in waste	Large reagent consumption, environmental pollution, low product purity	Simple principle and operation
Hydrochloric acid	Control pH of solution so that rare earth oxides preferentially react with hydrochloric acid	Low efficiency High wastewater output	Low reagent consumption Short process
Oxalic acid precipitation	Solubility difference of salts formed by Fe^{2+} and rare earth ions and oxalic acid	High cost Low product purity	Easy operation Simple process
Sulfate double salt method	Rare earth sulfate reacts with Na_2SO_4 to produce double salt precipitation	Harsh reaction conditions polluted environment	Reaction conditions are mild and cost is relatively low
Solvent extraction	Difference in binding ability between rare earth and organic extractant	Easy to emulsify extractant Poor production environment	High productivity Highly targeted
Electrodeposition	Electrochemical oxidation of Fe^{2+} to Fe^{3+} , re-precipitation of rare earth	High power consumption Cumbersome operation	Less chemical reagent consumption, more convenient and efficient
Bioleaching	Migration and transformation of metal ions by microbial oxidation and complexation	High power consumption Cumbersome operation	Large processing capacity, low cost, environmental protection
Hydrogenation	Disproportionation dehydrogenation to separate rare earth Nd	Long reaction time and low efficiency	High recovery rate
Mechanochemical method	With the kinetic energy of ball milling, lower reaction temperature	Research needs to be in-depth Lack of actual basis	Mild process conditions and low cost

不断完善, 且更加绿色高效, 但也存在较多弊端。为了更好地推动 NdFeB 废料中稀土的综合利用, 今后的研究应主要从以下几个方面入手: 1) 开发新的回收工艺, 缩短生产流程, 降低生产成本; 2) 开发并筛选性能更优萃取剂, 尤其是离子萃取剂, 更高效地回收浸出液中的稀土元素, 降低离子液体萃取剂的溶解度, 争取早日实现工业化应用; 3) 对微生物浸出的研究需要进一步深入, 培育性能更优、针对性更强、稳定性更高的菌种, 使其能在更温和的条件回收废料中的稀土元素; 4) 深入研究机械化

学法处理 NdFeB 废料技术, 探究其最佳工艺条件, 在最低能耗条件下回收稀土; 5) 由于从 NdFeB 废料中回收稀土工艺的成本整体较高, 急需开发低成本的工艺技术来推动稀土回收产业的发展。

6 结语

我国虽然是稀土大国, 但肆意的开采使不可再生的稀土资源消耗急剧增大, 急需加大力度对二次资源中稀土的循环利用。这不仅能极大缓解稀土的

供应压力,还能提高企业的经济效益。相较于欧美等发达国家,我国在稀土循环领域还有巨大差距,处理技术和意识也较落后。随着相关政策的出台,我国学者对二次资源中稀土循环利用意识逐渐增强,已经积极开展相关研究,将共同促进我国对FeNdB废料中稀土循环利用技术的提升。

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Current status and prospect of recycling and utilization of rare earth in NdFeB permanent magnet waste

SONG Qiang^{1,2,3}, TONG Xiong^{1,2}, XIE Xian^{1,2}, ZHANG Wen-jie^{1,2}, CAO Yang^{1,2},
DU Yun-peng^{1,2}, CHENG Ya-zhi^{1,2}

(1. Faculty of Land and Resources Engineering, Kunming University of Science and Technology,
Kunming 650093, China;

2. National and Local Joint Engineering Research Center for Green Comprehensive Utilization of
Metal Mine Tailings Resources, Kunming 650093, China;

3. Yunnan Yuankuang Technology Development Co., Ltd., Kunming 650093, China)

Abstract: Neodymium iron boron (NdFeB) permanent magnet materials are widely used in many fields. In the process of producing NdFeB permanent magnet materials, a large amount of waste will be generated. Direct discarding will not only pollute the environment, but also waste secondary resources. This article summarized the technical status of the recycling of rare earths in NdFeB permanent magnet waste. Comparative analysis of the current situation and shortcomings of fire methods in industrial applications such as chlorination method, alloy method, and selective oxidation method was carried out. The research status of wet methods, such as solvent extraction method, has deeply analyzed the limitations and advantages of different methods also was carried out. At the same time, the research status of new technology methods such as electrodeposition method, biological leaching method, hydrogenation method and mechanochemical method were introduced. On this basis, the future development direction of recycling and recycling of rare earth technology in NdFeB permanent magnet waste was prospected.

Key words: NdFeB permanent magnet material; waste; rare earth; recycling and utilization; fire method; wet method

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Corresponding author: XIE Xian; Tel: +86-15987188290; E-mail: kgxianxie@126.com

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