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Electrochemical extraction of lead from urea-1-ethyl-3-methylimidazolium fluoride system containing PbO at 353 K

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Abstract: To electrochemically extract Pb from PbO at room temperature, a new electrolyte, urea–1-ethyl-3methylimidazolium fluoride (urea–[EMIM]F), was synthesized to dissolve PbO. Afterwards, the electrochemical behavior of Pb in this electrolyte was studied. The density, viscosity and conductivity of this electrolyte were investigated before electroextraction. The electrochemical behavior of Pb in the urea–[EMIM]F system was recorded via cyclic voltammograms, chronoamperometry and potentiostatic electrolysis. The results illustrate that Pb can be electrochemically extracted from PbO in this system at room temperature and that Pb reduction involves a quasireversible process and follows a one-step and two-electron transfer process. The reduction of Pb proceeds with a three-dimensional (3D) progressive model. With an increase in temperature, the onset potentials for Pb reduction shift anodically. The diffusion coefficient of Pb(II) is determined to be 6.88×10^{-10} cm²/s at 353 K. Additionally, spherical Pb particles are obtained after electrodeposition in the urea–[EMIM]F system via potentiostatic electrolysis. **Key words:** Pb; ionic liquids; imidazolium fluoride; electrodeposition; viscosity

1 Introduction

Lead is often used in lead-acid batteries that account for more than 85% of the global lead consumption [1]. Traditionally, lead is produced from galena through desulfurization (PbS to PbO) and deoxidation (PbO to Pb) in furnaces at a high temperature [2]. However, this process requires high energy consumption. Therefore, many laboratory studies have focused on hydrometallurgical methods that are operated at room temperature in aqueous systems, such as alkaline, nitrate, iodide, bromide, acetate, and methanesulfonate. Room-temperature ionic liquids (RTILs) are considered alternative electrolytes in laboratory studies during metal electrodeposition [3–5]. KATAYAMA et al [6] electrochemically extracted lead from Pb(TFSA)₂ in a BMPTFSA system at 298 K. BHATT et al [7] electrodeposited lead from Pb(NO₃)₂ and Pb(CO₃)₂ in the DIMCARB system. WANG et al [8] reported Pb electroreduction from PbCl₂ in the MBIC–AlCl₃ system. Similarly, TSAI et al [9] studied Pb electrodeposition in EMIBF₄ using PbCl₂ as the lead source. Furthermore, SIMONS et al [10] studied the extraction of metallic lead in a [C₂mim][NTf₂] system containing 50 mmol of Pb(NTf₂)₂.

In the above studies, lead salts were used as

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lead sources. It is interesting to use lead oxide as a lead source during metal electrodeposition [2,11]. However, it is difficult to dissolve metal oxides in molecular solvents, except for acids and bases [12]. Therefore, specific solvents have been developed by researchers. Previously, ABBOTT et al [13] reported that PbO₂ has a high solubility (9.157 mg/mL) in urea-choline chloride (ChCl). In addition, YANG and REDDY [14] presented the concentration of PbO $(7.5 \times 10^{-3} \text{ mol/L})$ and the voltammetric behavior of lead in the urea-ChCl system. RU et al [15-17] electrochemically analyzed various morphologies of lead from PbO-urea-ChCl and discussed the mechanism of PbO electroreduction in an ethylene glycol-ChCl system. HE et al [18] investigated the voltammetric and chronoampero- metric behavior of PbO in urea-EMIC system. Moreover, LIAO et al [19] and YEH et al [20,21] electrochemically studied the recovery of lead from PbO in urea-ChCl and in [Hbet][TFSA], respectively. Recently, LI and LI [22] have extracted Pb from PbO in acetamide-1methylimidazolium trifluoromethylsulfonate in a low-temperature system at room temperature. LIU et al [23] reported that Co-Nd films were electrosynthesized from urea-ChCl а system. CVETKOVIĆ et al [24] electrodeposited Al metal from an AlCl₃-urea RTIL. ALESARY et al [25] electrodeposited Zn-Sn alloys and studied the corrosion behavior of Zn-Sn coatings from the ChCl system. These unexpected solvating attributes are attractive in the processing of metal oxides and open a new route for metal electrodeposition from metal oxide precursors at room temperature.

However, compared with common EMIM salts, [EMIM]F can provide an interesting RTIL in a solvated form for metal electrodeposition. Lead electrodeposition in a urea-1-ethyl-3methylimidazolium chloride (urea-[EMIM]Cl) system has been reported in our previous work [18]. To avoid chlorine generation at the anode, we developed urea-[EMIM]F as an electrolyte instead of urea-[EMIM]Cl in this study. In addition, urea-[EMIM]Cl is sensitive to air, and lead electrodeposition in this system is required to be conducted in an inert-atmosphere glove box, while urea-[EMIM]F is stable in air. Additionally, urea-[EMIM]F has a higher conductivity than urea-[EMIM]Cl. Although [EMIM]F has been reported by HAGIWARA et al [26,27], RIJKSEN

and ROGERS [28], ZHU et al [29] and by our group [30-32], to the best of our knowledge, the application of [EMIM]F in lead extraction has not been elucidated so far. These findings expanded the range of applications of [EMIM]F and provided a simple route to extract lead particles from precursors of metal oxides at room temperature. Based on this study, the urea-[EMIM]F system was capable of dissolving PbO and extracting lead. The density, viscosity and conductivity of urea-[EMIM]F were determined, and the electrochemical characteristics of lead were investigated via cyclic voltammograms, chronoamperometry and potentiostatic electrolysis.

2 Experimental

2.1 Chemicals and materials

1-ethyl-3-methylimidazolium chloride, that is, [EMIM]Cl (>98%, Lanzhou Institute of Chemical Physics, China) was purified according to the procedure described in literatures [30,32,33]. Before use, the urea (99%, Sinopharm Chemical Reagent Co., Ltd., China) was dried in a vacuum for 10 h at 393 K. AgF (>98%, Alfa Aesar) and PbO (99.99%, Sinopharm Chemical Reagent Co., Ltd., China) were used as-received. Tungsten foils (99.99%, 0.3 mm thick) were used as the substrate for electrodeposition [18].

[EMIM]F was synthesized according to the procedure described in previous studies [30,32,33]. 25 mL of 2.76 mol/L [EMIM]Cl aqueous solution and 20 mL of 3.45 mol/L AgF aqueous solution were mixed and stirred for 24 h. A white precipitate was produced and centrifuged. The supernatant was dried for 48 h in a vacuum and [EMIM]F was obtained. Two samples of [EMIM]F were titrated via AgNO₃ and NaCl, respectively. No precipitates suggested that Cl^{-} and Ag^{+} were removed completely. The water content in [EMIM]F was measured to be 16.97% by Karl-Fischer titration. Additionally, urea and [EMIM]F were mixed at a molar ratio of 2:1 and the mixture was used to dissolve 1.4 mmol of PbO [18]. This final mixture was the labeled urea-[EMIM]F-PbO (0.31 mol/L).

2.2 Physical properties of urea-[EMIM]F

Measurements of the physical properties of urea-[EMIM]F were all performed according to literatures [30,34]. The densities of urea-[EMIM]F

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(molar ratio 2:1) were examined by the Archimedean method at temperatures ranging from 333 to 373 K, the viscosities were measured via the rotation method on a viscometer (DV–2TLV, Brookfield), and conductivity measurements were completed using the impedance method.

2.3 Electrodeposition of lead

The lead extraction and electrochemical investigation in the urea-[EMIM]F-PbO system were completed according to procedures reported in literature [18]. Specifically, the electrochemical behavior was investigated by means of cyclic voltammograms and chronoamperometry techniques using AUTOLAB an (Metrohm PGSTAT 30, Switzerland) potentiostat/galvanostat controlled by the GPES software. The cyclic voltammograms chronoamperometric and experiments were performed in a three-electrode cell, which consisted of a tungsten wire $(0.11 \text{ cm}^2,$ 99.95%) as the working electrode (WE), a platinum wire $(0.055 \text{ cm}^2, 99.95\%)$ as the counter electrode (CE) and a silver wire $(0.055 \text{ cm}^2, 99.95\%)$ as the quasi-reference electrode (QRE). All electrodes were polished with emery paper, degreased with an anhydrous alcohol solution in an ultrasonic bath, washed with doubly distilled water, and air-dried before conducting the experiments.

Electrodeposition experiments were conducted on a tungsten (W) substrate $(0.55 \text{ cm}^2, 99.99\%)$ in a three-electrode cell. The lead electrodeposition was performed at -0.62 V (vs Ag) and 353 K on the W substrate via potentiostatic electrolysis. After electrodeposition was completed, the substrate was immersed in an anhydrous alcohol solution to remove the electrolyte adhered to the surface. The phase constitutions of electrodeposits were detected via an X-ray diffractometer (XRD, PANalytical MPDDY 2094, Netherlands), and the elemental compositions and surface morphologies of the electrodeposits were examined using a scanning electron microscope (SEM, ZEISS ULTRA-43-13, Germany) equipped with an energy-dispersive spectroscope (EDS, X-Max 50, Oxford, England).

3 Results and discussion

3.1 Physical properties

Figure 1 shows the densities of urea– [EMIM]F (molar ratio 2:1) at different temperatures. A linear decrease with increasing temperature was identified. A linear correlation was obtained using Eq. (1), which is similar to that of other imidazolium-based RTILs reported in literature [32] and indicates that the density of urea–[EMIM]F changes linearly with increasing temperatures from 333 to 373 K.

$$\rho = 1.4060 - 6.1133 \times 10^{-4} T \tag{1}$$

where ρ is the density in g/cm³ and T is the thermodynamic temperature in K.



Fig. 1 Density of urea-[EMIM]F (molar ratio 2:1) as function of temperature

Figure 2 shows the viscosities for urea– [EMIM]F (molar ratio 2:1). These viscosities decrease with increasing temperature, which may be related to changes in van der Waals forces [35]. The viscosities do not decrease linearly with the increase of temperature. Similar behaviors were found in imidazole-based RTILs [36].



Fig. 2 Viscosity of urea–[EMIM]F (molar ratio 2:1) as function of temperature

Figure 3 shows the conductivity for urea– [EMIM]F and urea–[EMIM]Cl (molar ratio 2:1). Urea–[EMIM]F has conductivity varying from 6.59 to 24.52 mS/cm at temperatures between 333 and 373 K, which is higher than that of urea–[EMIM]Cl. This difference may be related to the ionic mobility being enhanced at a high temperature [37].



Fig. 3 Conductivity of urea-[EMIM]F and urea-[EMIM]Cl (molar ratio 2:1) as function of temperature

3.2 Cyclic voltammetry

To investigate the electrochemical behavior of lead in the urea-[EMIM]F (molar ratio 2:1) system, a linear scan voltammogram for urea-[EMIM]F (molar ratio 2:1) without lead was recorded from 0.56 to -0.8 V using a tungsten working electrode under a scan rate of 40 mV/s, which was considered a blank experiment, as shown in Fig. 4. There was no significant current within the electrochemical window, indicating that urea-[EMIM]F was electrochemically stable within the potential range. Figure 5 shows a cyclic voltammogram recorded from 0.25 to -0.65 V in urea-[EMIM]F (molar ratio 2:1) containing 0.31 mol/L PbO system under the same conditions. A cathodic peak at -0.476 V (vs Ag) and an anodic peak at -0.125 V were addition of PbO observed after the into urea-[EMIM]F. The metallic lead was obtained after potentiostatic electrolysis, as verified by XRD and EDS spectra. Therefore, the peak at -0.476 V was considered the electroreduction of Pb(II) to Pb. Similarly, the peak at -0.125 V corresponded to the dissolution of the reduced lead. These results indicate that the reduction of Pb(II) proceeds via a single-step and two-electron transfer process [2,18]. Figure 6 presents cyclic voltammograms for the urea-[EMIM]F-PbO (0.31 mol/L) system at



Fig. 4 Linear scan voltammogram of urea-[EMIM]F (molar ratio 2:1) (WE: W; *v*=40 mV/s; QRE: Ag; 353 K)



Fig. 5 Cyclic voltammogram for urea–[EMIM]F–PbO (0.31 mol/L) system (WE: W; *v*=40 mV/s; QRE: Ag; 353 K)



Fig. 6 Cyclic voltammograms for urea–[EMIM]F–PbO (0.31 mol/L) system at different scan rates (WE: W; QRE: Ag; 353 K)

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different scan rates. The currents in the cathodic peaks (I_{pc}) and anodic peaks increased with increasing scan rates. The cathodic and anodic peak potentials shifted to increasingly negative values when the scan rate increased to higher values. The difference between the cathodic half-peak potential and the cathodic peak potential $(\varphi_{pc/2} - \varphi_{pc})$ increased as the scan rate increased, and exceeded the limit for a reversible process (33.5 mV, 353 K), as shown in Table 1. BABD and FAULKNER [38], and MATSUDA and AYABE [39] suggested that zone boundaries for reversible ($\Lambda \ge 15$), quasireversible $(15 \ge A \ge 10^{-2(1+\alpha)})$, and totally irreversible $(A \le 10^{-2(1+\alpha)})$ systems can be calculated from Eq. (2). For the urea-[EMIM]F-PbO (0.31 mol/L) system, the $\Delta(\Lambda,$ α) was calculated to be 5.0591 via Eq. (2) and α was calculated to be 0.3670 via Eq. (3). Based on the function of $\Delta(\Lambda, \alpha)$ with Λ and α [38,39], the reduction of lead in the urea-[EMIM]F system could be considered a quasi-reversible process. Some nucleation loops were detected during sweep, the cathodic indicating that lead electrodeposition requires an overpotential to initiate nucleation [2].

 $\varphi_{\rm pc/2} - \varphi_{\rm pc} = \Delta(\Lambda, \alpha) [RT/(nF)]$ (2)

$$|\varphi_{\rm pc} - \varphi_{\rm pc/2}| = 1.857 RT/(\alpha nF) \tag{3}$$

where $\varphi_{pc/2}$ is the cathodic half-peak potential in V, φ_{pc} is the cathodic peak potential in V, α is the transfer coefficient, Λ is a parameter, Δ is a parameter that varies with Λ and α , *n* is the number of exchanged electrons, *F* is the Faraday constant of 96485 C/mol and *R* is the molar gas constant of 8.314 J/(K·mol).

Table 1 Values of φ_{pc} , $\varphi_{pc/2}$, $\varphi_{pc/2}-\varphi_{pc}$ and I_{pc} at different scan rates

$\frac{v}{(\mathrm{mV}\cdot\mathrm{s}^{-1})}$	$arphi_{ m pc}/ m mV$	$arphi_{ m pc/2}/ m mV$	$(arphi_{ m pc/2}-arphi_{ m pc})/mV$	$I_{\rm pc}/10^{-4}{ m A}$
20	-418.55	-369.61	48.94	3.85
40	-476.07	-405.63	70.44	4.54
60	-515.75	-430.86	84.89	4.95
80	-565.34	-461.84	103.50	5.24

3.3 Chronoamperometry

Figure 7 presents the chronoamperometric curves of the lead nucleation/growth process in the urea-[EMIM]F-PbO (0.31 mol/L) system at various potentials. These potential values were

chosen based on the value that failed to cause nucleation/growth, and negatively increased with the same gradient until full nucleation/growth. Chronoamperometric experiments were performed at potentials of -0.38, -0.44, -0.50, -0.54, -0.58 and -0.62 V. At the beginning of the experiment, each transient had a large decaying current due to the charge of the double-layer on the surface of the electrode. After dropping to a minimum value, these currents reversed and increased because of the nucleation of lead. The current in this stage is referred to as the Faraday current, which obtains an inflection point at $t_{\rm m}$, where $t_{\rm m}$ is the time at the maximum current I_m [40,41]. All instantaneous currents decay after time tm. As the potentials negatively increased, the $I_{\rm m}$ also increased, while $t_{\rm m}$ tended to decline. This may be attributed to less time to overlap with the discrete diffusion zone, and the enhancement of the nucleation rate and nucleation density at a higher cathodic potential [42].



Fig. 7 Chronoamperometric curves for urea-[EMIM]F-PbO (0.31 mol/L) system (WE: W; QRE: Ag; 353 K) at different potentials

The instantaneous current relationship $(I-t^{-1/2})$ after t_m , which was obtained from Fig. 7 during the chronoamperometric experiments is shown in Fig. 8. A linear relationship with the characteristics of Cottrell behavior was discovered. Hence, the lead nucleation/growth in this system may follow a diffusion-controlled process [38].

The instantaneous model (Eq. (4)) and the progressive model (Eq. (5)) are often involved in metal electrodeposition [40,41]. For instantaneous model, the fixed nucleation sites on the electrode surface are all activated after each potential step,



Fig. 8 Correlations between current and time $(t^{-1/2})$ in chronoamperometric experiments at different potentials: (a) $\varphi = -0.62$ V; (b) $\varphi = -0.58$ V; (c) $\varphi = -0.54$ V; (d) $\varphi = -0.50$ V

and the number of nucleation sites is constant during the chronoamperometric experiment. However, the nucleation sites are gradually activated and increase as time increases in the progressive model. To identify the mode of lead nucleation, the experimental data in Fig. 7 are normalized by I/I_m versus t/t_m and then compared with Eqs. (4) and (5). The results agree well with the 3D progressive model (Fig. 9). Over a longer period, the experimental data are larger than the theoretical data, which may be related to partial kinetic control during electrodeposition [2,43,44]. Therefore, electrodeposition could be considered a 3D progressive process.

Instantaneous model:

$$\left(\frac{I}{I_{\rm m}}\right)^2 = 1.9542 \left(\frac{t_{\rm m}}{t}\right) \left\{ 1 - \exp\left[-1.2564 \left(\frac{t}{t_{\rm m}}\right)\right] \right\}^2 \quad (4)$$

Progressive model:

$$\left(\frac{I}{I_{\rm m}}\right)^2 = 1.2254 \left(\frac{t_{\rm m}}{t}\right) \left\{1 - \exp\left[-2.3367 \left(\frac{t}{t_{\rm m}}\right)^2\right]\right\}^2 \quad (5)$$

where I is the instantaneous current in A, and t is the instantaneous time in s.

3.4 Effect of temperature

Figure 10 shows that the cathodic peak potentials and the onset potentials anodically shift as the temperature rises. In addition, the current of the reduction and oxidation peaks also increases significantly. These are related to the enhanced diffusion of species high at temperatures. Chronoamperometric curves of the urea-[EMIM]F-PbO (0.31 mol/L) system at different temperatures are shown in Fig. 11. The current reaches a maximum in a shorter time as the temperature increases due to the nucleation/growth of lead nuclei at a faster rate. The corresponding Cottrell plots in the inset of Fig. 11 show the change in slopes with temperature, illustrating that lead diffusion is easier at high temperatures. The diffusion coefficient can be determined by Eq. (6) [40,41]:

$$I_{\rm m}^2 t_{\rm m} = 0.2598 D F^2 n^2 c_0^2 \tag{6}$$



Fig. 9 Comparison between experimental curves for urea–[EMIM]F–PbO (0.31 mol/L) system and theoretical models of instantaneous and progressive nucleation at different potentials: (a) –0.62 V; (b) –0.58 V; (c) –0.54 V; (d) –0.50 V



Fig. 10 Cyclic voltammograms for urea–[EMIM]F–PbO (0.31 mol/L) at different temperatures (WE: W; *v*= 40 mV/s; QRE: Ag)

where *D* is the diffusion coefficient in cm²/s, *F* is the Faraday constant of 96485 C/mol, *n* is the number of exchanged electrons, and c_0 is the metal ion bulk concentration in mol/mL. The values of I_m and t_m can be obtained from Fig. 11. The lead diffusion coefficients of substituting values for *n*,



Fig. 11 Chronoamperometric curves for urea-[EMIM]F-PbO (0.31 mol/L) system at different temperatures (Cathodic potential: -0.58 V; Inset: corresponding Cottrell plots (WE: W; QRE: Ag))

F and c_0 into Eq. (6) are listed in Table 2. In addition, Table 3 presents the lead diffusion coefficients obtained from different RTILs. The small difference may be related to various ionic liquids and different temperatures.

 Table 2 Lead diffusion coefficients (D) for urea

 [EMIM]F-PbO system at various temperatures

Temperature/K	$D/(\mathrm{cm}^2\cdot\mathrm{s}^{-1})$		
333	3.20×10^{-10}		
343	4.44×10^{-10}		
353	6.88×10^{-10}		
363	8.09×10^{-10}		

 Table 3 Diffusion coefficients of Pb(II) in different ionic liquids

Ionic liquid	<i>T</i> /K	$D/(\mathrm{cm}^2\cdot\mathrm{s}^{-1})$	Ref.
Urea-[EMIM]F	353	6.88×10^{-10}	This work
Urea-EMIC	353	1.67×10^{-8}	[18]
MIMTfO	373	3.60×10^{-8}	[45]
Urea-ChCl	363	2.20×10^{-7}	[19]
Urea-BMIC	353	3.22×10^{-8}	[2]

3.5 Electrodeposition and characterization

Potentiostatic electrolysis was completed on a tungsten substrate. During electrodeposition, the electrolyte was not stirred. Figure 12 presents the variation in current during potentiostatic electrolysis in urea–[EMIM]F–PbO (0.31 mol/L) system at -0.62 V (vs Ag) and 353 K for 60 min. The current decreases rapidly at the beginning and then remains relatively stable over the rest of the experimental period. After potentiostatic electrolysis, electrodeposits are obtained on the tungsten substrate and characterized by XRD, EDS and SEM.



Fig. 12 Current–time curve recorded during potentiostatic electrodeposition of Pb in urea–[EMIM]F–PbO (0.31 mol/L) system (Substrate: W; Cathodic potential: -0.62 V; *T*: 353 K)

The XRD pattern of electrodeposits is shown in Fig. 13. 2θ angles (31.3°, 36.3°, 52.2°, 62.1°, 65.2°, 85.4°, 88.2°) are associated with lead (ICCD files No. 03-065-2873), while the remaining peaks correspond to the tungsten substrate and carbon from electrolyte decomposition. No peaks of lead oxide are discovered in this XRD pattern, suggesting that Pb(II) in urea-[EMIM]F was electroreduced to Pb. Figure 14 shows the EDS analysis results of the electrodeposits. The peaks in this spectrum are related to lead and tungsten substances. Figure 15 shows the morphologies of the electrodeposits. Uniform and spherical lead particles were observed with sizes of about 100 nm, which were evenly distributed on the tungsten substrate. Similar morphologies were also discovered by LIU et al [2] for the urea-BMIC system.



Fig. 13 XRD pattern of electrodeposits obtained from urea-[EMIM]F-PbO (0.31 mol/L) system (Substrate: W; Cathodic potential: - 0.62 V; *T*: 353 K)



Fig. 14 EDS spectrum of electrodeposits obtained from urea–[EMIM]F–PbO (0.31 mol/L) system (Substrate: W; Cathodic potential: -0.62 V; *T*: 353 K)



Fig. 15 Lower (a) and higher (b) magnification SEM images of electrodeposits obtained from urea–[EMIM]F–PbO (0.31 mol/L) system (Substrate: W; Cathodic potential: -0.62 V; *T*: 353 K)

4 Conclusions

(1) Urea-[EMIM]F is capable of dissolving PbO. The lead particles were then electrochemically extracted from urea-[EMIM]F-PbO (0.31 mol/L) system at room temperature.

(2) The density, viscosity and conductivity of urea-[EMIM]F were recorded. The density linearly decreased and the conductivity increased as the temperature increased from 333 to 373 K. The viscosity decreased with increasing temperature.

(3) The reduction of Pb(II) involves a quasi-reversible, one-step and two-electron transfer process. The lead electrodeposition follows a 3D progressive nucleation and a growth model governed by diffusion mixing. The diffusion coefficient of Pb(II) in urea–[EMIM]F was determined to be 6.88×10^{-10} cm²/s at 353 K, and increased with increasing temperature.

(4) Uniform spherical lead particles were electrochemically extracted from the urea– [EMIM]F–PbO (0.31 mol/L) system at room temperature via potentiostatic electrolysis, as verified by XRD, EDS and SEM.

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含 PbO 的尿素-1-乙基-3-甲基氟化咪唑体系在 353 K 下电化学提取铅

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摘 要:为了能在室温下从氧化铅中电化学提取铅,合成一种新的电解质尿素-1-乙基-3-甲基氟化咪唑(urea-[EMIM]F)以溶解氧化铅,并研究铅在此电解质中的电化学行为。电化学提取前,研究该电解质的密度、黏度和电 导率。采用循环伏安法、计时电流法和恒电位电解技术研究铅在尿素-1-乙基-3-甲基氟化咪唑中的电化学行为。 结果表明:采用该电解质可在室温下从氧化铅中电化学提取铅;铅的还原遵循一步两电子的准可逆过程和三 维(3D)连续成核模型;随着温度的升高,铅还原的起始电位逐渐向阳极移动;在 353 K 下 Pb(II)的扩散系数为 6.88×10⁻¹⁰ cm²/s;对尿素-1-乙基-3-甲基氟化咪唑体系进行恒电位电沉积后,获得球状铅颗粒。 关键词:铅;离子液体;氟化咪唑;电沉积;黏度

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