



# Hydrogen storage properties of magnesium hydride catalyzed by Ni-based solid solutions

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**Abstract:** The Ni–25%X (X=Fe, Co, Cu, molar fraction) solid solutions were prepared and then doped into MgH<sub>2</sub> through high-energy ball milling. The initial dehydrogenation temperatures of MgH<sub>2</sub>/Ni–25%X composites are all decreased by about 90 °C relative to the as-milled pristine MgH<sub>2</sub>. The Ni–25%Co solid solution exhibits the most excellent catalytic effect, and the milled MgH<sub>2</sub>/Ni–25%Co composite can release 5.19 wt.% hydrogen within 10 min at 300 °C, while the as-milled pristine MgH<sub>2</sub> can only release 1.78 wt.% hydrogen. More importantly, the dehydrogenated MgH<sub>2</sub>/Ni–25%Co composite can absorb 5.39 wt.% hydrogen at 275 °C within 3 min. The superior hydrogen sorption kinetics of MgH<sub>2</sub>/Ni–25%Co can be ascribed to the actual catalytic effect of in-situ formed Mg<sub>2</sub>Ni(Co) compounds. First-principles calculations show that the hydrogen absorption/desorption energy barriers of Mg/MgH<sub>2</sub> systems decrease significantly after doping with transition metal atoms, which interprets well the improved hydrogen sorption properties of MgH<sub>2</sub> catalyzed by Ni-based solid solutions.

**Key words:** MgH<sub>2</sub>; Ni-based solid solutions; catalytic effect; hydrogen storage properties; first-principles calculations

## 1 Introduction

The traditional fossil fuels, such as coal, oil, and natural gas, have become a powerful driving force for the development of the world economy since the second industrial revolution. Especially from the beginning of the 21st century, the trade activities between countries become increasingly frequent with the development of economic globalization, making the demand for energy in human society continue to expand. However, the current use of energy by countries around the world is still at the level of traditional fossil energy [1]. Their massive use has brought many environment problems, such as global warming, air pollution,

and water pollution [2]. In order to realize the sustainable development of human society, it is urgent to seek a cheap, clean, and renewable energy source. In the past few decades, the researchers have conducted many explorations on replacing traditional fossil fuels with clean and renewable energy sources, such as wind energy, tidal energy, geothermal energy, solar energy, nuclear energy and hydrogen energy [3]. Among them, hydrogen energy is considered to be the most ideal clean energy in the future due to its wide range of sources, high energy density, clean and non-toxic combustion products [4–7].

Although hydrogen energy exhibits the broad development prospects, providing safe and efficient hydrogen storage methods is still the key bottleneck

for the realization of hydrogen economy. The currently used hydrogen storage methods are mainly composed of gaseous, liquid and solid-state hydrogen storage [8–12]. Among solid-state hydrogen storage methods, metal hydrides are widely favored by researchers owing to their safety and high efficiency. A large number of studies have shown that magnesium hydride ( $\text{MgH}_2$ ) is a potential solid-state hydrogen storage material among numerous metal hydrides due to its high reversible hydrogen mass capacity (7.6 wt.%), high volume capacity (110 g/L), abundant raw material sources and low cost [13,14].

Despite many advantages of  $\text{MgH}_2$ , its high thermodynamic stability, slow hydrogen sorption kinetics and poor cycle performance make its wide application face huge challenges [15,16]. In the past few decades, the researchers have performed numerous modification studies to improve the hydrogen storage properties of  $\text{MgH}_2$ . So far, the modification strategies can be mainly divided into catalyzing [17–28], nanosizing [29–34] and alloying [35–40], etc., among which catalyzing is one of the most effective modification means. A variety of catalysts, such as transition-metal (e.g., Ti, V, Nb, Fe, Co, Ni, Cu, Zn) and their compounds (e.g., hydrides, carbides, nitrides, oxides, fluorides, halides), intermetallics, and some nonmetallic materials (e.g., graphite, graphene, carbon nanotubes) have been reported to play significant roles in enhancing the hydrogen storage properties of  $\text{MgH}_2$  [17]. In particular, the Ni-based catalysts show superior catalytic effect on the dehydrogenation/hydrogenation kinetics of  $\text{MgH}_2$ . For example, XIE et al [41] systematically investigated the effects of Ni on the dehydrogenation performance of  $\text{MgH}_2$ . They found that Ni facilitated the nucleation of magnesium phase and accelerated the recombination of hydrogen atoms during the dehydrogenation of  $\text{MgH}_2$ , and the activation energy decreases with increasing nickel content. Based on the excellent catalytic effect of metal Ni, the researchers further studied the synergistic catalytic effect of Ni and carbon materials on  $\text{MgH}_2$ . For example, MENG et al [17] reported an electrospinning-based reduction approach to in situ generate nanostructured nickel catalyst in carbon nanofibers ( $\text{Ni@C}$ ). They found that the prepared  $\text{Ni@C}$  showed a remarkable catalytic effect on improving the hydrogen storage

properties of  $\text{MgH}_2$ . Compared with the as-milled  $\text{MgH}_2$ , the dehydrogenation capacity of the  $\text{MgH}_2$ –10wt.%Ni@C composite was observably increased. Simultaneously, the dehydrogenation activation energy of  $\text{MgH}_2$ –10wt.%Ni@C was 93.08 kJ/mol, which was 94.33 kJ/mol lower than that of the as-milled  $\text{MgH}_2$ . YAO et al [20] prepared uniformly dispersed Ni nanoparticles (NPs) anchored on reduced graphene oxide ( $\text{Ni@rGO}$ ) to catalyze the dehydrogenation/hydrogenation of  $\text{MgH}_2$ . The onset dehydrogenation temperature of  $\text{MgH}_2$  decreased from 251 to 190 °C. Meanwhile, HUANG et al [42] found that the  $\text{MgH}_2$ + 10wt.%Ni@C-MXene also exhibited high cycling stability and eminent hydrogen sorption kinetics.

The researchers further explored the role of Ni-based catalysts in improving the hydrogen storage properties of  $\text{MgH}_2$  based on the excellent catalytic effect of metal Ni and carbon materials. For example, CHENG et al [43] synthesized bimetallic Pd–Ni nanoparticles supported by mesoporous carbon material CMK-3 ( $\text{Pd}_{30}\text{Ni}_{70}/\text{CMK-3}$ ) through hydrogen reduction methods and solution impregnation. They found that the initial dehydrogenation temperature of  $\text{MgH}_2$ – $\text{Pd}_{30}\text{Ni}_{70}/\text{CMK-3}$  decreased from 593 K of pristine  $\text{MgH}_2$  to 435 K, and the hydrogen storage properties of  $\text{MgH}_2$  at low temperatures were improved significantly. They attributed the enhanced hydrogen storage properties of  $\text{MgH}_2$  to the synergistic effects of destabilization and catalysis of nano-dispersed Pd and Ni particles. In addition, the original core-shell  $\text{CoNi@C}$  bimetallic nanoparticles were also used to improve the dehydrogenation/hydrogenation kinetics of  $\text{MgH}_2$ . ZHAO et al [44] showed that the dehydrogenation of the  $\text{MgH}_2$ –8wt.%CoNi@C started at 173 °C, and the dehydrogenation capacity was 5.83 wt.% within 1800 s at 275 °C. More importantly, the system could absorb 4.83 wt.% hydrogen even at 1800 s and a low temperature of 100 °C. They suggested that the reversible phase transitions of  $\text{Mg}_2\text{Co}/\text{Mg}_2\text{CoH}_5$  and  $\text{Mg}_2\text{Ni}/\text{Mg}_2\text{NiH}_4$ , and the confinement effect of carbon shell were the key factors for the obvious improvement of hydrogen storage properties of  $\text{MgH}_2$ . In our recent work [45], the modification effects of NiCu solid solutions with different molar ratios on improving hydrogen storage properties of  $\text{MgH}_2$  were systematically investigated. It was found that the  $\text{MgH}_2/$

Ni–50%Cu system could not only release 5.14 wt.% hydrogen within 15 min at 300 °C, but also absorb 4.37 wt.% hydrogen at 250 °C within 30 min. The enhanced hydrogen sorption kinetics of  $\text{MgH}_2/\text{Ni–50\%Cu}$  mainly attributes to the “hydrogen spillover” effect of in-situ formed  $\text{Mg}_2\text{Ni}(\text{Cu})$  phases.

In view of the excellent catalysis of Ni-based solid solution, we further studied and compared the effects of NiCo, NiCu and NiFe solid solutions on the hydrogen storage properties of  $\text{MgH}_2$  in this work. According to the knowledge of phase diagram, Cu and Fe can realize infinite solid solution in Ni, while the maximum molar fraction of Co in Ni solid solution is 25%. Thus, the Ni–25%Co, Ni–25%Cu and Ni–25%Fe solid solutions were prepared by high-energy ball milling in this work. Then, the catalytic effects of these solid solutions on the hydrogen absorption/desorption properties of  $\text{MgH}_2$  were investigated and compared. Furthermore, first-principles calculations were performed to explain the corresponding catalysis mechanisms of Ni-based solid solutions. The obtained results will enrich the Ni-based solid solution catalysts system and provide an important guidance for designing more transition metal solid solutions to improve the hydrogen storage properties of magnesium-based and other metal-based hydrides.

## 2 Experimental

### 2.1 Samples preparation

In this work, the Fe powder (99.5 wt.%), Co powder (99.8 wt.%), Ni powder (99.8 wt.%) and Cu powder (99.9 wt.%) were obtained from Alfa Aesar. The  $\text{MgH}_2$  powder (98 wt.%) was commercially got from Saiamin Chemical Co., Ltd. All as-received powders were directly used without further purification. Firstly, the Ni–25%X (X=Fe, Co, Cu) solid solutions were prepared by high-energy ball milling (Ni/X molar ratio was 3:1). For comparison, the pristine Ni was also milled under the same condition. Then, the obtained Ni–25%X (X=Fe, Co, Cu) solid solutions and Ni powder after ball milling were further mixed with  $\text{MgH}_2$  with a mass ratio of 1:9. At the same time, the as-milled pristine  $\text{MgH}_2$  was used to compare with these catalysts-doped systems under the same ball milling conditions. The mill used was a QM–3C high-speed vibration ball

mill with a stainless-steel tank. The balls of 10 mm in diameter made of stainless steel (SUS304) were employed. All samples were ball milled at 1000 r/min of rotational speed for 5 h with the ball to powder mass ratio of 30:1. In order to avoid the excessively temperature elevation during the ball milling, these samples were stopped to cool for 10 min at every 1 h. All operations on the samples were carried out under high purity argon (99.999 vol.%) atmosphere in a glove box with water/oxygen concentrations lower than 0.1 r/min.

### 2.2 Samples characterization

The phase structures of samples were characterized by using X-ray diffraction (XRD) apparatus (Rigaku D/Max 2500) with  $\text{Cu K}_\alpha$  radiation at a scanning rate of 0.02 (°)/0.15 s, in the  $2\theta$  range between 5° and 90°. Diffraction data were recorded at room temperature, and the current and voltage were 250 mA and 40 kV, respectively. The Rietveld refinement method based on XRD patterns was used to calculate and refine the lattice parameters of different phases. Scanning electron microscopy (SEM) (TESCAN MIRA 3LMU/X-Max20/H1002) equipped with energy dispersive spectrometer (EDS) microanalysis and a backscattered mode, and transmission electron microscopy (TEM) (JEM2100F) were employed to characterize the microstructures of samples. The non-isothermal dehydrogenation performance (temperature programmed desorption (TPD)) and isothermal hydrogen adsorption/desorption kinetics of samples were tested using a Sieverts type volumetric apparatus (University of Science and Technology Beijing, and Yongxing Technology Co., Ltd). The samples were heated from room temperature to 500 °C at a heating rate of 3 °C/min during TPD test. The isothermal hydrogen absorption/desorption kinetics curves of samples were obtained at different temperatures (i.e., 250, 275 and 300 °C, respectively). The initial hydrogen pressures of  $\text{MgH}_2/\text{Ni–25\%X}$  (X=Fe, Co, Cu) systems for hydrogen desorption and absorption are 0.003 and 3.0 MPa, respectively.

### 2.3 Computational methods

All calculations were carried out by using first-principles plane-wave pseudopotential method as implemented in Cambridge Sequential Total Energy Package (CASTEP) code based on density

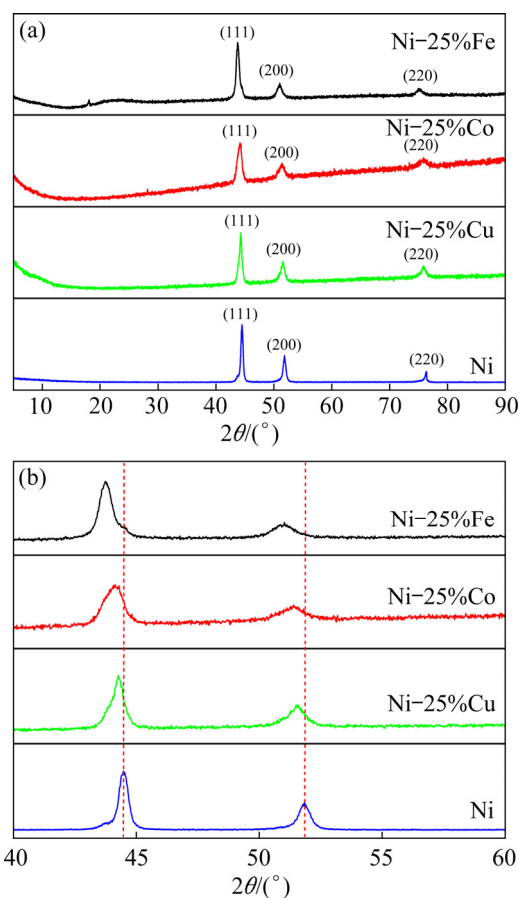
functional theory (DFT) [46]. The Generalized Gradient Approximation (GGA) of Perdew-Burke-Ernzerhof (PBE) functional [47] was adopted to describe the exchange-correlation energy and the plane wave cutoff energy with 400 eV was employed in this work. The convergences criteria of the variable-cell relaxation and transition state (TS) search were  $1.0 \times 10^{-5}$  eV/atom, 0.03 eV/Å, 0.05 GPa and 0.001 Å for energy, force, stress and displacement, respectively.

### 3 Results and discussion

#### 3.1 Structural and morphological characterizations of Ni-25%X solid solutions and MgH<sub>2</sub>/Ni-25%X composites

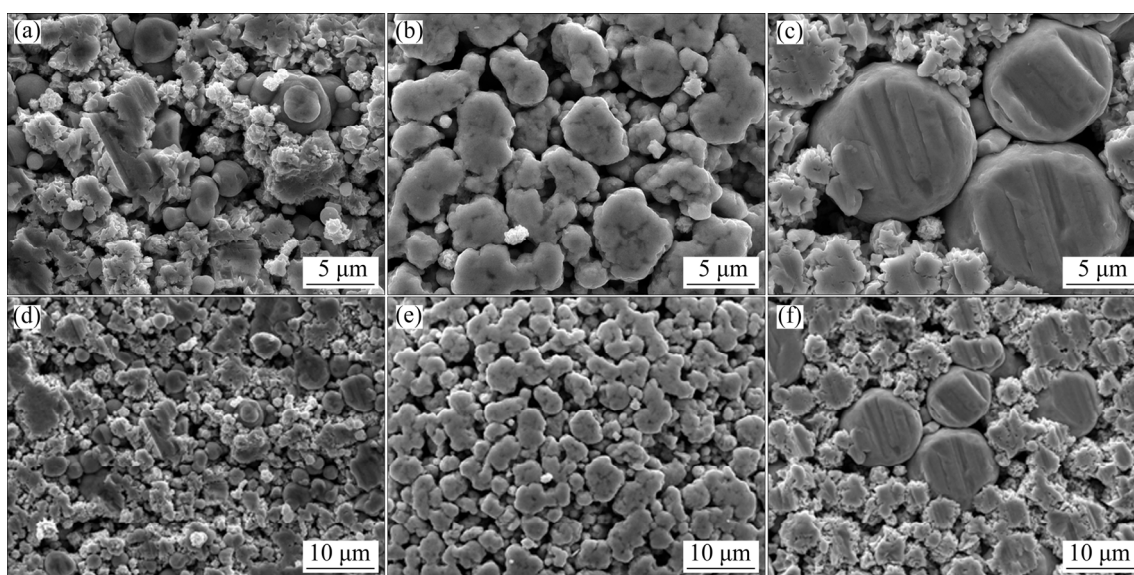
Figure 1 shows the XRD patterns of pristine Ni powder and Ni-25%X (X=Fe, Co, Cu) after ball milling for 5 h. All the samples are composed of three diffraction peaks corresponding to (111), (200) and (220) planes, respectively, as shown in Fig. 1(a). For pristine Ni, the three characteristic peaks are distributed at 44.5°, 51.8° and 76.3°, respectively. After Fe, Co and Cu doping, the diffraction peaks of samples all shift to the left and no new phase is detected, as shown in Fig. 1(b). Furthermore, the lattice parameters of the as-milled Ni-25%X samples are refined by the Rietveld refinement method, and the obtained results exclude that the left deviation of diffraction peaks is caused by sampling shift or zero shift during scanning. This indicates that the Ni-25%X solid solutions are successfully synthesized through ball milling. The lattice expansion of Ni after X (X=Fe, Co, Cu) doping should be ascribed to the larger atomic radius of X (Fe=1.26 Å, Co=1.25 Å, Cu=1.28 Å) atom relative to Ni (1.24 Å), which results in the left shift of the diffraction peaks for the Ni-25%X solid solutions.

Figure 2 presents the SEM images of Ni-25%X solid solutions with different magnifications. It can be seen that the particle size of these solid solutions is decreased in the order of Ni-25%Cu, Ni-25%Co, and Ni-25%Fe. For Ni-25%Fe system, its particle distribution is relatively uniform, and the size varies from 1 to 5 μm, as shown in Figs. 2(a) and (d). Compared with Ni-25%Fe system, the particle size of Ni-25%Co is significantly larger, which is mainly concentrated in 3–5 μm, as shown in Figs. 2(b) and (e). For Ni-25%Cu system, the



**Fig. 1** XRD patterns of as-milled Ni-25%X solid solutions

particles are relatively coarse, and their sizes are larger than 5 μm, as shown in Figs. 2(c) and (f). As we all know, the elastic constants determine the response of crystal to external force, and they play an important role in the mechanical properties of material. In order to explain the relationship between the morphologies and mechanical properties of Ni-25%X solid solutions, the elastic properties of Ni crystal doped with 25 at.% X (X=Fe, Co, Cu) atom are calculated by a stress-strain approach. The ductility/brittleness of a crystal is usually judged by the quotient of its shear modulus  $G$  to bulk modulus  $B$ , i.e.,  $G/B$  [48]. According to the Pugh criterion [49], the  $G/B$  value of 0.57 is the critical value for judging the ductility/brittleness of crystal. Generally, a crystal is regarded as ductile if  $G/B$  value is less than 0.57, and vice versa. The calculated  $G/B$  values of Ni-25%Fe, Ni-25%Co and Ni-25%Cu solid solutions in this work are 0.46, 0.45, and 0.41 respectively, which are all lower than 0.57, suggesting that these solid solutions are all ductile. Among them, the Ni-25%Cu solid solution



**Fig. 2** SEM images of as-milled Ni-25%Fe (a, d), Ni-25%Co (b, e) and Ni-25%Cu (c, f) solid solutions

has the best ductility due to the smallest  $G/B$  value, which should be the intrinsic reason for the difficulty to refine Ni-25%Cu particles through ball milling, as shown in Figs. 2(c) and (f).

Figure 3 shows the XRD patterns of as-milled  $\text{MgH}_2/\text{Ni-25\%Fe}$ ,  $\text{MgH}_2/\text{Ni-25\%Co}$ ,  $\text{MgH}_2/\text{Ni-25\%Cu}$  and pristine  $\text{MgH}_2$  composites. All samples contain a major phase of  $\alpha\text{-MgH}_2$  and a small amount of  $\gamma\text{-MgH}_2$  phase. Besides, the Ni(X) (X= Fe, Co, Cu) solid solution phases are detected in as-milled  $\text{MgH}_2/\text{Ni-25\%X}$  composites, and no other new phases are generated.

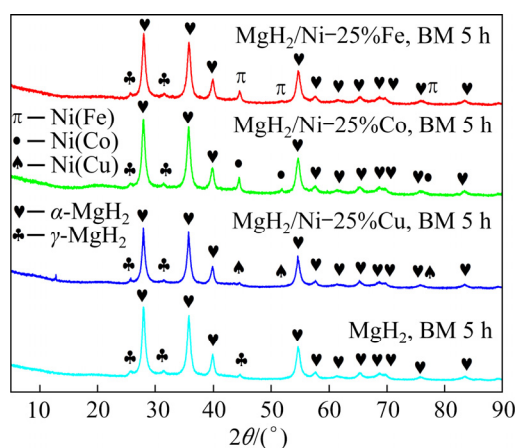
Figure 4 presents the SEM images of as-milled  $\text{MgH}_2/\text{Ni-25\%X}$  composites with different magnifications. The particle distribution of  $\text{MgH}_2/\text{Ni-25\%Fe}$  composite is uneven, and the size

is 1–5  $\mu\text{m}$ , as shown in Figs. 4(a) and (d). Comparatively, the particle distribution of  $\text{MgH}_2/\text{Ni-25\%Co}$  composite is relatively even, and the size is mainly concentrated in 2–4  $\mu\text{m}$ , as shown in Figs. 4(b) and (e). For  $\text{MgH}_2/\text{Ni-25\%Cu}$  composite, the particle distribution is more uniform, and the size is mainly concentrated in 1–3  $\mu\text{m}$ , as shown in Figs. 4(c) and (f).

### 3.2 Hydrogen storage properties of $\text{MgH}_2/\text{Ni-25\%X}$ composites

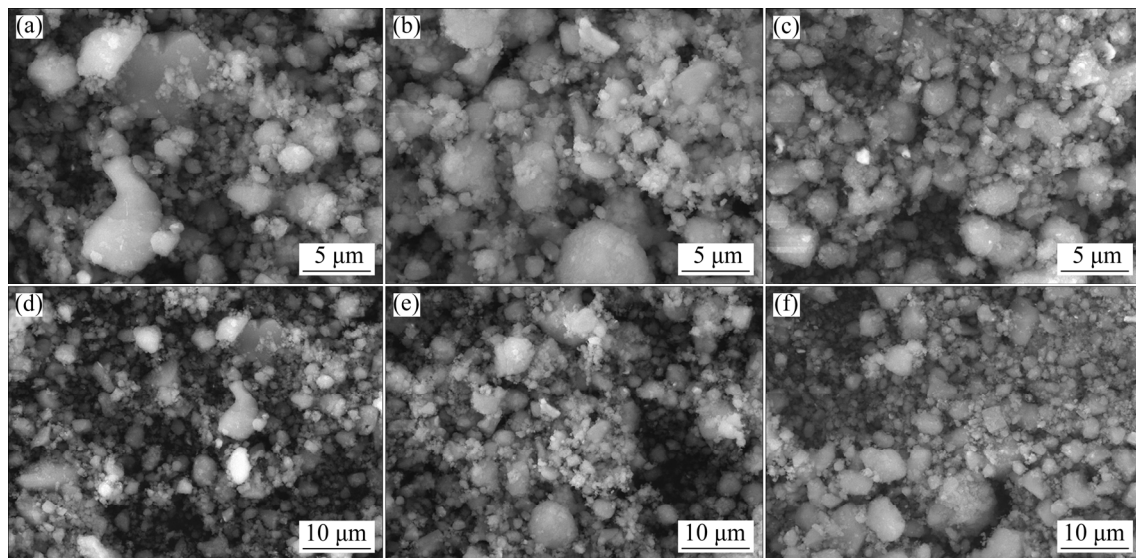
In order to investigate the catalytic effects of different Ni-based solid solutions on the hydrogen storage properties of  $\text{MgH}_2$ , the dehydrogenation temperatures of the as-milled pristine  $\text{MgH}_2$  and  $\text{MgH}_2/\text{Ni-25\%X}$  composites are firstly examined by using TPD test. These samples are heated from 20 to 500  $^{\circ}\text{C}$  at a heating rate of 3  $^{\circ}\text{C}/\text{min}$ , as shown in Fig. 5. It can be seen that the initial dehydrogenation temperature of as-milled pristine  $\text{MgH}_2$  is about 302.7  $^{\circ}\text{C}$ . After Fe, Co and Cu solid-solution, the initial dehydrogenation temperature of  $\text{MgH}_2$  is significantly reduced by about 90  $^{\circ}\text{C}$ . When the temperature rises to 305  $^{\circ}\text{C}$ , the dehydrogenation capacity of as-milled pristine  $\text{MgH}_2$ ,  $\text{MgH}_2/\text{Ni-25\%Fe}$ ,  $\text{MgH}_2/\text{Ni-25\%Co}$  and  $\text{MgH}_2/\text{Ni-25\%Cu}$  are 0.24, 5.17, 5.87 and 5.81 wt.%, respectively. This means that the Ni-based solid solutions have excellent catalytic effects on the dehydrogenation of  $\text{MgH}_2$ .

The isothermal hydrogen absorption and desorption kinetics of as-milled pristine  $\text{MgH}_2$  and

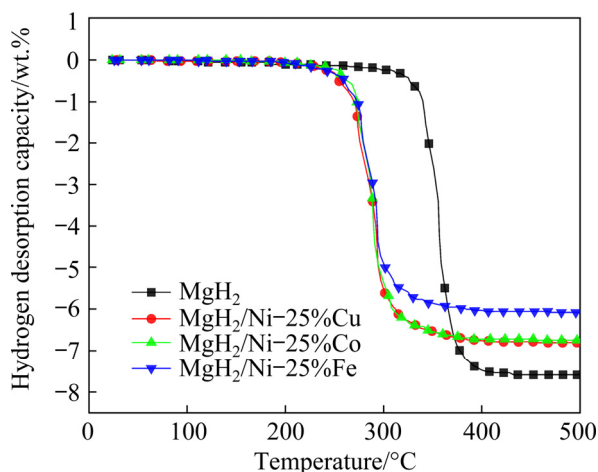


**Fig. 3** XRD patterns of as-milled pristine  $\text{MgH}_2$  and  $\text{MgH}_2/\text{Ni-25\%X}$  composites





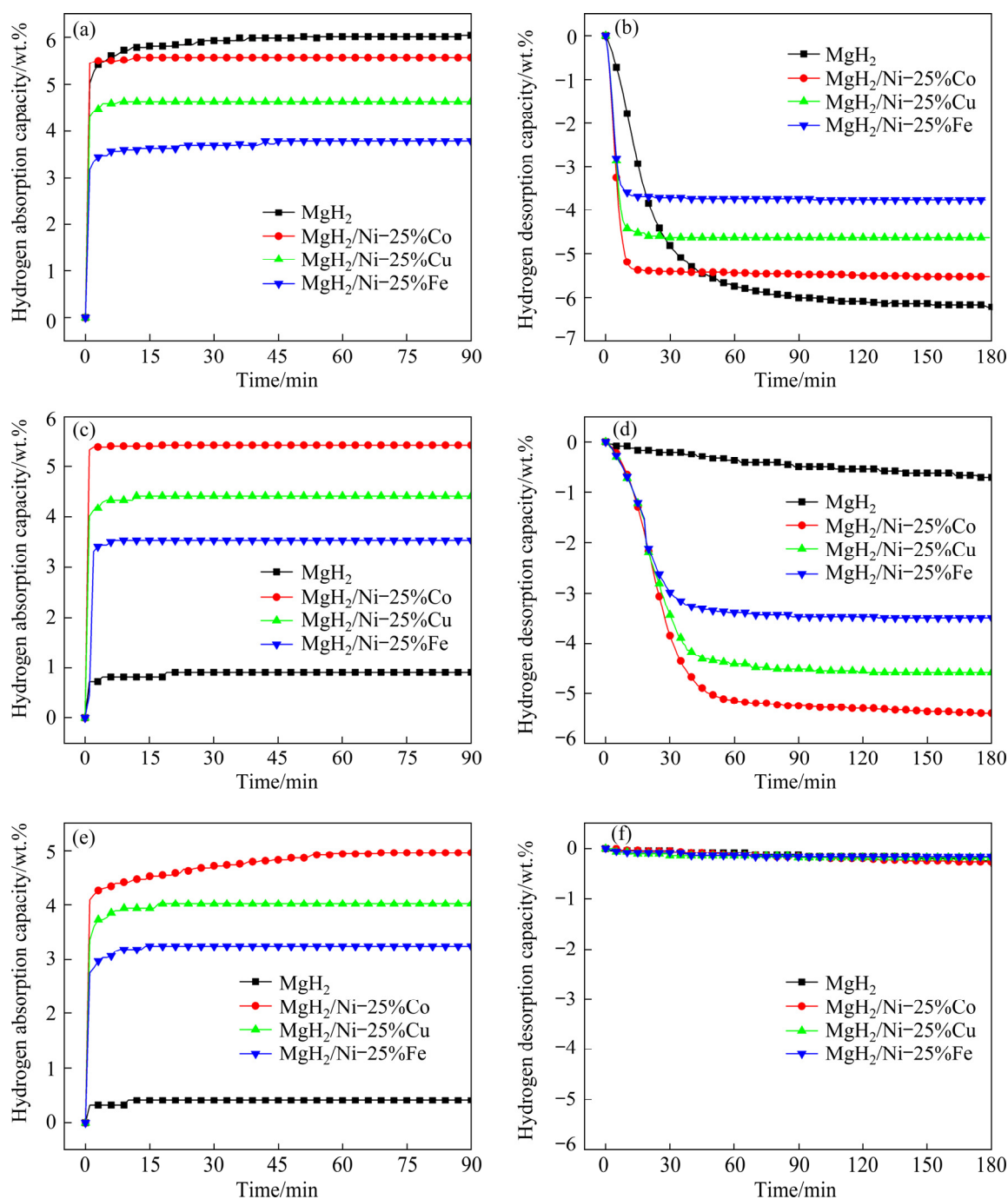
**Fig. 4** SEM images of as-milled  $\text{MgH}_2/\text{Ni-25\%Fe}$  (a, d),  $\text{MgH}_2/\text{Ni-25\%Co}$  (b, e), and  $\text{MgH}_2/\text{Ni-25\%Cu}$  (c, f) composites



**Fig. 5** TPD curves of as-milled pristine  $\text{MgH}_2$  and  $\text{MgH}_2/\text{Ni-25\%X}$  composites with heating rate of  $3\text{ }^\circ\text{C/min}$

$\text{MgH}_2/\text{Ni-25\%X}$  composites are further tested. Figures 6(a)–(f) present the isothermal hydrogenation and dehydrogenation curves of these samples at different temperatures (300, 275, and  $250\text{ }^\circ\text{C}$ , respectively). At  $300\text{ }^\circ\text{C}$ , all samples exhibit the excellent hydrogenation kinetic properties, as shown in Fig. 6(a). Among them, the  $\text{MgH}_2/\text{Ni-25\%Co}$  composite has the fastest hydrogenation rate, which can absorb 5.50 wt.% hydrogen within 3 min, while the as-milled pristine  $\text{MgH}_2$ ,  $\text{MgH}_2/\text{Ni-25\%Cu}$  and  $\text{MgH}_2/\text{Ni-25\%Fe}$  composites can only absorb 5.42, 4.47 and 3.46 wt.% hydrogen, respectively. With decreasing temperature, the  $\text{MgH}_2/\text{Ni-25\%Co}$  composite still

keeps the fastest hydrogenation kinetics. At  $275\text{ }^\circ\text{C}$ , the  $\text{MgH}_2/\text{Ni-25\%Co}$  composite can absorb 5.39 wt.% hydrogen within 3 min, as shown in Fig. 6(c). Even at  $250\text{ }^\circ\text{C}$ , the  $\text{MgH}_2/\text{Ni-25\%Co}$  composite can still absorb 4.27 wt.% hydrogen within 3 min, while the as-milled pristine  $\text{MgH}_2$ ,  $\text{MgH}_2/\text{Ni-25\%Cu}$  and  $\text{MgH}_2/\text{Ni-25\%Fe}$  composites can only absorb 0.32, 3.73, and 2.97 wt.% hydrogen, respectively. Similar to the hydrogenation case, the  $\text{MgH}_2/\text{Ni-25\%Co}$  composite also shows excellent dehydrogenation kinetics. As shown in Fig. 6(b), the  $\text{MgH}_2/\text{Ni-25\%Co}$  composite can release 5.19 wt.% hydrogen within 10 min at  $300\text{ }^\circ\text{C}$ , while as-milled pristine  $\text{MgH}_2$ ,  $\text{MgH}_2/\text{Ni-25\%Cu}$ , and  $\text{MgH}_2/\text{Ni-25\%Fe}$  composites under the same conditions can only release 1.78, 4.42 and 3.59 wt.% hydrogen, respectively. At  $275\text{ }^\circ\text{C}$ , the  $\text{MgH}_2/\text{Ni-25\%Co}$  composite still maintains excellent dehydrogenation kinetics. It can release 3.84 wt.% hydrogen within 30 min, while as-milled pristine  $\text{MgH}_2$  under the same conditions can hardly release hydrogen, as shown in Fig. 6(d). Meanwhile, the  $\text{MgH}_2/\text{Ni-25\%Cu}$  and  $\text{MgH}_2/\text{Ni-25\%Fe}$  composites can only release 3.44 and 2.99 wt.% hydrogen, respectively. Thus, it can be deduced that the additions of Ni-25%X ( $\text{X} = \text{Fe}, \text{Co}, \text{Cu}$ ) solid solutions improve significantly the hydrogen sorption kinetics properties of  $\text{MgH}_2$ , and the Ni-25%Co solid solution exhibits the most remarkable catalytic effect.

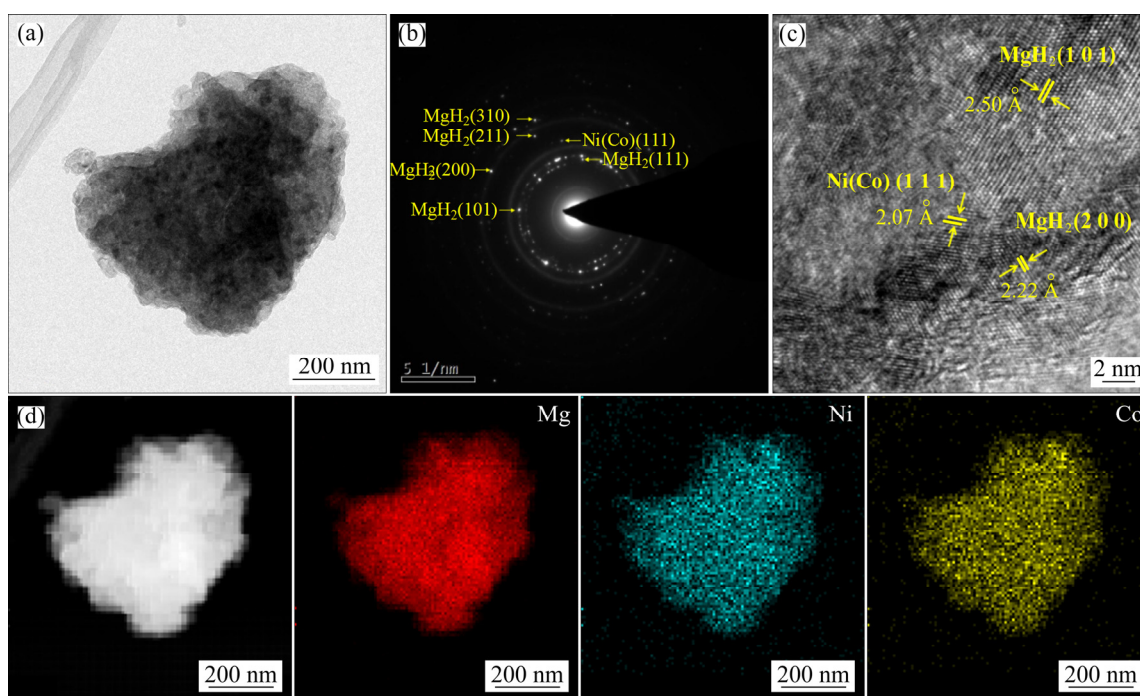


**Fig. 6** Hydrogen absorption (a, c, e) and desorption (b, d, f) kinetics curves of as-milled pristine  $\text{MgH}_2$  and  $\text{MgH}_2/\text{Ni-25\%X}$  composites at 300 °C (a, b), 275 °C (c, d), and 250 °C (e, f), respectively

### 3.3 Hydrogen storage mechanisms of $\text{MgH}_2/\text{Ni-25\%X}$ composites

In order to disclose the catalytic mechanisms of Ni-25%X solid solutions on hydrogen storage properties of  $\text{MgH}_2$ , the  $\text{MgH}_2/\text{Ni-25\%Co}$  composite was chosen and its microscopic morphology was characterized as shown in Fig. 7. Figure 7(a) shows the TEM image of as-milled  $\text{MgH}_2/\text{Ni-25\%Co}$  particles with the size of about 300 nm. Figure 7(b) shows the selected area

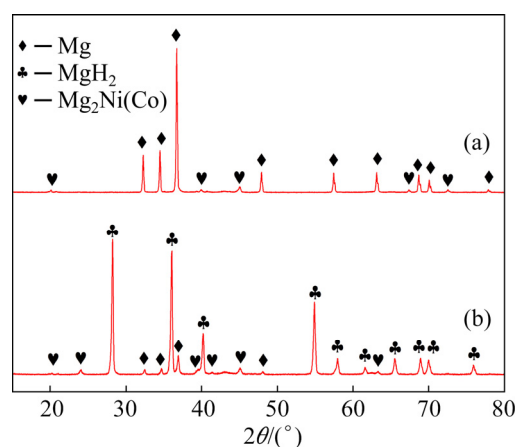
electron diffraction (SAED) image of particles, and the continuous diffraction rings correspond to  $\text{MgH}_2$  with the (111), (101), (211), (220) and (310) planes. Meanwhile, the (111) planes of Ni(Co) are also detected. Figure 7(c) presents the high-resolution transmission electron microscopy (HRTEM) of particles. The lattice fringes with interplanar spacing of 2.50 and 2.22 Å correspond to the (101) and (200) crystal plane of  $\text{MgH}_2$ , respectively. The lattice fringe with interplanar



**Fig. 7** TEM micrograph (a), selected area electron diffraction pattern (b), high resolution TEM micrograph (c) and corresponding EDS maps (d) of as-milled  $\text{MgH}_2/\text{Ni}-25\%\text{Co}$  composite

spacing of 2.07  $\text{\AA}$  is indexed to the (111) crystal plane of  $\text{Ni}(\text{Co})$  solid solution. The results of SAED and HRTEM verify the presence of  $\text{MgH}_2$  and  $\text{Ni}(\text{Co})$  solid solution in the as-milled sample and no new substances generate during ball milling, which is consistent with Fig. 3. The STEM and the corresponding energy dispersive X-ray spectroscopy (EDS) elemental mapping are further used to characterize the distribution of  $\text{MgH}_2$  and  $\text{Ni}(\text{Co})$  solid solution in the as-milled sample, as shown in Fig. 7(d). It can be seen that  $\text{Ni}(\text{Co})$  solid solution is homogeneously distributed on  $\text{MgH}_2$  matrix.

Figure 8 shows the XRD patterns of as-milled  $\text{MgH}_2/\text{Ni}-25\%\text{Co}$  composite after dehydrogenation and rehydrogenation. For the dehydrogenated  $\text{MgH}_2/\text{Ni}-25\%\text{Co}$  composite, Mg is the main phase. Meanwhile,  $\text{Mg}_2\text{Ni}(\text{Co})$  phase is also detected, which indicates that  $\text{Mg}_2\text{Ni}(\text{Co})$  is in-situ formed by the reaction of  $\text{MgH}_2$  with  $\text{Ni}-25\%\text{Co}$  solid solution during dehydrogenation. After rehydrogenation, the composite contains not only the main phase of  $\text{MgH}_2$  but also minor phase of Mg. A small amount of Mg phase is detected probably due to its incomplete hydrogenation. Notably, the  $\text{Mg}_2\text{Ni}(\text{Co})$  phase still appears in the rehydrogenated sample and no other new phase is detected, which means



**Fig. 8** XRD patterns of as-milled  $\text{MgH}_2/\text{Ni}-25\%\text{Co}$  composite after dehydrogenation (a) and rehydrogenation (b)

that the in-situ formed  $\text{Mg}_2\text{Ni}(\text{Co})$  is not decomposed during the hydrogenation. The XRD results demonstrate that the in-situ formed  $\text{Mg}_2\text{Ni}(\text{Co})$  phase plays a practical catalytic role in improving the hydrogen absorption and desorption properties of  $\text{MgH}_2/\text{Ni}-25\%\text{Co}$  composite. During dehydrogenation/ hydrogenation, the  $\text{Ni}-25\%\text{Co}$  solid solution uniformly distributed on the  $\text{MgH}_2$  matrix in-situ forms  $\text{Mg}_2\text{Ni}(\text{Co})$ , which provides a large number of active nucleation sites and hydrogen diffusion channels for the  $\text{Mg}/\text{MgH}_2$

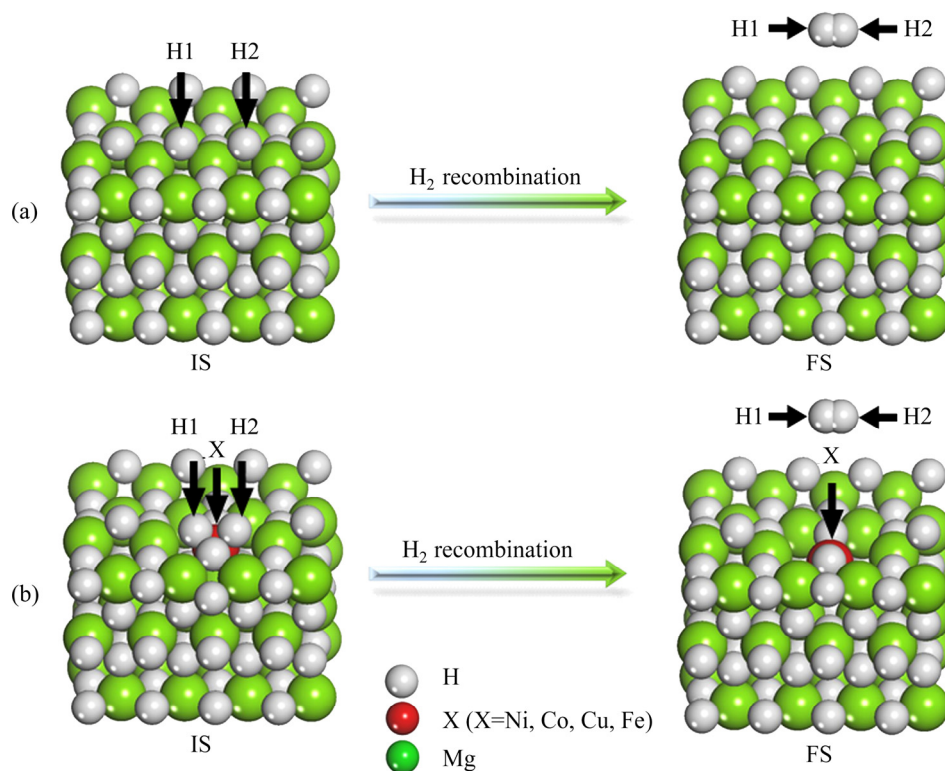


system to absorb and release hydrogen. Apparently, the in-situ formed  $\text{Mg}_2\text{Ni}(\text{Co})$  exhibits the typical hydrogen spillover effect on  $\text{MgH}_2$  [45].

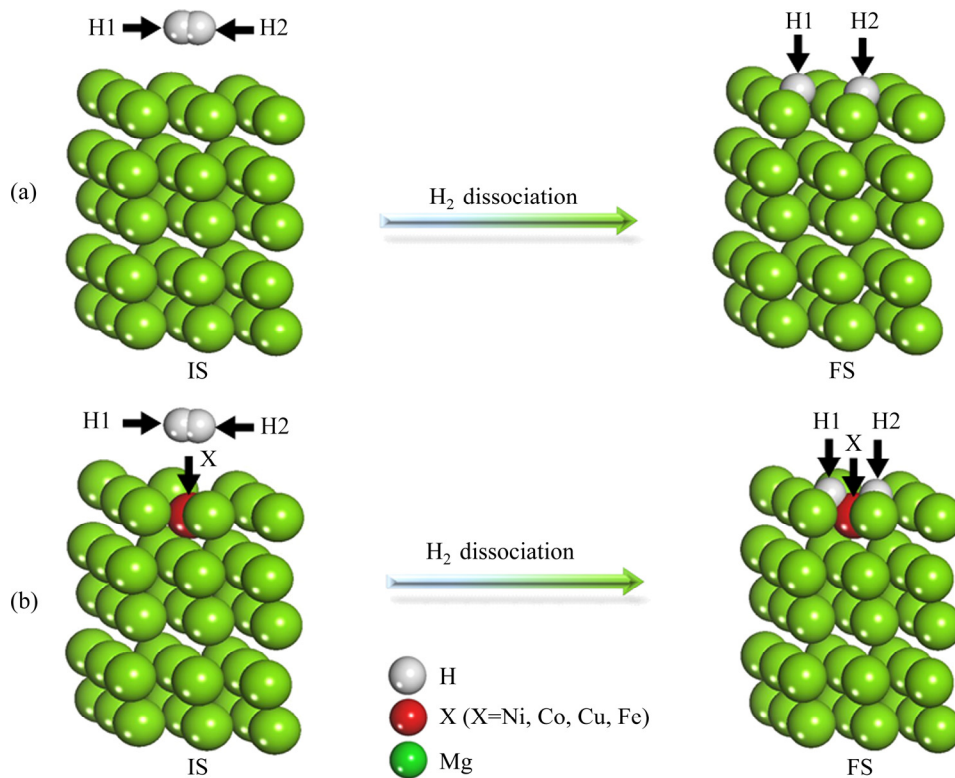
It is well known that the actual hydrogen absorption/desorption process of  $\text{Mg}/\text{MgH}_2$  will be affected by the hydrogen absorption/desorption kinetics. In other words, the hydrogen absorption energy barrier needs to be crossed when  $\text{H}_2$  molecule breaks from  $\text{H}-\text{H}$  bond to form  $\text{Mg}-\text{H}$  bond with  $\text{Mg}$  atom. Similarly, the hydrogen desorption energy barrier also needs to be crossed when  $\text{H}$  atom breaks from  $\text{Mg}-\text{H}$  bond to form  $\text{H}_2$  molecule. In order to further interpret the intrinsic reason of different catalytic effects of  $\text{Ni}-25\%\text{X}$  solid solutions on hydrogen storage properties of  $\text{Mg}/\text{MgH}_2$  system, the transition state (TS) of  $\text{H}_2$  dissociation/recombination on  $\text{Mg}/\text{MgH}_2$  surfaces doped with different transition metals  $\text{X}$  ( $\text{X}=\text{Fe}, \text{Co}, \text{Ni}, \text{Cu}$ ) are calculated. Figure 9 shows the optimized initial state (IS) and final state (FS) models of  $\text{H}_2$  recombination on pristine  $\text{MgH}_2(110)$  and the transition metal  $\text{X}$ -doped  $\text{MgH}_2(110)$  surfaces. Similarly, Fig. 10 shows the optimized IS and FS models of  $\text{H}_2$  dissociation on pristine  $\text{Mg}(0001)$  and  $\text{X}$ -doped  $\text{Mg}(0001)$  surfaces. The calculated energy barrier values are plotted in

Fig. 11. For the pristine  $\text{MgH}_2(110)$ , the  $\text{H}_2$  recombination energy barrier value is 6.34 eV, as shown in Fig. 11(a). After  $\text{X}$  doping, the energy barrier values of  $\text{H}_2$  recombination on  $\text{MgH}_2(110)$  surface are decreased significantly, which indicates that the  $\text{Mg}-\text{H}$  bond strength is greatly weakened due to the doping of transition metals. This is consistent with the experimental results from TPD (see Fig. 5) and isothermal dehydrogenation (see Fig. 6). For pristine  $\text{Mg}(0001)$ , the  $\text{H}_2$  dissociation energy barrier value is 1.49 eV, as shown in Fig. 11(b). After  $\text{X}$  doping, the energy barrier values of  $\text{H}_2$  dissociation on  $\text{Mg}(0001)$  surface are also decreased with different degrees. This reveals that the doping of transition metals enhances the catalytic activity of  $\text{Mg}(0001)$  surface for  $\text{H}_2$  dissociation, which is consistent with the experimental results of isothermal hydrogenation (see Fig. 6).

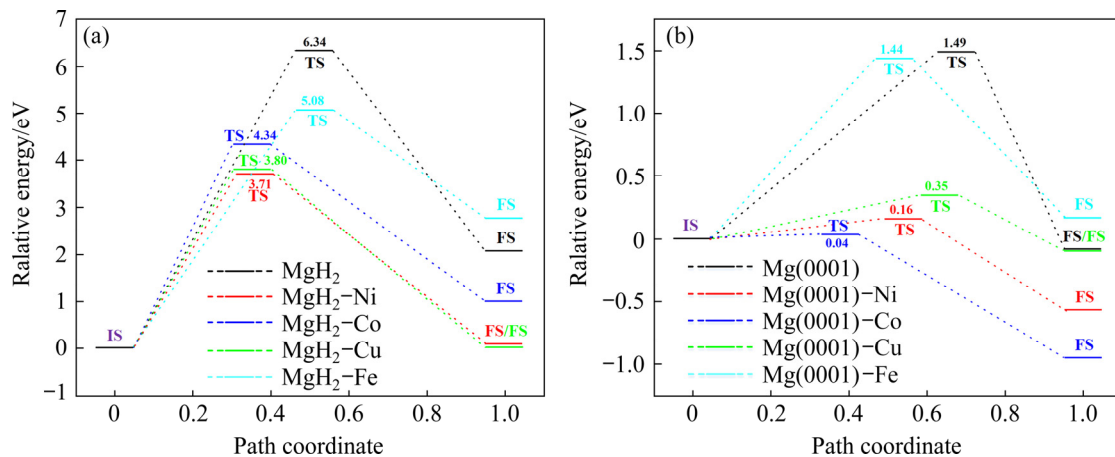
Figure 12 further gives the total densities of states (DOS) of pristine  $\text{MgH}_2(110)/\text{Mg}(0001)$  and the transition metal  $\text{X}$  ( $\text{X}=\text{Fe}, \text{Co}, \text{Ni}, \text{Cu}$ ) doped  $\text{MgH}_2(110)/\text{Mg}(0001)$ . In the density of states (DOS) plots, the Fermi level ( $E_F$ ) is set as zero and used as a reference. From Fig. 12(a), the total DOS of pristine  $\text{MgH}_2(110)$  surface is mainly distributed



**Fig. 9** Optimized initial state (IS) and final state (FS) models of  $\text{H}_2$  recombination on pristine  $\text{MgH}_2(110)$  (a), and transition metal  $\text{X}$ -doped  $\text{MgH}_2(110)$  surfaces (b)



**Fig. 10** Optimized initial state (IS) and final state (FS) models of  $H_2$  dissociation on pristine  $Mg(0001)$  (a), and transition metal X-doped  $Mg(0001)$  surfaces (b)



**Fig. 11**  $H_2$  recombination (a) and dissociation (b) energy barriers on pristine  $MgH_2(110)/Mg(0001)$  and transition metal (Fe, Co, Ni, Cu) doped  $MgH_2(110)/Mg(0001)$  surfaces

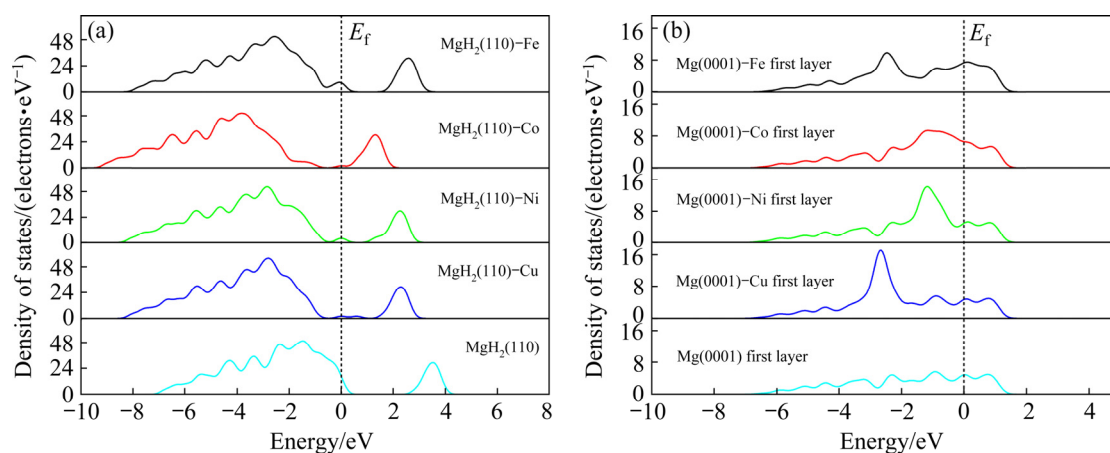
in the range of  $-7.5$  to  $4.5$  eV. As for X-doped  $MgH_2(110)$  surfaces, the total DOS moves to the lower energy level, which is mainly distributed in the range of  $-9.5$  to  $3.5$  eV. More importantly, the energy gap of X-doped  $MgH_2(110)$  surfaces near the Fermi level ( $E_F$ ) is narrower than that of the pristine  $MgH_2(110)$  surface. Commonly, the energy gap near the Fermi level ( $E_F$ ) can be used to judge the structural stability of crystal or surface, the smaller the energy gap near the Fermi level ( $E_F$ )

means the lower structural stability of crystal or surface [44]. Therefore, the enhanced dehydrogenation ability of  $MgH_2(110)$  surface doped with transition metals should be ascribed the weakened structural stability of  $MgH_2(110)$  surface after transition metals doping, which leads to the easier hydrogen releasing from  $MgH_2$ . Figure 12(b) further compares the total DOS of the first layer atoms of pristine  $Mg(0001)$  and X-doped  $Mg(0001)$  surfaces. It can be found that the X-doped

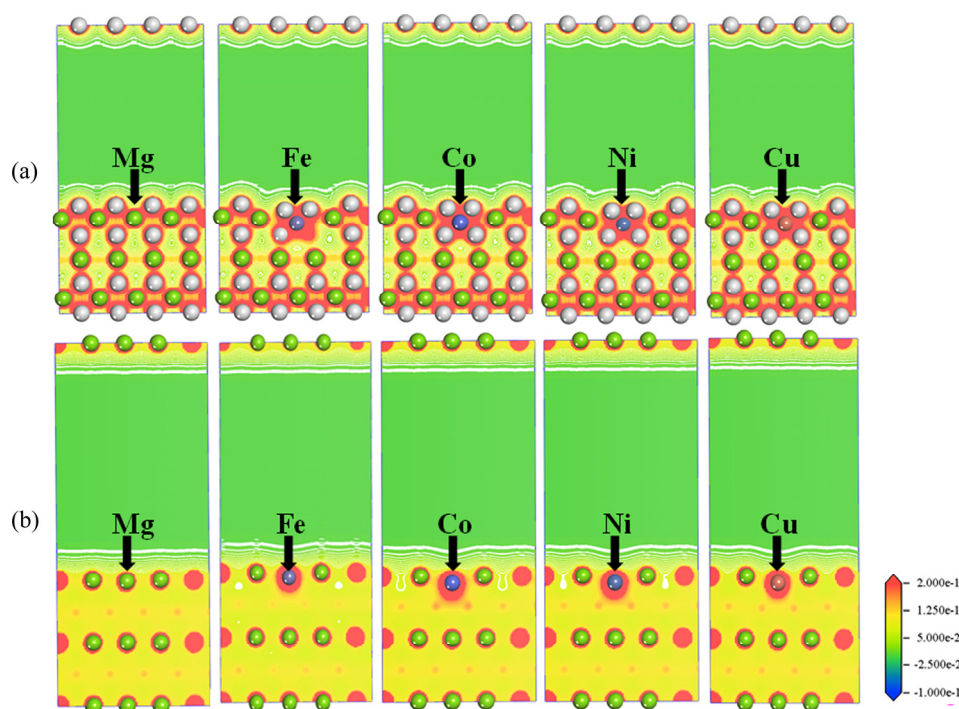
Mg(0001) surfaces have higher surface states relative to pristine Mg(0001) surface near the Fermi level ( $E_F$ ) due to the contribution of 3d orbitals of Fe, Co, Ni and Cu atoms, which indicates that the X-doped Mg(0001) surfaces have a stronger catalytic activity for  $H_2$  dissociation.

Figure 13 further presents the valence charge densities plots of pristine and X-doped  $MgH_2(110)/Mg(0001)$  surfaces. Compared with the pristine  $MgH_2(110)$  surface, as shown in Fig. 13(a), more electrons cloud overlapping between the transition metal atoms (Fe, Co, Ni, Cu) and the two adjacent H atoms on the surface in X-doped

$MgH_2(110)$  surfaces, which means that the bond strength between X and H is stronger than that between Mg and H. The strong bonding interactions between transition metal atoms (Fe, Co, Ni, Cu) and H atoms will result in the weakened bonding strength between H and adjacent Mg atoms, which will be conducive to promoting the release of H atoms and  $H_2$  recombination from  $MgH_2$  surface. From Fig. 13(b), the electron cloud on pristine Mg(0001) surface is relatively flat. Comparatively, the electron on X-doped Mg(0001) surfaces becomes rugged a little. Especially, the slight sinking of electron on the top of transition metals



**Fig. 12** Total densities of states of pristine and transition metal (Fe, Co, Ni, Cu) doped  $MgH_2(110)$  surfaces (a), and total densities of states of the first layer of pristine and transition metal (Fe, Co, Ni, Cu) doped Mg(0001) surfaces (b)



**Fig. 13** Valence charge densities of pristine and transition metal (Fe, Co, Ni, Cu) doped  $MgH_2(110)$  surfaces (a) and doped Mg(0001) surfaces (b)

can be seen, which may be the underlying reason for enhanced catalytic activity for  $H_2$  dissociation on Mg(0001) surface doped with transition metals.

## 4 Conclusions

(1) The prepared Ni–25%X (X=Fe, Co, Cu) solid solutions and  $MgH_2$  do not react to form new phases.

(2) As compared with as-milled pristine  $MgH_2$ , the initial dehydrogenation temperature of  $MgH_2$ /Ni–25%X (X = Fe, Co, Cu) is decreased by about 90 °C. The Ni–25%Co solid solution exhibits the best catalytic effect on the dehydrogenation kinetic properties of  $MgH_2$ .

(3) The superior hydrogen sorption kinetics of  $MgH_2$ /Ni–25%Co should be ascribed to the actual catalytic role of in-situ formed  $Mg_2Ni$ (Co) compounds during hydrogen absorption/desorption. The homogeneous distributed  $Mg_2Ni$ (Co) phases significantly promote the dissociation of hydrogen molecules and recombination of hydrogen atoms from Mg/ $MgH_2$ .

(4) The first-principles calculations demonstrate that the energy barriers of  $H_2$  dissociation and recombination on Mg(0001)/ $MgH_2$ (110) surfaces are significantly decreased after doping transition metal atoms (Fe, Co, Ni, Cu). The narrowed energy gap of  $MgH_2$ (110) surface and enhanced surface state of Mg(0001) surface further interpret the underlying catalytic mechanisms of Ni-based solid solutions.

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## 基于镍基固溶体催化的氢化镁储氢性能

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**摘要:** 采用高能球磨制备 Ni–25%X (X=Fe, Co, Cu, 摩尔分数)固溶体, 然后将其掺杂于 MgH<sub>2</sub> 体系中。与球磨纯 MgH<sub>2</sub> 相比, MgH<sub>2</sub>/Ni–25%X 复合体系初始放氢温度降低近 90 °C, 其中, Ni–25%Co 固溶体呈最佳催化效果。球磨 MgH<sub>2</sub>/Ni–25%Co 复合体系在 300 °C、10 min 内可释放 5.19%(质量分数)氢, 而相同条件下, 纯 MgH<sub>2</sub> 仅释放 1.78%(质量分数)氢; 更为重要的是, 放氢后 MgH<sub>2</sub>/Ni–25%Co 复合体系在 275 °C、3 min 内可吸收 5.39%(质量分数)氢。MgH<sub>2</sub>/Ni–25%Co 体系优异的吸放氢动力学可归因于其在吸/放氢过程中原位形成 Mg<sub>2</sub>Ni(Co)化合物的催化作用。第一性原理计算表明, 掺杂过渡金属原子后, Mg/MgH<sub>2</sub> 体系吸放氢反应能垒显著降低, 较好地解释了镍基固溶体催化改善 MgH<sub>2</sub> 储氢性能的实验结果。

**关键词:** MgH<sub>2</sub>; 镍基固溶体; 催化效果; 储氢性能; 第一性原理计算

(Edited by Xiang-qun LI)