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# A photocatalytic reaction kinetics model based on electrical double layer theory( I ) <sup>©</sup>

# —Surface complexation model at TiO<sub>2</sub>/ water interface

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[Abstract] The kinetics of photocatalysis can be usually described by Langmiur-Hinshelwood adsorption expression. The adsorption can be greatly influenced by the surface properties of photocatalyst. Triple layer model (TLM) was chosen to describe the surface adsorption of  $TiO_2$  based on electrical double layer (EDL) theory at the  $TiO_2$ /water interface. And through the potentiometric titration the parameters of TLM were determined by the extrapolation method and Fiteq13. 1 software. The results show that surface complexation dominates the surface charge and the numerical calculation fits the experiment data satisfactorily.

[ **Key words**] TiO<sub>2</sub>; photocatalysis; model; adsorption [ **CLC number**] TB 39

#### [Document code] A

#### 1 INTRODUCTION

The photocatalytic process is an emergency as a promising technology for oxidation of organic contaminants in environmental control<sup>[1]</sup>. However, the rate of photocatalytic reaction is one major factor to limit its practical applications. Most experimental results<sup>[2]</sup> show that the kinetics of photocatalysis can be expressed by Langmiur-Heinshelwood adsorption equation. But the farther study on the relationship between adsorption and photocatalytic reaction is little reported. Because the heterogeneous photocatalytic reaction takes place at the surface of the catalyst<sup>[3]</sup>, it is worth studying the factors that affect the organic adsorption on the surface of photocatalyst, such as properties of catalyst, pH, ionic strength.

Surface complexation model (SCM) proposed by Stumm is well accepted to describe the adsorption and surface reaction at interface. It includes tow kinds of model, non electrical model (NEM) and electrical double layer (EDL)<sup>[4]</sup>. In EDL, according to the physical description of the electrostatics of the interface provided by classic theories of Gouy, Chapman, Stern, et al, it can be recalled constant capacity model (CCM), Stern model, triple layer model (TLM), Multi-site Complexation (MUSIC)<sup>[5]</sup> model, etc, in which TLM is widely used.

In conventional photocatalytic process, titanium

dioxide (TiO<sub>2</sub>) was used as the catalyst. In this paper, the surface adsorption of TiO<sub>2</sub> are described by triple layer model (TLM) based on electrical double layer (EDL) theory at the TiO<sub>2</sub>/water interface. And through the potentiometric titration the parameters of TLM can be determined by the extrapolation method and Fiteql3. 1 software.

#### 2 EXPERIMENTAL

#### 2. 1 Materials

All reagents used in this study were analytical grade and were used without farther purification.  $TiO_2$  was purchased from Japan Titan Kogyokk Co. The BET surface area was  $61 \text{ m}^2/\text{ g}$ . By X-ray diffraction analysis no other crystal besides anatase was detected.

# 2. 2 Method

All titration experiments were carried out in the experimental setup which can be found elsewhere  $^{[6]}$ . Purified nitrogen was used to create a CO<sub>2</sub>-free atmosphere in the titration beaker. The TiO<sub>2</sub> suspension with dry NaCl and NaOH added was stirred. The titration procedure was performed by adding HCl solution. Measurements were performed under non-stirred conditions. The system was taken to be as equilibrium when the drift was less than 0.02 mV/

min. Detailed and accurate HCl and NaOH dosage were obtained.

# 3 SURFACE COMPLEXATION MODEL AND DETERMINATION OF PARAMETER

### 3.1 Surface complexation model

The ionization reaction of surface site on  ${\rm TiO_2}$  can be written as  $^{[6,\ 7]}$ 

$$-SOH_2^+ = -SOH + H^+$$

$$-SOH = -SO^- + H^+$$

and its equilibrium constant can be expressed as

$$K_{a1} = [-SOH_2^+]/[-SOH][H^+]_s$$
 (1)

$$K_{a2} = [-SO^-][H^+]_s/[-SOH]$$
 (2)

where [-SOH<sub>2</sub><sup>+</sup>] and [-SOH] and [-SO<sup>-</sup>] are the concentrations of protonated, unprotonated and deprotonated surface site, respectively.

The concentrations of protons at some location in the electrical double layer is related to the bulk solution concentration by the Boltzmann distribution, e. g. ,

$$[H^{+}]_{s} = [H^{+}] \exp[-F\phi_{0}/(RT)]$$

where  $\phi_0$  is the mean potential in the plane of surface change ( $\sigma_0$ ), F is Faraday constant (96 484. 5 C/mol), [H<sup>+</sup>] is the concentration of protons in the bulk solution, R is the universal gas constant, T is the absolute temperature. And hence

$$K_{al} = \begin{bmatrix} -SOH_{2}^{+} \end{bmatrix} / \begin{bmatrix} -SOH \end{bmatrix} \begin{bmatrix} H^{+} \end{bmatrix} \bullet$$

$$\exp \begin{bmatrix} -F \phi_{0} / (RT) \end{bmatrix}$$

$$K_{a2} = \begin{bmatrix} -SO^{-} \end{bmatrix} \begin{bmatrix} H^{+} \end{bmatrix} / \begin{bmatrix} -SOH \end{bmatrix} \bullet$$

$$\exp \begin{bmatrix} -F \phi_{0} / (RT) \end{bmatrix}$$
(4)

Similarly, to account for specific adsorption of electrolyte (NaCl) ions, its equilibrium equation can be written as

$$-SOH_2^+ + Cl^- = -SOH_2^+ -Cl^-$$
$$-SO^- + Na^+ = -SO^- -Na^+$$

and its equilibrium constant can be expressed as

$$K_{\text{Cl}^{-}} = [-\text{SOH}_{2}^{+} - \text{Cl}^{-}]/[-\text{SOH}][\text{H}^{+}] \cdot [\text{Cl}^{-}] \exp[F(\psi_{0} - \psi_{\beta})/(RT)]$$
(5)  
$$K_{\text{Na}^{+}} = [-\text{SO}^{-} - \text{Na}^{+}][\text{H}^{+}]/[-\text{SOH}] \cdot [\text{Na}^{+}] \exp[-F(\psi_{0} - \psi_{\beta})/(RT)]$$
(6)

where [—SOH<sub>2</sub><sup>+</sup>—Cl<sup>-</sup>] and [—SO<sup>-</sup>—Na<sup>+</sup>] are the concentrations of protonated surface site bound to countercation and deprotonated surface site bound to counteranion, respectively, [Cl<sup>-</sup>] and [Na<sup>+</sup>] are the concentrations of anion and cation in bulk solutions, respectively. The surface site concentration is given by

$$N_{s}= [-SO^{-}] + [-SOH_{2}^{+}] + [-SOH] + [-SO^{-}-Na^{+}] + [-SOH_{2}^{+}-Cl^{-}]$$
 (7)

For  $TiO_2$ ,  $N_s$  was fixed at 20.8  $\mu$ mol/m<sup>2</sup> that is the value recommended by Yates et al based on crystallographic consideration and tritium exchange and

mass loss experiment<sup>[8]</sup>.

lationship as follows:

# 3. 2 Relationship between charge and potential

For TLM<sup>[7]</sup>, electroneutrality requires that 
$$\sigma_{0+}$$
  $\sigma_{\beta+}$   $\sigma_{d}=$  0 (8)

and

$$\sigma_{0} = \left( \begin{bmatrix} -SOH_{2}^{+} \end{bmatrix} - \begin{bmatrix} -SO^{-} -Na^{+} \end{bmatrix} + \begin{bmatrix} -SOH_{2}^{+} -CI^{-} \end{bmatrix} - \begin{bmatrix} -SO^{-} \end{bmatrix} \right) \cdot F/(\Omega )$$

$$\sigma_{\beta} = \left( \begin{bmatrix} -SO^{-} -Na^{+} \end{bmatrix} - \begin{bmatrix} -SOH_{2}^{+} -CI^{-} \end{bmatrix} \right) \cdot F/(\Omega )$$

F/(QA) (10) Constant capacitances are assumed in the surface regions between the planes and the charge potential re-

$$\sigma_0 = C_1(\phi_0 - \phi_\beta) \tag{11}$$

$$\sigma_{d} = C_2( \phi_d - \phi_\beta) \tag{12}$$

From Gouy-Chapman diffuse layer theory, the charge in the diffuse layer is

 $\sigma_{\rm d}=-\left(8\,\mbox{EE}_0RTI\right)^{1/2} \sinh[\,F\,\phi_{\rm d}/\,(\,2RT\,)\,]$  (13) where  $\sigma_0$ ,  $\sigma_{\rm B}$  and  $\sigma_{\rm d}$  are the charge at the plane 0,  $\beta$  and d, respectively;  $C_1$  and  $C_2$  are capacity values in inner and outer plane, respectively;  $\epsilon$  and  $\epsilon_0$  are the bulk dielectric constant of medium (water) and permittivity of vacuum, respectively; I is ionic strength.

# 3. 3 Determination of equilibrium constant and parameter

Equilibrium constant can be determined by the method of extrapolation or numerical fit. Fiteql family are the widely used software  $^{[9,\ 10]}$ , but its model-dependent fitting parameters are too many for the result to be unique. By the method of extrapolation, the other parameter, such as  $C_1$ ,  $C_2$ , can not be determined. In this paper, the complexation constants were determined by the extrapolation first, then the other parameters were done by Fiteql3. 1.

#### 3. 3. 1 Extrapolation

Surface charge density is a function of pH and is defined by

$$\sigma_0 = (C_a - C_b - 10^{-pH} + 10^{-14+pH}) \cdot F/(QA)$$
(14)

where  $C_a$  and  $C_b$  are the concentrations of acid or base after addition.

For a positively charged surface,

$$\sigma_0 = ([-SOH_2^+] + [-SOH_2^+ -Cl^-]) F/(QA)$$
(15)

For a negatively charged surface,

$$\sigma_0 = -([-SO^-] + [-SO^- -Na^+]) F/(QA)$$
(16)

According to the calculation procedure by Stumm and Schinlder, the surface charge is assumed to result from only simple amphoteric acid-base reaction of surface. The surface complexation is ignored.

However, there are errors in the approximation

of the above procedure if the complexation is significant. Sprycha<sup>[11]</sup> proved in theory that when  $\Delta pK_a > 2$ , in the range of all pH, either  $[-SOH_2^+]$  or  $[-SO^-]$  is much less than [-SOH]. Yates et al proved the  $\Delta pK_a$  of TiO<sub>2</sub> make an appointment of  $3^{[11]}$ . So the intrinsic acidity constant cannot be determined by the procedure above. In fact, surface complexation dominated the surface charge. The complexation can be done by the extrapolation method below.

For a positively charged surface, 
$$\sigma_0 = [ -SOH_2^+ -CI^- ] F/( \ PA ),$$
 
$$[ -SOH] = N_s - [ -SOH_2^+ -CI^- ]$$
 For a negatively charged surface, 
$$\sigma_0 = - [ -SO^- -Na^+ ] F/( \ PA ),$$
 
$$[ -SOH] = N_s - [ -SO^- -Na^+ ]$$
 Let 
$$\alpha = \sigma_0/N_s,$$
 and for a positively charged surface, let 
$$p \ P_{Na^+} = pH - lg[ \ \alpha - /(1- \ \alpha -) ] + lg[ \ Na^+ ]$$
 (17)

then

 $pK_{Na}^{+} = pQ_{Na}^{+} + F(\psi_{0} - \psi_{\beta})/2.303RT \quad (18)$  For a negatively charged surface, let

0.000

0.000

H[+] OH[-] 0.000

0.000

0.000

0.000

$$p Q_{Cl^{-}} = pH + lg[(\alpha_{+}/(1-\alpha_{+})] - lg[Cl^{-}]$$
(19)

then

$$pK_{CI}^- = pQ_{CI}^- + F(\psi_0 - \psi_\beta)/2.303RT$$
 (20)

When pH= pH<sub>pzc</sub>,  $\sigma_0 = 0$ ,  $\psi_0 = \psi_\beta = 0$ , the last terms in Eqns. (18) and (20) are vanished, p $K_{Na}^+ = pQ_{Na}^+$ , p $K_{Cl}^- = pQ_{Cl}^-$ . The point of intersection of pQ vs pH curves with the vertical line pH= pH<sub>pzc</sub> fixes the p $K_{Na}^+$  and p $K_{Cl}^-$  value.

### 3. 3. 2 Fiteql3. 1

Fiteq13. 1 is a business software, by which the surface equilibrium can be solved. According to the material and mass law, the equation matrix, in which the species are expressed by components of reaction products, can be solved by the iterative method of Newton-Raphson<sup>[5,9,10]</sup>. Tables 1 and 2 are the Storchiometry matrix  $\boldsymbol{A}$  and  $\boldsymbol{B}$  in the Fiteq13. 1 software.

### 4 RESULTS AND ANALYSIS

#### 4. 1 Potential titration of TiO<sub>2</sub>

The surface charge is formed on the metal oxide as a result of ionization and complexation reactions of surface hydroxyl groups. Electric charge vs pH value

**Table 1** Species,  $\lg K$ , and stoichiometry matrix A

		Tau	ter spe	ecies, ig	<b>A</b> , and	Stolemon	ietry ma	$\mathbf{H}$			
Name	$\lg K$	XOH	PSI(0)	PSI(b)	PSI(d)	H[+]	I/f	Cl[ - ]	Na[+]	<i>K</i> +	К –
$XOH_2[+]$	0.000	1.000	1.000	0.000	0.000	1.000	1.000	0.000	0.000	1.000	0.000
ХОН	0.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
XO[ - ]	0.000	1.000	- 1.000	0.000	0.000	- 1.000	- 1.000	0.000	0.000	0.000	1.000
$XOH_2Cl$	3. 100	1.000	1.000	- 1.000	0.000	1.000	2.000	1.000	0.000	1.000	0.000
XONa	3. 100	1.000	- 1.000	1.000	0.000	- 1.000	0.000	0.000	0.000	1.000	0.000
Na[ + ]	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	1.000	0.000	1.000
Cl[ - ]	0.000	0.000	0.000	0.000	0.000	0.000	0.000	1.000	1.000	0.000	0.000
H[+]	0.000	0.000	0.000	0.000	0.000	1.000	0.000	0.000	0.000	0.000	0.000
OH[-]	- 13.8	0.000	0.000	0.000	0.000	- 1.000	2.000	0.000	0.000	0.000	0.000

		Table 2	Species, lg	gK, and sto	oichiometry :	matrix <b>B</b>			
Name	хон	PSI(0)	PSI(b)	PSI(d)	H[+]	I/f	CI[ - ]	Na[+]	
ХОН	1.000	1.000	0.000	0.000	1.000	0.000	0.000	0.000	
XO[-]	1.000	- 1.000	0.000	0.000	- 1.000	0.000	0.000	0.000	
$\mathrm{XOH_{2}Cl}$	1.000	1.000	- 1.000	0.000	1.000	0.000	1. 000	0.000	
XONa	1.000	- 1.000	1.000	0.000	- 1.000	0.000	0.000	1.000	
Na[ + ]	0.000	0.000	0.000	0.000	0.000	0. 500	0.000	1.000	
Cl[ - ]	0.000	0.000	0.000	0.000	0.000	0.500	1.000	0.000	

0.000

0.000

1.000

-1.000

0.500

0.500

0.000

0.000

0.000

0.000

dependence is one of the most important characteristics of the surface properties of the metal oxide suspension solutions. The position of  $pH_{pzc}$  depends on the alkaliacid character of surface hydroxyl groups [12]. The values of  $pH_{pzc}$ , presented in many papers, are often very divergent, they range from 5.2 to 7 for  $TiO_2$  of the anatase structure [13].

The surface charge, expressed as surface excessive H, versus pH dependence for  $TiO_2$  suspension, whose concentrations are 0.000 89, 0.000 15, 0.1 and 0.000 69 mol/L, respectively, is depicted in Fig. 1. As can be seen, the obtained  $pH_{pzc}$  value is about 6.6.

Based on the dependence of surface charge densir

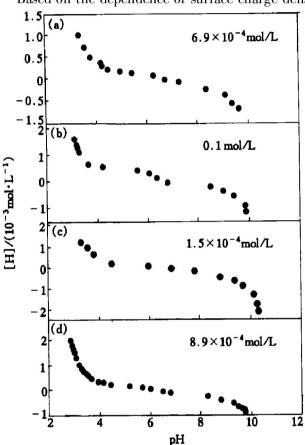


Fig. 1 Surface excessive H vs pH curves in system at different concentration of electrolyte

ty on pH, the surface equilibrium constants and other parameters were calculated as follows.

# **4. 2** Determination of $pK_{Na^+}$ , $pK_{Cl}^-$ by extrapolation

According to Eqns. (18) and (20),  $pK_{Na^+} = 5.24$  and  $pK_{Cl^-} = 8.2$  can be determined by linearity extrapolation of  $pQ_{Na^+}$  or  $pQ_{Cl^-}$  vs  $\alpha$  at  $\alpha = 0$  as shown in Fig. 2(a) and (b).

# 4. 3 Determination of $pK_{a1}$ and $pK_{a2}$

The results of p $K_{\rm al}$  and p $K_{\rm a2}$  at different electrolyte system can be obtained by Fiteql3. 1 software as shown in Table 3. The average values of p $K_{\rm al}$  and p $K_{\rm a2}$  are 5. 20 and 7. 96, respectively. The point of zero charge of TiO<sub>2</sub> can be calculated as

$$pH_{pze} = (pK_{a1} + pK_{a2})/2 = 6.58$$

The point of zero charge for rutile is  $pH_{pzc}$  = 5.4, and that for commercial product P25 (rutile/anatase= 30/70) is 6.25. Our calculation for TiO<sub>2</sub> (anatase),  $pH_{pzc}$ = 6.58, is approximated to that reported by Ref. [13].

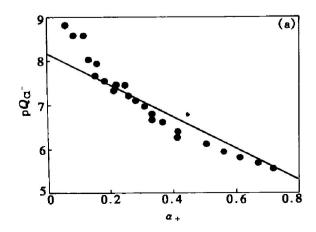
The intrinsic stability constant,  $K_{\,{
m Na}}^{\,{
m int}_+}$  and  $K_{\,{
m Cl}}^{\,{
m int}_+}$  can be calculated as

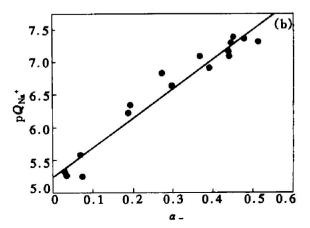
$$\begin{split} \lg K_{\mathrm{Na}}^{\mathrm{int}_{+}} &= \mathrm{p} K_{\mathrm{a2}} - \mathrm{p} K_{\mathrm{Na}^{+}} \,,\; \lg K_{\mathrm{Cl}}^{\mathrm{int}} = \mathrm{p} K_{\mathrm{Cl}^{-}} - \mathrm{p} K_{\mathrm{a1}} \\ \mathrm{so,}\; \lg K_{\mathrm{Na}^{+}}^{\mathrm{int}_{+}} &= 2.72 \text{ and } \lg K_{\mathrm{Cl}}^{\mathrm{int}_{-}} = 3.0, \text{ which is approximated to the calculation by Sprycha}^{[11]},\; \lg K_{\mathrm{Na}^{+}}^{\mathrm{int}_{+}} \\ &= \lg K_{\mathrm{Cl}}^{\mathrm{int}_{-}} = 3.1. \end{split}$$

# 4. 4 Determination of parameters $C_1$ and $C_2$

For the triple layer model, the outer layer capacitance ( $C_2$ ) is assumed to be 0. 2 since this is a reasonable value for compact layer capacitance and provide good agreement with electro-kinetic data<sup>[8]</sup>. The inner layer capacitance ( $C_1$ ) is an adjustable parameter in our model. The capacitance value is relative to dielectric constant of the Stern layer ( $\mathcal{E}$ ) and the distance of charge separation (d) between both electrostatic planes of the Stern layer,

$$C = \mathcal{E}_0 / d$$





**Fig. 2** Linearity regression of p $Q_{Cl}^-$  vs  $\alpha_+$  (a) and p $Q_{Na}^+$  vs  $\alpha_-$  (b)

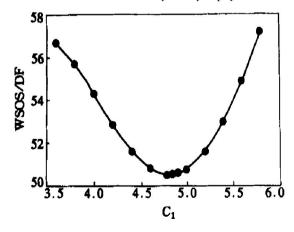
**Table 3** p $K_{a1}$  and p $K_{a2}$  calculated by Fiteq13. 1

Electrolyte concentration/ ( $mol^{\bullet}L^{-1}$ )	$\mathrm{p}K$ $_{\mathrm{al}}$	p $K_{ m a2}$
0.000 89	5. 206	7.865
0.1	5. 216	7.855
0.00069	5. 178	8.087
0.000 15	5. 194	8.038
Average	5. 20	7. 96

The value of  $\varepsilon$  is not known, but its maximum possible value can be taken as  $\varepsilon_b$ , the bulk dielectric constant of water. So, given  $\varepsilon_b = 78.45$ , freedom space penetration coefficient  $\varepsilon_0 = 8.854 \times 10^{-12}$ , the ionic radii of Na<sup>+</sup> and Cl<sup>-</sup> are  $1.02 \times 10^{-10}$  m and  $0.99 \times 10^{-10}$  m at 25 °C, respectively.  $C_1$  maximum value can be estimated to be 6.81 and 6.87, respectively. This help to partially constrain the fitted capacitance.  $C_1 = 4.8$  is obtained through minimization the error value between calculation and experimental data as shown in Fig. 3.

#### 4. 5 Numerical simulation analysis

The comparison between numerical calculation and experimental data is shown in Fig. 4 at system in 0.00089 mol/L electrolyte concentration. The agreement is satisfied. The surface species distribution is shown in Fig. 5. In the range of pH, [  $-SOH_2^+$  ] and [  $-SO^-$ ] are much less than [ -SOH] which is in favor of the theoretical analysis by Sprycha<sup>[11]</sup>.



**Fig. 3** Error values vs  $C_1$ 

#### 5 CONCLUSIONS

In this paper, the surface properties of  $TiO_2$  were described by TLM through the potentiometric titration. The complexation constants were determined by the extrapolation first, then the other parameters were done by Fiteql3. 1 software. For the  $TiO_2$ ,  $pH_{pzc}=6.58$ ,  $pK_{al}=5.20$ ,  $pK_{a2}=7.96$ ,  $pK_{Na}^+=5.24$ ,  $pK_{Cl}^-=8.2$ , and  $C_2=0.2$ ,  $C_1=4.8$ . The numerical calculation fits the experimental

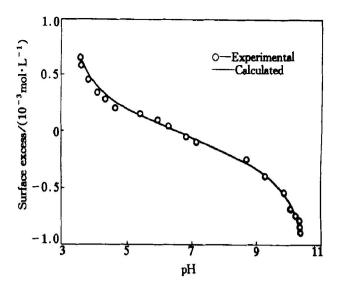
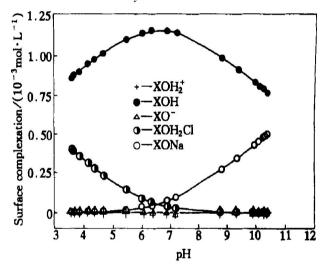


Fig. 4 Comparison between calculated and experimental data at system in 0.000 89 mol/ L electrolyte concentration



**Fig. 5** Distribution of surface species as function of pH

data satisfactorily.

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