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# Effects of polyaniline on electrochemical properties of composite inert anodes used in zinc electrowinning

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**Abstract:** In order to search for a suitable anode material used in zinc electrowinning in place of Pb–Ag alloy, Al/Pb–PANI (polyaniline)–WC (tungsten carbide) composite inert anodes were prepared on aluminum alloy substrate by double pulse electrodeposition (DPE) of PANI and WC particles with  $Pb^{2+}$  from an original plating bath. Thereafter, anodic polarization curves, cyclic voltammetry curves and Tafel polarization curves for the composite inert anodes obtained under different PANI concentrations in the original plating bath were measured, and the microstructural features were also investigated by scanning electron microscopy (SEM). The results show that Al/Pb–PANI–WC composite inert anode obtained under PANI concentration of 20 g/L in the original plating bath possesses uniform microstructures and composition distributions, higher electrocatalytic activity, better reversibility of electrode reaction and corrosion resistance in a synthetic zinc electrowinning electrolyte of 50 g/L Zn<sup>2+</sup>, 150 g/L H<sub>2</sub>SO<sub>4</sub> at 35 °C. Compared with Pb–1%Ag alloy, the overpotential of oxygen evolutions for the composite inert anode are decreased by 185 mV and 166 mV, respectively, under 500 A/m<sup>2</sup> and 1000 A/m<sup>2</sup>.

**Key words:** composite inert anodes; double pulse electrodeposition; anodic polarization curves; cyclic voltammetry curves; Tafel polarization curves; microstructures

#### **1** Introduction

Zinc is mainly extracted from its sulfide ores, oxide ores or other secondary resources by means of electrowinning process for hydrometallurgy. Generally, the electrode materials used in zinc electrowinning must meet the following requirements of good electroconductivity, mechanical strength and electrocatalytic activity, excellent corrosion resistance and long service life. At present, only Pb-Ag alloy anode in which Ag content ranges form 0.5% to 1.0% (mass fraction), is used extensively in zinc electrowinning, but it also has some shortages of higher overpotential of oxygen evolution, worse conductivity and mechanic performance [1-5]. The overpotential of oxygen evolution, current efficiency and corrosion rate for

Pb-Ag-Sb, Pb-Ca-Sn, Pb-Ag-Ca and Pb-Co alloy anodes used in zinc electrowinning were investigated and some valuable results have been obtained [6–8].

PANI particle has been intensively researched in recent years owing to its high conductivity, good electrocatalytic activity and environment stability, and has a large variety of applications in the fields of light-emitting materials, electronic device materials, chemical sensor materials and electrode materials [9–13]. WC particle can increase distortion resistance and decrease overpotential of oxygen evolution in zinc electrowinning when deposited into matrix metal Pb or metal oxidation PbO<sub>2</sub>. Compared with direct current electrodeposition (DCE), pulse electrodeposition (PE) with higher instantaneous current density can increase cathodic activation polarization and decrease cathodic concentration polarization, which is easier to make out

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metal matrix composite materials in the fine grained structures by means of relaxation of pulse current [14–18]. In order to search for a suitable anode material used in zinc electrowinning in place of Pb–Ag alloy, a new kind of Al/Pb–PANI–WC composite inert anode was prepared by double pulse electrodeposition (DPE) and it has been found to a potential anode material. In this research, effects of PANI concentrations in an original plating bath on electrochemical properties and microstructural features for the composite inert anodes were studied.

#### 2 Experimental

#### 2.1 Preparation of composite inert anodes

Al/Pb–PANI–WC composite inert anodes were prepared on aluminum alloy substrate by DPE from an original plating bath. The dimensions of plating cell were  $80 \text{ mm}(L) \times 60 \text{ mm}(W) \times 130 \text{ mm}(H)$ ; a pair of electrolytic lead sheets with dimensions of 30 mm(L) × 3 mm(W) × 100 mm(H) were used as electrodepositing anodic materials, and were connected with anodic wire of DPE supply; aluminum alloy sheet with dimensions of 30 mm(L)×2 mm(W)×60 mm(H) was used as cathodic material, and was connected with cathodic wire of DPE supply; the electrode spacing between anodic material and cathodic material was 40 mm.

The original plating bath compositions used for electrodepositing Al/Pb-PANI-WC composite inert anodes were as follows: 180 g/L Pb(AC)<sub>2</sub>, 220 mL/L HBF<sub>4</sub>, 20 g/L H<sub>3</sub>BO<sub>3</sub>, 1.0 g/L gelatin, 0.2 g/L thiourea, 5 mL/L polyethylene glycol, 20 g/L WC and 0-25 g/L PANI. The plating temperature was maintained at 35 °C, the plating pH value was about 1.0. The waveforms of DPE supply used for electrodepositing the composite inert anode from the original plating bath were as follows: forward and reverse pulse duty cycles were 10% and 30% respectively, forward and reverse pulse average current densities were 4 A/dm<sup>2</sup> and 0.4 A/dm<sup>2</sup> respectively, and forward and reverse pulse working time were 200 ms and 20 ms, respectively. The electrodeposition time was 1.5 h. Thereafter, the composite inert anodes were used for measuring of electrochemical properties and surface microstructural features.

To guarantee better dispersion of PANI and WC particles in the original plating bath and in the composite inert anodes, the original plating bath was dispersed by ultrasonic device with 2 A for 30 min before DPE. After that, the mechanical stirring was used for the original plating bath in DPE experiments and the stirring speed was controlled at 150 r/min.

#### 2.2 Measurement and analysis

The electrochemical workstation (CHI760C) with

three-electrode system was used for measuring the anodic polarization curves, cyclic voltammetry curves and Tafel polarization curves for the composite inert anodes in a synthetic zinc electrowinning electrolyte of 50 g/L  $Zn^{2+}$ , 150 g/L  $H_2SO_4$  at 35 °C. The auxiliary electrode was graphite, the reference electrode was a saturated calomel electrode, the working electrode was the composite inert anode and the working areas were 1.0 cm<sup>2</sup>. The working electrode and auxiliary electrode were connected with KCl agar salt bridge, and their electrode spacing was 30 mm. Scanning electron microscope (SEM, XL30 ESEM-TEP+EDAX) was used for determining surface microstructures and composition distributions of the composite inert anodes.

#### **3 Results and discussion**

#### 3.1 Anodic polarization curves and kinetic parameters of oxygen evolution

At a constant scan rate of 5 mV/s, anodic polarization experiments for Al/Pb–PANI–WC composite inert anodes obtained under different PANI concentrations in the original plating bath, were carried out in a synthetic zinc electrowinning electrolyte of 50 g/L  $Zn^{2+}$ , 150 g/L  $H_2SO_4$  at 35 °C, and the results are shown in Fig. 1.



Fig. 1 Anodic polarization curves for composite inert anodes obtained under PANI concentrations in original plating bath

As shown in Fig. 1, the relationships of PANI concentrations in the original plating bath and anodic polarization curves have identical characteristics in the potential ranges of 0-2.9 V, but PANI concentrations in the original plating bath have no obvious effects on the initial anodic behavior for the composite inert anodes in the potential ranging from 0 V to 1.8 V. It can also be seen that the potentials of oxygen evolution for the composite inert anodes obtained under PANI concentrations of 0 g/L and 5 g/L in the original plating bath, are higher in the potential ranging from 1.8 V to

2.9 V. Increasing PANI concentrations from 0 to 20 g/L in the original plating bath leads to the decrease of the potential of oxygen evolution in the range of high potential, and it reaches the lowest value under PANI concentration of 20 g/L, displaying better electrocatalytic activity. Thereafter, the potential of oxygen evolution begins to increase when PANI concentration is increased from 20 g/L to 25 g/L in the original plating bath.

According to Fig. 1, the kinetic parameters of oxygen evolution calculated by Tafel equation  $(\eta = a + b \lg J_0)$  are listed in Table 1. The value of  $J_0$  for the composite inert anode obtained under PANI concentration of 20 g/L in the original plating bath, is the highest  $(4.98 \times 10^{-7} \text{ A/cm}^2)$ , and higher than that for other composite inert anodes, displaying that the anodic reaction is easier to happen and its electrocatalytic activity is the highest when current passes through the anode. In addition, it can be seen that in the synthetic zinc electrowinning electrolyte of 50 g/L Zn<sup>2+</sup>, 150 g/L  $H_2SO_4$  at 35 °C, the values of  $\eta$  for the composite inert anodes obtained under PANI concentrations of 20 g/L in the original plating bath, are 0.975 V and 1.034 V under 500  $A/m^2$  and 1000  $A/m^2$ , respectively. Under above current density conditions, the values of  $\eta$  for Pb-1%Ag alloy prepared in laboratory are 1.160 V and 1.200 V, respectively. Therefore, compared with Pb-1%Ag alloy, the values of  $\eta$  for the composite inert anodes are decreased by 185 mV and 166 mV under 500 A/m<sup>2</sup> and  $1000 \text{ A/m}^2$ , respectively.

 
 Table 1 Oxygen evolution kinetic parameters of composite inert anodes obtained under different PANI concentrations in original plating bath

PANI concentrations in original plating bath/(g·L <sup>-1</sup> )	$\eta$	V	а	b	$J_0/$ (10 <sup>-7</sup> A·cm <sup>-2</sup> )
	$500 \ A/m^2$	1000 A/m <sup>2</sup>			
0	1.079	1.137	1.329	0.192	1.19
5	1.070	1.127	1.318	0.191	1.26
10	1.049	1.108	1.304	0.196	2.22
15	1.017	1.075	1.266	0.191	2.35
20	0.975	1.034	1.229	0.195	4.98
25	0.995	1.053	1.246	0.193	3.50

Note:  $\eta$ —Overpotential of oxygen evolution;  $J_0$ —Exchange current density; a and b—Constants

#### 3.2 Cyclic voltammetry curves

At a constant scan rate of 10 mV/s, cyclic voltammetric experiments for Al/Pb–PANI–WC composite inert anodes obtained under different PANI concentrations in the original plating bath, were carried out in the synthetic zinc electrowinning electrolyte of 50 g/L  $Zn^{2+}$ , 150 g/L  $H_2SO_4$  at 35 °C, and the results are shown in Fig. 2.



Fig. 2 Cyclic voltammetry curves for composite inert anodes obtained under different PANI concentrations in original plating bath

As shown in Fig. 2, one anodic oxidation peak in the forward scan and one cathodic reduction peak in the reverse scan appear in the cyclic voltammetry curves for Al/Pb-PANI-WC composite inert anodes obtained under different PANI concentrations in the original plating bath. The anodic oxidation peak should be the conversion peak for Pb/PbO<sub>2</sub>, and the cathodic reduction peak should be the conversion peak for PbO2/Pb. The potential difference between Pb/PbO<sub>2</sub> oxidation peak and PbO<sub>2</sub>/Pb reduction peak for the composite inert anode obtained under the PANI concentration of 20 g/L in the original plating bath, is only 0.41 V, and it is also the lowest among these composite inert anodes, which can be concluded that the reversibility of electrode reaction is better in the synthetic zinc electrowinning electrolyte of 50 g/L Zn<sup>2+</sup>, 150 g/L H<sub>2</sub>SO<sub>4</sub> at 35 °C.

#### 3.3 Tafel polarization curves

At a constant scan rate of 10 mV/s, Tafel polarization experiments for Al/Pb–PANI–WC composite inert anodes obtained under different PANI concentrations in the original plating bath, were carried out in the synthetic zinc electrowinning electrolyte of 50 g/L  $Zn^{2+}$ , 150 g/L  $H_2SO_4$  at 35 °C, and the results are shown in Fig. 3, the corrosion potential and corrosion current are listed in Table 2.

As shown in Table 2, the corrosion potential for the composite inert anode increases with the rise of PANI concentrations from 0 g/L to 20 g/L in the original plating bath and it reaches the highest value (-0.533 V) under the PANI concentration of 20 g/L. In the meantime, the corresponding corrosion current of the composite inert anode is also the lowest (1.05 mA), displaying better corrosion resistance in the synthetic zinc electrowinning electrolyte of 50 g/L Zn<sup>2+</sup>, 150 g/L H<sub>2</sub>SO<sub>4</sub> and 35 °C. Thereafter, the corrosion potential begins to

decrease and corrosion current begins to increase with further increasing PANI concentrations from 20 g/L to 25 g/L in the original plating bath, showing that the corrosion resistance for the composite inert anode becomes bad.



**Fig. 3** Tafel polarization curves for composite inert anodes obtained under different PANI concentrations in original plating bath

Table	2	Corros	ion	pote	ential	and	corros	ion	curren	nt	for
compos	site	inert	anc	odes	obtai	ined	under	dif	ferent	P/	٩NI
concent	trati	ions in d	origi	nal p	lating	bath					

PANI concentration in original plating bath/( $g$ ·L <sup>-1</sup> )	Corrosion potential/V	Corrosion current/mA		
0	-0.617	8.28		
5	-0.598	8.25		
10	-0.565	6.63		
15	-0.546	1.31		
20	-0.533	1.05		
25	-0.612	8.82		

## 3.4 Microstructural features and composition distributions

Surface microstructural features of Al/Pb–PANI–WC composite inert anodes obtained under different PANI concentrations in the original plating bath, are shown in Fig. 4, and the composition distribution results of line scanning are shown in Fig. 5 and Table 3.



**Fig. 4** Surface microstructural features for composite inert anodes obtained under different PANI concentrations: (a) 0 g/L; (b) 5 g/L; (c) 10 g/L; (d) 15 g/L; (e) 20 g/L; (f) 25 g/L

1696



**Fig. 5** Composition distributions for composite inert anodes obtained under different PANI concentrations: (a) 0 g/L; (b) 5 g/L; (c) 10 g/L; (d) 15 g/L; (e) 20 g/L; (f) 25 g/L

 Table 3 Results of line scanning for composite inert anodes

 obtained under different PANI concentrations in bath

PANI concentration	Mass fraction/%				
in bath/( $g \cdot L^{-1}$ )	Pb	Ν	WC	Other element	
0	88.31	-	11.69	-	
5	83.68	1.76	9.64	4.92	
10	82.68	2.38	10.19	4.75	
15	82.46	2.65	10.46	4.43	
20	80.12	3.13	12.85	3.90	
25	80.23	2.57	13.62	3.58	

Note: N is one of orgnic components for PANI.

It can be seen that increasing PANI concentration from 0 g/L to 20 g/L in the original plating bath leads to the refinement in the grained structures and the improvement of composition fluctuation. In the meantime, it also increases mass fractions for PANI particles and WC particles in the composite inert anodes. The main reasons may be that increasing PANI concentration from 0 g/L to 20 g/L in the original plating bath is favorable for their enrichment and deposition as the core on the cathodic surface under the function of mechanical stirring and electrical forces, which brings on a large amount of nucleation points for matrix metal Pb, increases deposition rate and deposition amount of solid particles, inhabits the continuous growth of Pb grains and refines the grains. While when PANI concentration is increased from 20 g/L to 25 g/L in the original plating, higher particle concentration in the original plating bath results in serious coacervation for solid particles in the composite inert anodes owing to the fact that the increase of electrolyte viscidity and the coacervation of solid particles absorbed on the cathodic surface. Therefore, the structural defects such as cavities and cracks and composition fluctuations, are obvious, showing that too higher PANI concentration in the original plating bath is not favorable to preparing the uniform composite materials.

#### **3.5 Discussion**

Composite electrodeposition is a valuable new surface intensification technology to obtain metal-matrix composite materials by making inorganic and organic particles co-deposit with metal or alloy [19–21]. The composite materials are made up of matrix metal and the second phase particles which are dispersed evenly within matrix metal, possessing comprehensive performances of matrix metal and the second phase particles. Especially, pulse electrodeposition is found to be an effective means of controlling microstructures and properties of the composite materials by varying pulse parameters owing to higher instantaneous current density [22–25], and has received a considerable attention in recent years [26,27].

The above research results show that Al/Pb-PANI-WC composite inert anode obtained under PANI concentration of 20 g/L in the original plating bath possesses a higher electrocatalytic activity and lower overpotential of oxygen evolution in the synthetic zinc electrowinning electrolyte of 50 g/L Zn<sup>2+</sup>, 150 g/L H<sub>2</sub>SO<sub>4</sub> at 35 °C, which is related to the characteristics of solid particles, the distribution of solid particles in the composite inert anodes and the electrochemical active sites amounts used for oxidation-reduction transition on the surface of the composite inert anodes. On one hand, PANI particle is a typical conducting polymer with organic conjugated structure, and its macroscopic conductivity is affected by conjugate degree and mutual stack mode of molecular chain [28,29]. PANI doped with inorganic acid possesses a higher electrical conductivity owing to the fact that the extension of molecular chain structure leads to high conjugate degree and close chain packing is favorable to the transmission of charge in the chain and between the chain [30]. The conductive mechanism of doped PANI differs from metal and semiconductor, in which the carriers are composed of "delocalization"  $\pi$  electrons and solitons, polarons or bipolarons formed by doping [31], which has been described by peace model [32,33], granular metal island model [34-36] and monopole and bipolar sub-transformation model [37]. Meanwhile, PANI has an active surface that exceeds geometric surface and can play a role in selective catalysis to some certain when used as the electrode materials, such as the electrocatalytic oxidation of ascorbic acid at polyaniline film modified glassy carbon electrodes [38], the electrocatalysis of polyaniline film on Fe [II] and Sb [II], the synergistic effects of electrocatalytic oxidation of polyaniline on small organic molecules [39-41] and the same electrocatalytic activity for Pb/PANI and Pt/PANI in acid solutions [42]. On the other hand, WC particle has the electrochemical characteristics that is similar to platinum owing to the fact that the existing of carbide changes the electronic surface properties of tungsten, possessing a higher electrochemical activity, better catalytic activity and conductivity in a acidic medium low temperature [43–46]. For example, the reduction of activation energy in the reaction control steps improves the electrocatalytic activity of hydrogen evolution for Pb–WC composite anode [47], the deposition of WC particles into Cu/PbO<sub>2</sub> composite anode changes deposition mode and preferred orientation of PbO<sub>2</sub>, leading to that the electrocatalytic activity of oxygen evolution reaction for PbO<sub>2</sub>–WC composite anode in 0.5 mol/L H<sub>2</sub>SO<sub>4</sub> solution is increased nearly by one-fold [48].

Therefore, the deposition of PANI particles and WC particles as conductive matrix and electrocatalytic activity substance and their dispersion distributions obviously improve the electrocatalytic activity and decrease the overpotential of oxygen evolution for Al/Pb-PANI-WC composite anode in the synthetic zinc electrowinning electrolyte of 50 g/L  $Zn^{2+}$ , 150 g/L H<sub>2</sub>SO<sub>4</sub> at 35 °C. In addition, high deposition amounts of PANI particles and WC particles in the composite inert anode obtained under PANI concentration of 20 g/L, provide more electrochemical active sites used for oxidationreduction transition on the surface of the composite inert anodes, displaying a higher electrocatalytic activity and lower overpotential of oxygen evolution in the synthetic zinc electrowinning electrolyte of 50 g/L Zn<sup>2+</sup>, 150 g/L H<sub>2</sub>SO<sub>4</sub> at 35 °C.

#### 4 Conclusions

1) Al/Pb–PANI–WC composite inert anode obtained by DPE under PANI concentration of 20 g/L in the original plating bath, is a suitable anode material used in zinc electrowinning in place of Pb–Ag alloy, possessing uniform microstructures, composition distributions and less microstructural defects.

2) In the synthetic zinc electrowinning electrolyte of 50 g/L  $Zn^{2+}$ , 150 g/L  $H_2SO_4$  at 35 °C, the composite inert anode possesses a higher electrocatalytic activity, lower overpotential of oxygen evolution, better reversibility of electrode reaction and corrosion resistance. Compared with Pb–1%Ag alloy, the overpotentials of oxygen evolution for the composite inert anode are decreased by 185 mV and 166 mV under 500 A/m<sup>2</sup> and 1000 A/m<sup>2</sup>, respectively.

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### 聚苯胺对锌电积用复合惰性阳极材料电化学性能的影响

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摘 要:为了寻找一种可以替代锌电积用 Pb-Ag 合金的阳极材料,通过 PANI(聚苯胺)、WC(碳化钨)颗粒与 Pb<sup>2+</sup> 的双脉冲电沉积,在 Al 合金基体上制备了 Al/Pb-PANI-WC 复合惰性阳极材料。测试了镀液中不同 PANI 浓度下制备的惰性阳极材料的阳极极化曲线、循环伏安曲线和塔菲尔极化曲线,采用扫描电镜考察复合惰性阳极材料的 微观组织特征。结果表明:当将制备镀液中 PANI 浓度控制在 20 g/L 时,Al/Pb-PANI-WC 复合惰性阳极材料的 微观组织和成分分布均匀,在含 50 g/L Zn<sup>2+</sup>、150 g/L H<sub>2</sub>SO<sub>4</sub> 的 35 ℃ 锌电积液中具有较高的电催化活性、较好的 电极反应可逆性和耐腐蚀性,在电流密度 500 A/m<sup>2</sup>和 1000 A/m<sup>2</sup>下的析氧过电位与 Pb-1%Ag 合金相比分别降低 了 185 mV 和 166 mV。

关键词:复合惰性阳极材料;双脉冲电沉积;阳极极化曲线;循环伏安曲线;塔菲尔极化曲线;微观组织

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