

Microscopic mechanism in solvent extraction of $\text{Au}(\text{CN})_2^-$ by cationic surfactant^①

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Abstract: A new solvent extraction system of $\text{Au}(\text{I})$ by surfactant CTMAB-TBP-inert diluent- $\text{Au}(\text{CN})_2^-$ - H_2O was investigated and established. The infrared spectra and the conductivities of loaded organic phases containing $\text{Au}(\text{I})$ were recorded stage by stage. It was reported that in the presence of salting-out agents the percent extraction of $\text{Au}(\text{I})$ decreased, and the conversion of emulsions from W/O to O/W happened in the extraction process. The results demonstrate that the extraction process of $\text{Au}(\text{CN})_2^-$ is carried out by two steps. First, an associated molecule between CTMA^+ and TBP, as $(\text{C}_{16}\text{H}_{33})(\text{CH}_3)_3\text{N}^+ \cdot \text{H}_2\text{O} \cdot \text{O}=\text{P}(\text{OC}_4\text{H}_9)_3$, is formed by dint of water molecule, then it will pull $\text{Au}(\text{CN})_2^-$ into the organic phase based on the electroneutrality.

Key words: surfactant; solvent extraction; $\text{Au}(\text{CN})_2^-$

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1 INTRODUCTION

Since Mooiman, Miller et al^[1, 2] reported their investigation in 1983, solvent extraction of $\text{Au}(\text{CN})_2^-$ from alkaline cyanide solutions has been an attractive project. In the recent years, these studies have been more and more explored, and the representative papers are listed in Refs. [3 - 17].

The solvent extraction of $\text{Au}(\text{CN})_2^-$ by surfactant CTMAB(cetyl trimethyl ammonium bromide) has been studied. It is different from the solvent extraction of $\text{Au}(\text{CN})_2^-$ by quaternary ammonium salts that the first CTMAB is a sort of typical cationic surfactant with a longer carbon-hydrogen chain; the second, it was added into the extracted aqueous phase directly by the molar ratio with $\text{Au}(\text{CN})_2^-$ and the third, the extraction organic phase consists of a sort of inert diluent (*n*-dodecane or sulphonated kerosene) and a sort of modifier with basic group (TBP or mixed-alcohol).

It is interesting, in this extraction system, $\text{Au}(\text{CN})_2^-$ could be highly selectively and quantitatively extracted into the organic phases^[18-21]. It is also important there are some new results, such as the formation of W/O or O/W microemulsions and their conversion, the disruption of emulsions, the variation of infrared spectra and conductivities of the organic phases containing gold and the influence of adding the salting out agents in aqueous

phase.

In this paper we try to show the microscopic process in solvent extraction of $\text{Au}(\text{CN})_2^-$ by cationic surfactant based on some new idea.

2 EXPERIMENTAL

2.1 Materials

Aurous solution was prepared by aurous potassium cyanide, $\text{KAu}(\text{CN})_2$, with AR grade, and the initial concentration was 5.077×10^{-3} mol/L containing Au 1.002 g/L. Sulphonated kerosene was obtained by refining the commercial kerosene. Tributylphosphate(TBP), cetyl trimethyl ammonium bromide(CTMAB) and other chemicals used are of AR grade.

2.2 Determination of gold content

The gold contents in the raffinates and the organic phase were determined by Z-8000 Atomic Absorption Spectrograph or 722 Spectrophotometer.

2.3 Infrared spectroscopy

The infrared spectra of the organic phase in the ranges $670 - 3550 \text{ cm}^{-1}$ and $2850 - 8850 \text{ cm}^{-1}$ were obtained by using a SP100 Infrared Spectrometer.

2.4 Conductance

The conductivities of the organic phase were

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determined by using a DDS-11A Conductometer at $(25 \pm 0.5) \text{ }^\circ\text{C}$.

2.5 Extraction systems

The six extraction systems in Fig. 1 were investigated. The extraction system F was composed of five components, containing surfactant, modifier, inert diluent, $\text{Au}(\text{CN})_2^-$ and water. It could be evolved either from the system A to B to D or A to C to E. The dosage and volume of components and the character of phenomena in the six systems are listed in Table 1.

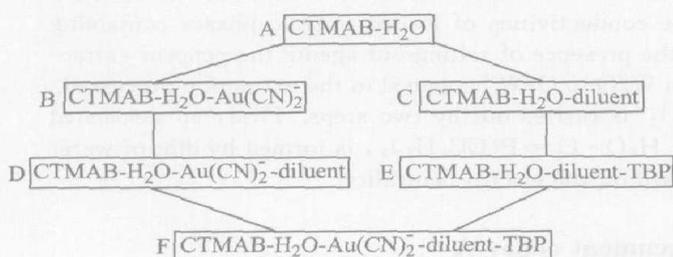
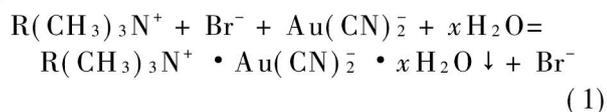


Fig. 1 Evolution of five element extraction system

3 RESULTS AND DISCUSSION

3.1 System B: CTMAB·H₂O·Au(CN)₂⁻

Since the CTMAB aqueous solution was added into the $\text{NaAu}(\text{CN})_2$ solutions by mole ratio 1 : 1 with Au, immediately, then it can be seen that the white exiguous precipitate was formed. This is due to the fact that the body of $\text{Au}(\text{CN})_2^-$ is bigger than that of Br^- , while its surface charge density is much smaller, so the hydration of $\text{Au}(\text{CN})_2^-$ is much weaker, and is easy to form the big neutral molecule with $\text{C}_{16}\text{H}_{33}(\text{CH}_3)_3\text{N}^+$ according to Eqn. (1).



where R represents the $\text{C}_{16}\text{H}_{33}$ group. In the aqueous

solutions, the surfactant itself is easy to form the colloid owing to the twist of long chain alkyl, the precipitate formed in the reaction may be a sort of ion association among which the hydrophilic group is wrapped up, even some of water molecules carried in.

The white precipitate was altered out through the compact filter paper, and dried out by the vacuum drier, and then analyzed on the components of it. The results obtained show that the components of the precipitate are $\text{Au}(\text{CN})_2^-$, CTMAB and H_2O , and their mole ratio is 5.846 : 7.309 : 1, respectively. In the aqueous phase, as we have known, the molar of CTMAB was the same as the $\text{Au}(\text{CN})_2^-$, so the gold contained in the precipitate is about 80% of the total gold content, and it indicates that $\text{Au}(\text{CN})_2^-$ could only be precipitated by 80% in Eqn. (1).

3.2 System D: CTMAB·H₂O·Au(CN)₂⁻-inert diluent

The equal volume of inert diluent was added into the system C containing the white precipitate, then shaken, and laid aside for 24 h, a coexistent three-phase system was obtained, as shown in Fig. 2. The up-layer is the clear organic phase and the down layer is clear aqueous phase, while the middle layer is emulsion. The gold contents in the aqueous phase and organic phase were analyzed chemical method. The obtained data show that their gold contents are all quite low, which indicates that the $\text{Au}(\text{CN})_2^-$ is mainly gathered in the white emulsion. This can be explained as that the precipitate in Eqn. (1), $\text{R}(\text{CH}_3)_3\text{N}^+ \cdot \text{Au}(\text{CN})_2^- \cdot x\text{H}_2\text{O}$, was insoluble in the inert diluent. Even though some of its hydrophobic groups R— have been inserted in the organic phase, the hydrophilic end with positive charge and the counter ion $\text{Au}(\text{CN})_2^-$ with negative charges as well as the water molecules wrapped into the above two polar groups all yet cannot be extracted into the

Table 1 Dosage and volume of components and characters of these systems

System	Component					Phenomena
	$n(\text{CTMAB}) / \text{mmol}$	$V(\text{H}_2\text{O}) / \text{mL}$	$V(\text{inert diluent}) / \text{mL}$	$n(\text{Au}(\text{CN})_2^-) / \text{mmol}$	$V(\text{TBP}) / \text{mL}$	
A	0.0508	10	0	0	0	Surface tension decrease, forming bubble
B	0.0508	10	0	0.0508	0	Forming white fine precipitation
C	0.0508	10	10	0	0	W/O emulsion, aqueous phase clear
D	0.0508	10	10	0.0508	0	Forming the third phase, aqueous-oil phases clear, Au(I) in the third phase
E	0.0508	10	7	0	3	O/W emulsion, organic phase clear
F	0.0508	10	7	0.0508	3	Quick disengagement, clear aqueous-oil phases, Au(I) extraction > 98%

pH = 10.5, 10 min

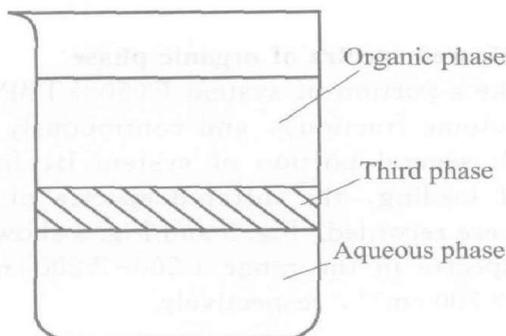


Fig. 2 Formation of third phase of system D

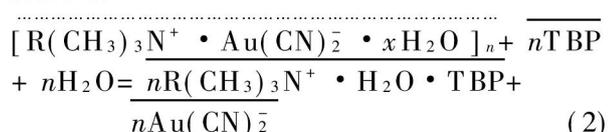
organic phase, so the precipitate containing gold concentrated in the milky third phase of the middle layer.

3.3 System F: CTMAB-H₂O-Au(CN)₂⁻-inert diluent-TBP

Since the equal volume of the organic phase of 50% TBP in *n*-dodecane was added into system B, shaken and then laid aside, the system quickly divided into two clear up and down layers. While if an amount of TBP was added into the system D directly, the milky third phase disappeared. The concentration of Au(I) in the two aqueous phases are all dropped to 0.022 g/L, and the one-run percentage extraction of gold are all about 98%. These can be explained that a sort of polar head-to-polar head associated molecule between the Lewis acid CTMA⁺ and the Lewis alkali TBP, or a sort of associated molecule by dint of the hydrogen bonding of water molecule was formed. The following facts will indicate that, the associated molecule formed mainly depends on the bridging of the hydrated water in $\text{R}(\text{CH}_3)_3\text{N}^+ \cdot \text{OH}_2$ or the hydrated water of the $\text{P}=\text{O}$ bond in TBP.

The hydration energy released from the association will compensate the energy needed by stripping the weak hydrated layer of $\text{Au}(\text{CN})_2^-$, and the $\text{Au}(\text{CN})_2^-$ will be extracted into the organic phase based on the electric neutrality principle.

Using 50% TBP in *n*-dodecane as the extraction organic phase, the extraction reaction can be expressed as



where the dotted line and the full line represent the aggregates in the third phase and the organic phase, respectively. Eqn. (2) shows that, TBP makes the associate between the surfactant and $\text{Au}(\text{CN})_2^-$ decomposed. This is due to the fact that the hydrophilic group in the $\text{R}(\text{CH}_3)_3\text{N}^+ \cdot \text{H}_2\text{O} \cdot \text{O}=\text{P}(\text{OC}_4\text{H}_9)_3$ is enwrapped, and the unit positive charge is distributed over the several methylic

hydrogens, easy to be solvated by water and TBP molecules, the surfactant loses the surface activity, unnecessary to array at the interface of the organic and aqueous phase, and also unnecessary to associate with the $\text{Au}(\text{CN})_2^-$ in the organic phase. So the conductivity of the organic phase increases with the extraction stages.

3.4 System C: CTMAB-H₂O-inert diluent

The equal volume of inert diluent, *n*-dodecane or sulfonated kerosene, was added into the CTMAB aqueous solution, and shaken in the separatory funnel, and then laid aside for the phase disengagement. We can see the down-layer aqueous phase is clear, but the up-layer organic phase is emulsive, that is, the W/O emulsion is formed. The W/O emulsion structure formed in the organic phase are shown in Fig. 3.

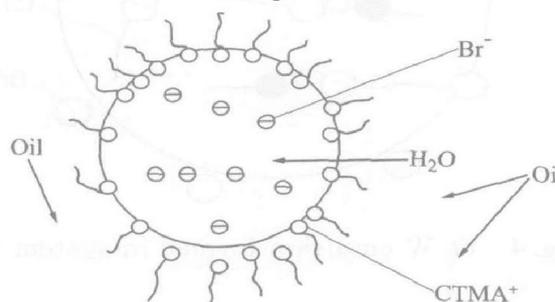


Fig. 3 W/O emulsion structure formed in organic phase

It is thinkable for that, in fact, CTMAB is soluble in anhydrous inert diluent at some extent, and its solubility increases with the temperature; but if the organic phase is contacted with the CTMAB aqueous solution, the hydrophilic group of the surfactant will be inserted in the water as shown in Fig. 3. On the other hand, the hydrophilicity of Br^- is stronger and it has a strongly hydrated shell, so that it can not be extracted into the organic phase.

3.5 System E: CTMAB-H₂O-inert diluent-TBP

A moderate amount of TBP was added into the system C, shaken, and then laid aside for a while, the up-layer of the system become clear, while the down-layer emulsive. Increasing the dosage of CTMAB to some extent, the interface of water-oil phases disappeared, the whole system is emulsive. This emulsion system is very stable, and not varied for one month.

As far as we know, this important result has not been reported by other authors elsewhere. We think the TBP in the extraction process does not serve the function of an assistant surfactant, but converts the W/O into the O/W emulsion.

Fig. 4 shows the conversion process. Since

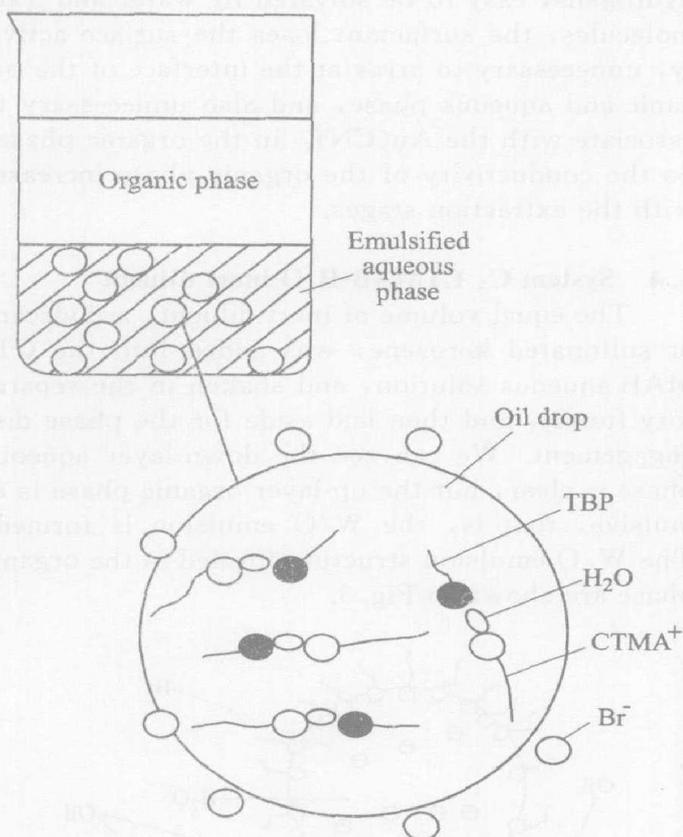


Fig. 4 O/W emulsion formed in system E

TBP was added into system C, the hydrophilic end of the cation CTMA⁺ arrayed over the interface of oil-water phases will associate with the basic group P=O in TBP by virtue of the bridging of water molecules, and draw the ammonium group inserted in the water into organic phase. The positive charge in the organic phase will exclude with each other and make the organic phase to divide into many of small oil drops with positive charge. The Br⁻ was absorbed around the surface of the small oil drops, and so the stable O/W emulsion was formed. It was observed under the microscope with the dyeing method. We could see that the colorful water is a continuous phase.

Since the aurous solutions containing Au(CN)₂⁻ was added into the system E, for the lower face charge density of Au(CN)₂⁻, the Au(CN)₂⁻ would be pulled into the organic phase priorotically and the organic phase became electroneutrality. The driving force of Au(CN)₂⁻ into the oil drops is similar to the electric-osmotic force. The electroneutral oil drops quickly, combines with each other, grows up, and becomes system F that is clear and diaphanous water-oil phases.

The O/W emulsive phase of system E can also be disrupted by adding NaClO₄ or NaSCN solution. This is due to the lower face charge density of ClO₄⁻ and SCN⁻ than Br⁻, easy to be pulled into the tiny oil-drops to neutralize the positive

charge in them.

3.6 Infrared spectra of organic phase

Take a portion of system F (50% TBP-*n*-dodricane, volume fraction), and continuously contacted with several portion of system B, for every stage of loading, the infrared spectra of organic phase were recorded. Fig. 5 and Fig. 6 show the infrared spectra in the range 1 200-2 200 cm⁻¹ and 3 100-3 700 cm⁻¹, respectively.

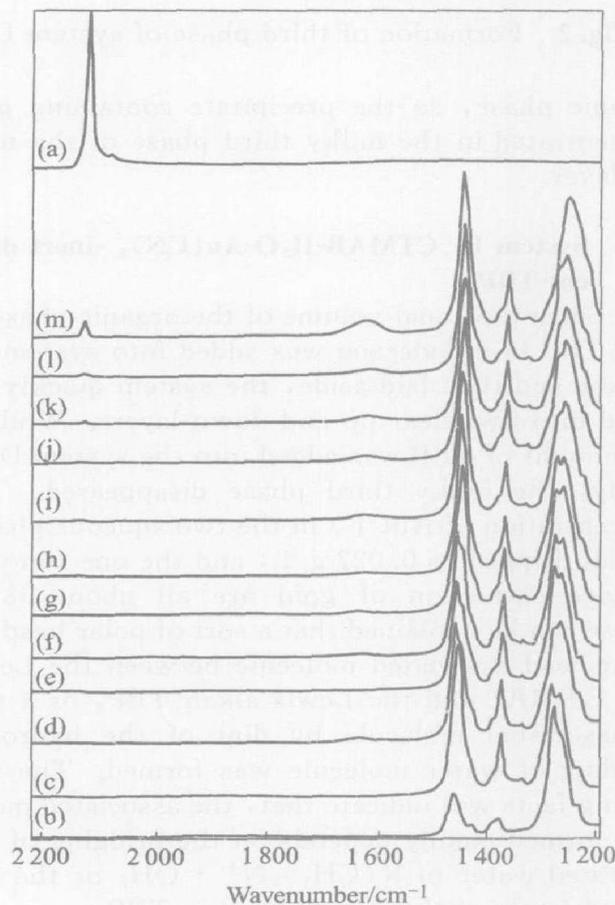


Fig. 5 Infrared spectrum of stage-by-stage loaded organic phase in range of 1 400 - 2 200 cm⁻¹
 (a) -KAu(CN)₂; (b) -50% TBP-*n*(dodicane);
 (c) -1st extracted; (d) -2nd extracted; (e) -3rd extracted;
 (f) -4th extracted; (g) -5th extracted; (h) -6th extracted;
 (i) -7th extracted; (j) -8th extracted; (k) -9th extracted;
 (l) -10th extracted; (m) -24th extracted

In Fig. 5, it can be seen that, the intensity of C≡N stretching band at 2 141 cm⁻¹ increases with the extraction steps, this is due to the fact that the loaded Au(CN)₂⁻ content in the organic phases increases with the extraction steps. And the 1 284 cm⁻¹ band of P=O stretching mode moves to lower frequency, 1 264 cm⁻¹, but the band area does not vary obviously. This may be due to the extractive cation among TBP, CTMA⁺ and H₂O, named as R(CH₃)₃N⁺ · OH₂ · O=P(OC₄H₉)₃, is formed in the system. We know that the O=P group in TBP is H-bonding associated with H₂O in the system, while the positive charges

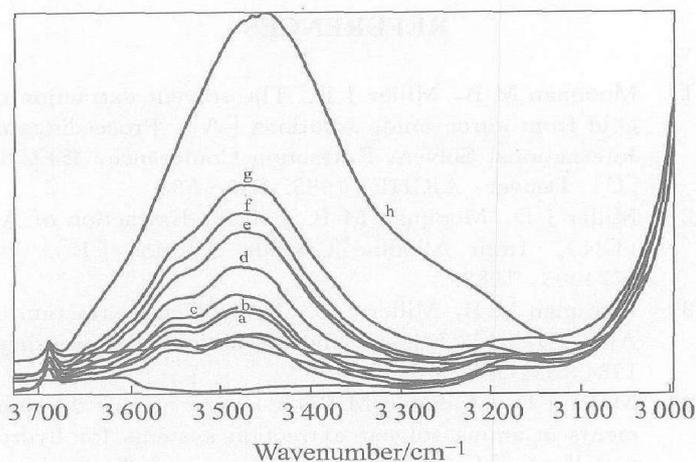


Fig. 6 Infrared spectrum of stage-by-stage loaded organic phase in range of $3100 - 3700 \text{ cm}^{-1}$

- (a) —2nd extracted; (b) —2rd extracted;
 (c) —4th extracted; (d) —5th extracted;
 (e) —6th extracted; (f) —7th extracted;
 (g) —8th extracted; (h) —24th extracted

in quaternary ammonium cation may be distributed over the methylic hydrogens by the induction effect, so that the methylic hydrogen with δ^- charge will associate with the oxygen in the water.

With the increase of the extraction stages, the concentration of the associated cation, $[\text{R} - (\text{CH}_3)_3\text{N}^+ \cdot \text{OH}_2 \cdot \text{TBP}]$, in the organic phase stepwise increases, and the frequency shift of $\text{P}=\text{O}$ group stretching mode became more and more obvious.

For the question how many H_2O and TBP molecules were associated with a quaternary ammonium cation, it is necessary to study further. Here we postulate all as one for H_2O and TBP molecule.

As shown in Fig. 6, with the increase in the extraction stages, the intensities and the area of $-\text{OH}$ stretching band at 3462 cm^{-1} became more and more large due to the increase of the H_2O content in the organic phases, while it has been thought the coming from the increase of the surfactant molecules extracted into the organic phases. This fact supports the precious discussion on the extraction mechanism. We have more detailed explanation about the infrared spectra of the organic phase^[22, 23].

3.7 Conductivities of organic phase

Fig. 7 shows the conductivities of the loaded organic phase in different extraction steps. It can be seen that the conductivities increase with the gold concentration in the organic phases and reach a maximum value at 11.24 g/L gold concentration, and then decrease. It may be due to the fact that, at beginning, the $\text{Au}(\text{CN})_2^-$ extracted in the organic phases existed in free state, as just shown in

Eqn. (2), the lower gold concentration in the organic phase made the lower conductivity, and increased with the gold concentration in the organic phase until the occurrence of the associated cation, $[\text{R}(\text{CH}_3)_3\text{N}^+ \cdot \text{OH}_2 \cdot \text{O} = \text{P}(\text{OC}_4\text{H}_9)_3]$, in the organic phases or the formation of W/O microemulsion packed $\text{Au}(\text{CN})_2^-$, then immediately decreased, and on this, we can see the organic phase separated into two layers, a light layer and heavy layer.

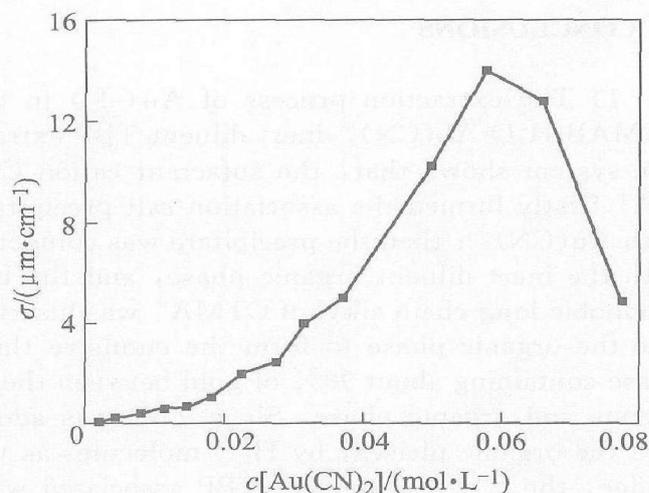


Fig. 7 Conductivities of stage-by-stage loaded organic phase

3.8 Salting out effects in aqueous phase

Adding Li, Na, K, Ca and Mg chloride into system A, their effect on the gold extraction is shown in Fig. 8.

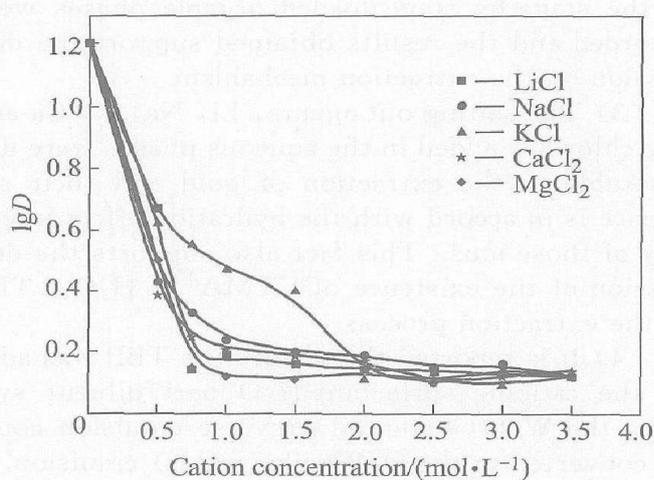


Fig. 8 Influence of salting out agents on distribution ratio of gold

In Fig. 8 we observe the addition of these salting out agents is unfavorable to the gold extraction. When the concentration of these chlorides in the aqueous phases is higher than 0.75 mol/L , the percent gold extraction is decreased sharply. Their influence sequence for the percent gold extraction is $\text{Li}^+ > \text{Na}^+ > \text{K}$, and $\text{Mg}^{2+} > \text{Ca}^{2+}$. That is just

the sequence of decreasing hydration of these ions due to the increase of their ion radii. This means the addition of the salting out agents decreases the water activity and is unfavorable to the formation of the associated cation, $\text{CTMA}^+ \cdot \text{H}_2\text{O} \cdot \text{TBP}$, which is bridged by H_2O molecule, so the percent gold extraction is decreased, which is the same as that reported on solvent extraction of Zr(IV) in hydrochloride acid system^[24].

4 CONCLUSIONS

1) The extraction process of Au(I) in the $\text{CTMAB-H}_2\text{O-Au(CN)}_2^-$ -inert diluent-TBP extraction system shows that, the surfactant cation CTMA^+ firstly formed the association salt precipitate with Au(CN)_2^- ; then the precipitate was contacted with the inert diluent organic phase, and the hydrophobic long-chain alkyl of CTMA^+ was inserted into the organic phase to form the emulsive third phase containing about 98% of gold between the aqueous and organic phase. Since TBP was added into the organic phases, by H_2O molecules as the bridge, the P=O group of TBP associated with the hydrophilic end of CTMA^+ to form the large cations. Perhaps the hydrophilic part located in the middle of the large cation lost the surface activity, so that the large ion were easy to be dissolved into the inert diluent; and then Au(CN)_2^- with lower face charge density will be drawn in the organic phase based on the electroneutrality.

2) The infrared spectra and the conductivities of the stage-by stage loaded organic phases were recorded and the results obtained support the discussion on the extraction mechanism.

3) The salting out agents, Li, Na, K, Ca and Mg chloride, added in the aqueous phases were unfavorable to the extraction of gold and their sequence is in accord with the hydration effect intensity of those ions. This fact also supports the discussion of the existence of $\text{CTMA}^+ \cdot \text{H}_2\text{O} \cdot \text{TBP}$ in the extraction process.

4) It is reported that, since the TBP was added the cationic surfactant- H_2O -inert diluent system, the W/O (water/oil) reverse emulsion could be converted to the O/W (oil / water) emulsion.

5) The main driving force in the extraction of Au(CN)_2^- by cationic surfactant CTMAB (or other quaternary ammonium salts) is the association among CTMA^+ , H_2O and TBP in the inert diluent, which lowers the energy of the system due to the evolution of the hydration energy, and the large cation $\text{CTMA}^+ \cdot \text{H}_2\text{O} \cdot \text{TBP}$ will pull Au(CN)_2^- with lower hydration energy into the organic phase by the coulombic force.

REFERENCES

- [1] Mooiman M B, Miller J D. The solvent extraction of gold from aurocyanide solutions [A]. Proceedings of International Solvent Extraction Conference, ISEC'83 [C]. Denver: AICHE, 1983. 530 - 531.
- [2] Miller J D, Mooiman M B. Solvent Extraction of Au(CN)_2^- from Alkaline Cyanide Solution [P]. US 4774003, 1988.
- [3] Mooiman M B, Miller J D. The solvent extraction of Au(CN)_2^- [J]. Mineral and Metallurgical Processing, 1984, 53: 157 - 162.
- [4] Miller J D, Mooiman M B. A review of new developments in amine solvent extraction systems for hydrometallurgy [J]. Separation Science and Technology, 1984 - 85, 19(11 - 12): 895 - 909.
- [5] Mooiman M B, Miller J D. The chemistry of gold solvent extraction from cyanide solution using modified amines [J]. Hydrometallurgy, 1986, 16: 245 - 251.
- [6] Riveros P A. Studies on the solvent extraction of gold from cyanide media [J]. Hydrometallurgy, 1990, 24: 135 - 156.
- [7] Alguacil F J, Caravaca C, Martinez S. Extraction of gold from cyanide or chloride media by cyanex 923 [J]. Journal of Chem Technol Biotechnol, 1998, 72: 339 - 346.
- [8] Alguacil F J, Hernandez A, Luis A. Study of the KAu(CN)_2^- -amine amberlite LA-2 extraction equilibrium system [J]. Hydrometallurgy, 1990, 24: 157 - 168.
- [9] Caravaca C, Alguacil F J, Sastre A, et al. Extraction of gold(I) cyanide by the primary amine tridecylamine [J]. Hydrometallurgy, 1996, 40: 89 - 97.
- [10] Caravaca C, Alguacil F J, Sastre A. The use of primary amines in Gold(I) extraction from cyanide solutions [J]. Hydrometallurgy, 1996, 40: 263 - 275.
- [11] Caravaca C, Alguacil F J. Gold(I) extraction equilibrium in the system KAu(CN)_2 primene JMT sulphate xylene [J]. Hydrometallurgy, 1992, 31: 257 - 264.
- [12] Caravaca C, Alguacil F J. Extraction of gold from cyanide aqueous media by primene JMT [J]. Hydrometallurgy, 1994, 35: 67 - 78.
- [13] Miller J D, Wan R Y, Mooiman M B, et al. Selective solvation extraction of gold from alkaline cyanide solution by alkyl phosphorous esters [J]. Separation Science and Technology, 1987, 22(2/3): 487 - 502.
- [14] Alguacil F J, Caravaca C, Coba A, et al. The extraction of gold(I) from cyanide solutions by the phosphine oxide cyanex 921 [J]. Hydrometallurgy, 1994, 35: 41 - 52.
- [15] Alguacil F J, Caravaca C, Martinex S, et al. The phosphine oxides cyanex 923 and cyanex 925 as extractants for gold(I) cyanide aqueous solutions [J]. Hydrometallurgy, 1994, 36: 369 - 384.
- [16] Kordosky G A, Sierakoski J M, Virnig M J, et al. Gold solvent extraction from typical cyanide leach solutions [J]. Hydrometallurgy, 1992, 30: 291 - 305.
- [17] Mooiman M B, Miller J D. The chemistry of gold solvent extraction from alkaline cyanide solution by solvating extractants [J]. Hydrometallurgy, 1991, 27: 29 - 46.
- [18] Zhu L Y, Chen J, Jing Y Q, et al. Solvent extraction of Au(CN)_2^- when additive added into aqueous phase [J]. The Chinese Journal of Nonferrous Metals,

- 1996, 6(2): 229 - 232. (in Chinese)
- [19] Pan X J, Chen J. Solvent extraction of gold(I) when additive added into aqueous phase [A]. The National Metallurgical Physical Chemistry Society. Proceedings of 1996 the National Symposium on Metallurgical Physical Chemistry [C]. Kunming: The National Metallurgical Physical Chemistry, 1996. 206 - 213. (in Chinese)
- [20] Chen J, Zhu L Y, Jing Y Q, et al. Solvent extraction of gold cyanide with tributylphosphate and additive added into aqueous phase [A]. Manziek Rohm & Haas Company. Precious Metals 1998 [C]. Toronto, Ontario, Canada: International Precious Metals Institute, 1998. 65 - 74.
- [21] Huang K, Chen J. Solvent extraction of gold(I) in mixed alcohol diluent-surfactant- $\text{Au}(\text{CN})_2^-$ system [A]. Deng D G. Proceedings of the International Symposium of Precious Metals, ISPM'99 [C]. Kunming: Yunnan Science and Technology Press, 1999. 283 - 288. (in Chinese)
- [22] Yan W F, Ma G, Weng S P, et al. Solvent extraction mechanism of $\text{Au}(\text{CN})_2^-$ by surfactant from the alkali cyanide solution [J]. Acta Scientiarum Naturalium Universitatis Pekinensis, 2000, 36(2): 461 - 466.
- [23] Yan W F, Ma G, Chen J, et al. Mechanism of $\text{Au}(\text{CN})_2^-$ solvent extraction by surfactant [J]. Spectroscopy and Spectral Analysis, 1999, 19(6): 806 - 810.
- [24] Yu S Q, Chen J Y. Discussion on salting-out effect for two different solvent extraction mechanism [J]. Acta Metallurgical Sinica, 1984, 20(6): B342 - 351.

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