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Electrosynthesis of Al/Pb/ α -PbO₂ composite inert anode materials

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Abstract: The α -PbO₂ deposition layers were prepared on the surface of Al/Pb substrates by constant current electrosynthesis from an alkaline bath, and Al/Pb/ α -PbO₂ composite inert anode materials were obtained. The effects of the bath composition and bath temperature on the electrosynthesis of α -PbO₂ were investigated by means of anodic polarization method, the phase structures and surface microstructures of Al/Pb and α -PbO₂ deposition layers were tested by means of X-ray diffraction (XRD) and scanning electron microscopy (SEM), respectively. The experimental data have shown that the process of α -PbO₂ formation have several stages. The appropriate conditions can effectively improve the formation rate of α -PbO₂ and avoid the occurrence of oxygen evolution reaction. The α -PbO₂ deposition layer obtained in alkaline bath possesses rhombic structure, and it is composed of well developed spherical unit cells.

Key words: Al/Pb substrate; α-PbO₂; electrosynthesis; anodic polarization

1 Introduction

The anode material is one of the critical components in the process of zinc electrowinning. The direction and kinetics of electrode process, structure of electrolytic cell and power consumption are closely related to not only the electrolyte composition but also the property of the electrode materials. Only some inert materials such as Pb and Pb-based alloys, PbO₂, Fe₃O₄, Pt and Pt group metal oxides can exist steadily in the electrowinning process which mostly happened in the sulfuric acid medium, and its main anode reaction is the oxygen evolution. In addition, the corrosivity of sulfuric acid and the oxidizing ability of new generated oxygen are strong. PbO₂ has attracted extensive attention due to its good electrochemical performance and stability in the acidic medium. At present, a new type of metal substrate/ $\alpha(\beta)$ -PbO₂ composite inert anode materials is the research hotspot of hydrometallurgy. The thermal decomposition coating is served for the underlayer, such as silver or lead silver alloys, palladium oxides, tin-antimony oxides and titanium-tantalum composite oxides. The α -PbO₂ is used for the interlayer between the Ti substrate and β -PbO₂. In such way, the stability and corrosion resistance of $Ti/\alpha(\beta)$ -PbO₂ composite inert anode materials can be effectively improved as the Ti substrate passivation can be inhibited and the stress between the coatings can be reduced [1–4]. However, the preparation of $Ti/\alpha(\beta)$ -PbO₂ composite inert anode materials is complicated with high cost. Moreover, the passivation of Ti substrate cannot be solved fundamentally. So, the application of $Ti/\alpha(\beta)$ -PbO₂ in zinc electrowinning is unsuitable [5,6]. Some hydrometallurgy researchers have put forward to Al/Pb/ $\alpha(\beta)$ -PbO₂ composite inert anode materials in recent years [7,8].

The α -PbO₂ working as the interlayer has remarkable impacts on the performance of Al/Pb/ $\alpha(\beta)$ -PbO₂ composite inert anode materials. Therefore, it is significant to study the electrosynthesis of α -PbO₂ on

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Al/Pb. The study of Al/Pb/ α -PbO₂ shows that there is PbO impurity phase existing in α -PbO₂, and the higher the current density of α -PbO₂ electrochemical synthesis is, the greater the roughness and porosity of the deposition layer are [9]. Furthermore, the factors of the Pb(II) concentration, bath temperature and electrosynthesis time can also influence the electrosynthesis of α -PbO₂. The α -PbO₂ deposition layers prepared at room temperature usually present loose structure of clusters, but the compact layers can be obtained at 40 °C [9,10]. When α -PbO₂ is electrochemically synthesized in alkaline bath, tender stirring can prevent the generation of reddish brown and loosely bound PbO. And the α -PbO₂ synthesized may partly transform into reddish brown PbO when Pb(II) is insufficient in bath [11]. The PbO₂ synthesized through constant current presents more compact structure and more excellent performance than that synthesized through constant voltage, as the former method can control the PbO₂ electrosynthesis rate by adjusting the current density [12,13].

In this research, the α -PbO₂ deposition layers were prepared on the surface of Al/Pb substrates by constant current electrosynthesis from an alkaline bath, and Al/Pb/ α -PbO₂ composite inert anode materials were obtained. The effects of the NaOH concentration, the addition amount of PbO and the bath temperature on the electrosynthesis of α -PbO₂ were investigated by means of anodic polarization method, the phase structures and surface microstructures of Al/Pb substrates and α -PbO₂ deposition layers were tested by means of X-ray diffraction (XRD) and scanning electron microscopy (SEM), respectively. The research results are helpful to provide theoretical basis and technical support for the preparation of Al/Pb/ α -PbO₂ composite inert anode materials.

2 Experimental

The Al sheets with dimensions of 20 mm \times 40 mm \times 2 mm were used as the substrates of the inert anode materials. The pretreatment of Al substrates was performed by the procedures such as polishing, sand blasting, chemical degreasing, and zinc galvanizing twice. Then, the Al/Pb was obtained by cathodic electrochemical synthesizing Pb underlayer on Al with double-pulse method. Finally, the Al/Pb/ α -PbO₂ was obtained by anodic electrochemical synthesizing α -PbO₂ on Al/Pb at constant current.

The bath components of cathodic electrochemical synthesis Pb underlayer were as follows: 180 g/L Pb(AC)₂, 220 mL/L HBF₄, 20 g/L H₃BO₃, 1 g/L gelatin, 0.2 g/L thiourea, 5 mL/L polyethylene glycol. The parameters of the double-pulse were as follows: the

forward and reverse duty ratios of pulse were 10% and 30%, respectively; the average current densities of forward and reverse pulse were 4 A/dm² and 0.4 A/dm², respectively; the forward and reverse working time of pulse were 200 ms and 20 ms, respectively. The bath temperature was 35 °C and the electrosynthesis time was 0.5 h with the pH smaller than 1. The Pb sheet was used as the anode material and the Al sheet was used as the cathodic material.

The electrosynthesis of α -PbO₂ on the surface of Al/Pb was performed on a DDZ–20A/12V rectifier. The bath components of α -PbO₂ electrosynthesis contained 20–50 g/L PbO and 120–160 g/L NaOH, and the bath temperature was 25–45 °C. The Al/Pb was used as the anode material and the stainless steel sheet was used as the cathodic material. In addition, the red sediments generated during the preparation of α -PbO₂ baths were removed by filtration.

All the electrochemical tests of anodic polarization, galvanostatic polarization and quasi-steady state polarization were performed on a PARSTAT2273 electrochemical workstation with three-electrode system. The working electrode, whose effective area was 1 cm^2 , was dealt with wax-sealing. The reference electrode was saturated calomel electrode (SCE). The counter electrode was graphite electrode. The reference electrode and the working electrode were linked by luggin capillary filled with KCl and agar. In addition, the distance between the capillary and the working electrode surface was about 2d(*d* is the diameter of the capillary) to minish the solution resistance and avoid shielding the electrode surface to the greatest extent. The quasi-steady state polarization curve was obtained under the condition that the current density at 0.1-0.8 V was stable for more than 2 min. All the potentials shown in the figures were against the SCE.

The concentration of Pb(II) in α -PbO₂ bath was tested by a Z-2310 atomic absorption spectrometer. The phase composition and surface microstructure characteristics of the Pb underlayers and α -PbO₂ deposition layers were tested by a D/Max-2200 X-ray diffractometer (XRD) and a VEGA3SBH scanning electron microscope (SEM), respectively.

3 Results and discussion

3.1 Effect of NaOH concentration on *a*-PbO₂ electrosynthesis

The anodic polarization curves of the electrosynthesis of α -PbO₂ on Al/Pb at 25 °C are shown in Fig. 1.

As can be seen from Fig. 1, the anodic polarization curve of Al/Pb in 120 g/L NaOH pure solution shows four peaks. Peak $A_{\rm I}$ appears at the beginning, and then the current density gradually decreases and reaches a



Fig. 1 Anodic polarization curves of Al/Pb in alkaline baths at 25 °C (Scan rate: 10 mV/s)

steady value as the Pb underlayer can be oxidized to form a PbO passivating film in alkaline bath. The Pb passivation can be shown as Reaction (1) [14,15]. The PbO film may break during its growth process, thus promoting the Pb oxidation again. Therefore, the current density increases slightly and peak A_{II} appears at about 0.32 V.

$$Pb+2OH^{-}-2e=PbO+H_{2}O$$
(1)

The current density increases rapidly and peak A_{III} appears at about 0.4 V when the potential reaches 0.36 V. Peak A_{III} may be the formation peak of Pb₃O₄ by the oxidation of PbO according to Reaction (2). The appearance of subsequent peak A_{IV} (about at 0.43 V) reflects the formation of α -PbO₂ [16,17], which can be expressed by Reactions (3) and (4). Then, the current density drops rapidly and achieves stability (about 5 mA/cm^2) as the potential is greater than 0.43 V. This is because the electrosynthesis rate of α -PbO₂ may slow down when it reaches the maximum, and the reaction nearly stops after an α -PbO₂ film generates on the Pb surface. However, the α -PbO₂ film is loose and falls off easily. Thus, the Pb or Pb oxides with intermediate state near the cracks could be continuously oxidized to form α -PbO₂ slowly. When the potential is greater than 0.7 V, the current density rises exponentially caused by oxygen evolution. The corresponding reaction is shown as Reaction (5).

$$3PbO+2OH^{-}-2e=Pb_{3}O_{4}+H_{2}O$$
(2)

$$Pb_{3}O_{4}+4OH^{-}-4e=3\alpha-PbO_{2}+2H_{2}O$$
(3)

$$PbO+2OH^{-}-2e=\alpha-PbO_{2}+H_{2}O$$
(4)

$$4OH^{-}-4e=O_{2}+2H_{2}O$$
 (5)

The anodic polarization curves of Al/Pb in different α -PbO₂ baths (40 g/L PbO, 120–160 g/L NaOH) show that, the current densities of Pb passivation and peak A_{IV} (the formation peak of α -PbO₂) decrease significantly, but the initial oxygen evolution potential increases. This

is because, the Pb(II) (HPbO₂⁻) exists in α -PbO₂ baths and the concentration of OH⁻ ions in them is lower than that in 120 g/L NaOH pure solution. These can be understood by Reactions (6) and (7). Therefore, the Pb oxidation rate decreases and the oxygen generation reaction becomes more difficult. In addition, the current density after peak A_{IV} drops slowly due to the electrosynthesis of α -PbO₂, and the current density at 0.55–0.72 V is obviously higher than that in 120 g/L NaOH pure solution. Particularly, the peak A_{II} becomes not so obvious, which may indicate that the primary cause of the fracture of PbO film is the high concentration of OH⁻ ions.

The electrosynthesis of α -PbO₂ can be expressed as follows [18]:

$$PbO+OH^{-}=HPbO_{2}^{-}$$
(6)

$$HPbO_2 + OH - 2e = \alpha - PbO_2 + H_2O \tag{7}$$

The above analysis shows that, the anodic polarization curves of Al/Pb in α -PbO₂ baths can be roughly divided into four parts. They are as follows: 0-0.35 V is the Pb underlayer passivation region, 0.35–0.55 V is the mixed region that the Pb passivation proceeds simultaneously with the α -PbO₂ synthesis, 0.55–0.72 V is the α -PbO₂ electrosynthesis region, and 0.72–0.80 V is the mixed region that the α -PbO₂ electrosynthesis occurs simultaneously with oxygen evolution (oxygen evolution region for short). It can be deduced that when electrosynthesis of α -PbO₂ on Al/Pb takes place in the bath, the surface of Pb underlayer firstly is passivated to form a poor conductive PbO film. Then, the electrosynthesis of α -PbO₂ proceeds simultaneously with step by step oxidation of PbO $(PbO \rightarrow Pb_3O_4 \rightarrow \alpha - PbO_2 \text{ or } PbO \rightarrow \alpha - PbO_2)$. The continual α -PbO₂ deposition layer is mainly formed by the oxidation of Pb(II) in the bath after the Pb surface is covered by an α -PbO₂ film.

It can also be seen from Fig. 1 that, the current densities of Pb underlayer passivation (0-0.35 V), α -PbO₂ electrosynthesis (0.55–0.72 V) and peak $A_{\rm IV}$ increase with increasing the NaOH concentration in different α -PbO₂ baths. And the initial oxygen evolution potential decreases from about 0.76 to 0.72 V. It is mainly because the increase of NaOH concentration is beneficial to Reaction (6), thus increasing the Pb(II) concentration. And the concentration of OH⁻ ions also increases with increasing the NaOH concentration. Therefore, the rates of Pb passivation and α -PbO₂ electrosynthesis increase, and the oxygen evolution becomes easier. This can be confirmed by the testing of Pb(II) concentration in every α -PbO₂ bath using atomic absorption spectrophotometer. The Pb(II) concentration increases with increasing the NaOH concentration, as shown in Table 1.

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Table 1 Pb(II) concentration in α -PbO₂ baths with 40 g/L PbO and different NaOH concentrations

$c(\text{NaOH})/(g \cdot L^{-1})$	120	130	140	150	160
$\overline{c(Pb(II))/(mol \cdot L^{-1})}$	0.1108	0.1197	0.1296	0.1383	0.1452

Furthermore, the remaining amount of the red sediments produced during the preparation of α -PbO₂ bath decreases with increasing the NaOH concentration. This indicates that all the baths are saturated with PbO, and the PbO amount of dissolved is the maximum when the NaOH concentration is 160 g/L. However, the current density increments of peak A_{IV} and α -PbO₂ electrosynthesis obtained in 160 g/L NaOH are not obvious compared with those in 150 g/L NaOH. Therefore, the continual increase of NaOH concentration in the bath has no obvious significance to the increase of Pb(II) concentration, which will even cause severe oxygen evolution due to the unsaturation of PbO when NaOH reaches 160 g/L. Therefore, it is suitable to keep the NaOH concentration in the bath at 160 g/L.

3.2 Effect of PbO addition amount on α-PbO₂ electrosynthesis

The anodic polarization curves tested in the bath with 160 g/L NaOH and 20–50 g/L PbO are shown in Fig. 2. The current densities of Pb passivation and peak A_{IV} obtained in the bath with 20 g/L PbO are obviously higher than the others. However, the α -PbO₂ electrosynthesis current density and the initial oxygen evolution potential (about 0.68 V) in such bath are the lowest. It is mainly because the concentrations of Pb(II) and OH⁻ ions are the lowest and highest in the bath containing 20 g/L PbO, respectively. This can also be confirmed by the complete solution of PbO, and there is no red sediment remaining during the preparation of such bath, i.e., the Pb(II) does not reach saturation. Therefore, the Pb passivation rate is the fastest, but the α -PbO₂ synthesis rate is the lowest. When the PbO addition



Fig. 2 Anodic polarization curves of Al/Pb in baths at 25 °C (Scan rate: 10 mV/s)

amount is 30–50 g/L, the current density magnitude of each curve has no obvious difference except that the α -PbO₂ electrosynthesis current density obtained in the bath with 30 g/L PbO is lightly lower than that obtained in the baths with 40 and 50 g/L PbO. In addition, there is little red sediment remaining during the preparation of the bath containing 30 g/L PbO. However, a few red sediments remain when the PbO addition amount is 40 g/L and more red sediments remain as the PbO addition amount reaches 50 g/L. It can be concluded that the Pb(II) concentration in the bath with 30 g/L PbO is near saturated, and that in the baths with 40 and 50 g/L PbO is fully saturated. In consequence, it is suitable to keep the PbO addition amount in the bath at 40 g/L.

3.3 Influence of bath temperature on α -PbO₂ electrosynthesis

The anodic polarization curves of Al/Pb obtained in the bath with 160 g/L NaOH and 40 g/L PbO at different temperatures (25–45 °C) are shown in Fig. 3.



Fig. 3 Anodic polarization curves of Al/Pb at different bath temperatures (Scan rate: 10 mV/s)

With increasing the bath temperature, the current density in the passivation region increases, but the initial oxygen evolution potential decreases gradually for the activity of OH⁻ ions is enhanced in the bath. Thus, the Pb passivation rate increases, and the oxygen evolution reaction becomes easier. In addition, the rupture of the PbO passivition film becomes easier as peak A_{II} becomes marked. Moreover, the current densities of peak A_{IV} and α -PbO₂ electrosynthesis gradually increase to the maximum with the temperature increasing to 40 °C. The thermodynamic analysis of α -PbO₂ electrosynthesis in alkaline bath shows that the standard electrode potential falls from 0.6392 to 0.5644 V when the bath temperature rises from 25 to 100 °C [20]. Therefore, increasing the bath temperature is beneficial to promoting the α -PbO₂ electrosynthesis.

However, the current densities of peak A_{IV} and

 α -PbO₂ electrosynthesis decrease obviously when the temperature exceeded 40 °C, and peak A_{IV} becomes sharp. This indicates that the α -PbO₂ electrosynthesis rate slows down under this condition. As the electrosynthesis of α -PbO₂ is an exothermic reaction, the faster the reaction runs, the larger the amount of heat releases. As a result, the continual increase of the bath temperature will hinder Pb(II) moving to the surface of the working electrode to oxidize and synthesize α -PbO₂[19]. And the peak A_{II} at 45 °C is more obvious than others, indicating that the PbO passivation film can break down easily, which may weaken the bond between the α -PbO₂ deposition layer and the Pb underlayer. In consequence, it is advisable to keep the bath temperature at 40 °C.

3.4 Influence of current density on α-PbO₂ electrosynthesis

At the beginning of α -PbO₂ electrosynthesis on Al/Pb, the high current density is necessary to promote the passivation of Pb underlayer and the nucleation of α -PbO₂, otherwise the Pb underlayer will be dissolved and the α -PbO₂ electrosynthesis will be impossible [18,20]. The galvanostatic polarization curves obtained in the bath with 160 g/L NaOH and 40 g/L PbO at 40 °C and different current densities are shown in Fig. 4.

Fig. 4 Galvanostatic polarization curves of Al/Pb at different current densities

As shown in Fig. 4, when the current density is 10 mA/cm^2 , the working electrode potential almost keeps at about -0.8 V, just a little rise after 500 s. The open circuit potential of Al/Pb under such condition is about -0.82 V (vs SCE), indicating that the Pb underlayer is difficult to be passivated at 10 mA/cm^2 . Of course, it is impossible to synthesize α -PbO₂ on Al/Pb. When the current density is 15 mA/cm^2 , the working electrode potential is about -0.8 V during the first 130 s, then sharply rises to 0.35 V and gradually decreases to a stable value (about 0.2 V). In detail, the process presents three peaks ($A_{\rm I}$, $A_{\rm II}$ and $A_{\rm III}$). This indicates that the Pb

surface is passivated to form a PbO film with poor conductivity in first 130 s, then further oxidized into α -PbO₂. Peak A_1 may reflect that the current density is not high enough to promote PbO transform into α -PbO₂ smoothly. Peak A_{II} reflects that the α -PbO₂ formed by the self-oxidation of PbO film, whereas the peak A_{III} reflects that the α -PbO₂ is formed by the oxidation of Pb(II) in the bath. In addition, the potential difference between A_{II} , A_{III} (about 0.35 V) and the stable value (about 0.2 V) reflects that the nucleation of α -PbO₂ is difficult, and it requires a certain magnitude of overpotential to decrease the activation energy of the α -PbO₂ electrosynthesis. The electrode potential begins to slightly increase at about 500 s due to the concentration polarization.

When the current density is 20 mA/cm^2 , the potential rapidly increases from -0.8 V to 0.35 V in first 50 s and peak A_{IV} appears but peak A_{I} disappears. This indicates that the Pb underlayer can be rapidly passivated to form PbO, and then successfully oxidized into α -PbO₂ at such a current density. In addition, it can be thought that peak A_{IV} is overlapped by peaks A_{II} and A_{III} , i.e., the oxidization of PbO film and Pb(II) to synthesize α -PbO₂ occurs simultaneously. Then, the potential is maintained at about 0.25 V, and obviously rises to 0.6 V after 450 s. Peak $A_{\rm V}$ appears at about 550 s, and severe oxygen evolution occurs. Therefore, it is suitable to keep the current density at 20 mA/cm² to promote the Pb surface passivation and α -PbO₂ nucleation for 3 min at the beginning of the α -PbO₂ electrosynthesis on Al/Pb. Then, a low current density is chosen to steadily synthesize α -PbO₂ and effectively avoid oxygen evolution caused by the concentration polarization.

The current density in the α -PbO₂ electrosynthesis region of anodic polarization curve is higher than the real diffusion current density of α -PbO₂ limiting electrosynthesis, as the anodic polarization is a transient process and the current density in the α -PbO₂ synthesizing region also includes that in the Pb passivation region. Therefore, the small current density should be obtained by quasi-steady state polarization. The quasi-steady state polarization curve of Al/Pb in α -PbO₂ bath is shown in Fig. 5. In which, the Al/Pb is passivated at 20 mA/cm² for 3 min in advance. As Fig. 5 shows, the current density increases with increasing the electrode potential. In detail, it changes little (about 5.5 mA/cm²) within 0.3–0.5 V. This indicates that the α -PbO₂ electrosynthesis is controlled by the mass-transfer diffusion step as the potential is above 0.3 V, however, it is controlled by the electrochemical step when the potential is below 0.3 V. Then, the current density increases sharply due to the oxygen evolution when the potential is above 0.5 V. Therefore, the stable electrosynthesis of α -PbO₂ can be realized at 5 mA/cm², and the oxygen evolution reaction can be avoided.

Fig. 5 Quasi-steady state polarization curve of Al/Pb with passivation treatment

3.5 Phase compositions and surface microstructures of Al/Pb and Al/Pb/α-PbO₂

The XRD patterns of Al/Pb before and after passivation treatment at 20 mA/cm² for 3 min, and those of Al/Pb/ α -PbO₂ synthesized at 5 mA/cm² for 2 min, 5 min and 2 h, respectively, are shown in Fig. 6. And their SEM images are shown in Fig. 7.

As shown in Fig. 6, there are some lead oxides with intermediate state, such as PbO and Pb_3O_4 , appearing in the Pb underlayer after passivating the Al/Pb for 3 min. This indicates that the Pb passivation process is step by

Fig. 6 XRD patterns of Al/Pb and Al/Pb/ α -PbO₂: (a) Al/Pb without passivation; (b) Al/Pb with passivation; (c) Al/Pb/ α -PbO₂ with α -PbO₂ electrosynthesis for 2 min; (d) Al/Pb/ α -PbO₂ with α -PbO₂ electrosynthesis for 5 min; (e) Al/Pb/ α -PbO₂ with α -PbO₂ electrosynthesis for 2 h

step oxidation. However, no α -PbO₂ is detected, as the α -PbO₂ film formed by the oxidation of Pb surface is too thin and loose to be detected. The α -PbO₂ appears after synthesizing α -PbO₂ for 2 min, which indicates that the α -PbO₂ begins to be synthesized on Al/Pb. The characteristic peaks of PbO and other lead oxides with intermediate state are weakened and even disappear when α -PbO₂ electrosynthesis is lasted for for 5 min, for

Fig. 7 SEM images of Al/Pb and Al/Pb/ α -PbO₂: (a) Al/Pb without passivation; (b) Al/Pb with passivation; (c) Al/Pb/ α -PbO₂ with α -PbO₂ synthesizing for 2 min; (d) Al/Pb/ α -PbO₂ with α -PbO₂ synthesizing for 5 min; (e) Al/Pb/ α -PbO₂ with α -PbO₂ synthesizing for 2 h

the α -PbO₂ deposition layer covers the Al/Pb surface and its thickness gradually increases. The α -PbO₂ with rhombic structure completely covers the Al/Pb when synthesizing α -PbO₂ for 2 h, and the characteristic peak of lead oxides with intermediate state disappears. Moreover, the α -PbO₂ crystalline characteristic peak intensities of (200) and (132) planes increase, but the rest is weakened with different extent.

Figure 7 shows the SEM images of Al/Pb and Al/Pb/ α -PbO₂. As can be seen from Fig. 7(a) that, the grains of Pb underlayer are uniform and arrange compactly. There are some whisker structures after passivating the Pb underlayer for 3 min (Fig. 7(b)). In addition, the grain shapes are various and the surface is loose. The whisker structure disappears and the grains are unevenly distributed on Al/Pb when α -PbO₂ is continued to synthesize for $2 \min (Fig. 7(c))$. It shows that the nucleation locations of α -PbO₂ on Al/Pb surface are selective. A uniform α -PbO₂ deposition layer covers the Al/Pb with α -PbO₂ electrosynthesis for 5 min (Fig. 7(d)). Then the α -PbO₂ deposition layer is constituted by well developed spherical unit cells with α -PbO₂ electrosynthesis for 2 h (Fig. 7(e)). In consequence, the α -PbO₂ electrosynthesis process according to the electrochemical analyses above is further confirmed here.

4 Conclusions

1) At the beginning of the α -PbO₂ electrosynthesis on Al/Pb with high current density, the Pb underlayer is firstly passivated to form a poor conductive PbO film. Then, the α -PbO₂ electrosynthesis is proceeded simultaneously with step by step oxidation of PbO (PbO \rightarrow Pb₃O₄ $\rightarrow \alpha$ -PbO₂ or PbO $\rightarrow \alpha$ -PbO₂). When an α -PbO₂ film is formed on the Pb underlayer, the continual α -PbO₂ deposition layer is mainly formed by the oxidation of Pb(II) in the bath.

2) The suitable plating conditions of α -PbO₂ electrosynthesis are 40 g/L PbO and 160 g/L NaOH at 40 °C. At the beginning of the α -PbO₂ electrosynthesis, the large current density of 20 mA/cm² is kept for 3 min to promote Pb passivation and α -PbO₂ nucleation. Then, steadily synthesizing α -PbO₂ is performed at a small current density of 5 mA/cm².

3) The α -PbO₂ deposition layer obtained in the alkaline bath possesses the rhombic structure, and it is composed of well developed spherical unit cells.

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$Al/Pb/\alpha$ -PbO₂复合惰性阳极材料的电化学合成

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摘 要:利用恒电流从碱性镀液中在 Al/Pb 表面电化学合成 *a*-PbO₂ 沉积层,制备出 Al/Pb/*a*-PbO₂ 复合惰性阳极材料。通过阳极极化法考察 *a*-PbO₂ 镀液组成及镀液温度对在 Al/Pb 表面电化学合成 *a*-PbO₂ 的影响,采用 XRD 和 SEM 分别测试 Al/Pb 基体材料及 *a*-PbO₂ 沉积层的相结构和表面微观组织特征。结果表明: *a*-PbO₂ 的电化学合成 分由几个不同的步骤完成;适宜的条件能有效提高 *a*-PbO₂ 电化学合成速率并避免析氧副反应的发生;从碱性溶液中合成的 *a*-PbO₂ 具有斜方晶型结构,沉积层由发育良好的圆球形晶胞构成。 关键词: Al/Pb 基体; *a*-PbO₂; 电化学合成; 阳极极化

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